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THE POCKET BOOK OF REFRIGERATION AND ICE-MAKING

EDITED BY

A. J. WALLIS-TAYLER, C.E.

ASSOC, MEMB. INST. C.E.

ETC.

AUTHOR OF "REFRIGERATING AND ICE-MAKING MACHINERY," "REFRIGERATION COLD STORAGE AND ICE-MAKING," ETC. ETC.

Fourth Edition, Enlarged

ILLUSTRATED BY THIRTY-ONE DIAGRAMS

NEW YORK

THE NORMAN W. HENLEY

PUBLISHING COMPANY

132 NASSAU STREET

1905

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PUBLISHERS' PREFACE.

THE rapid extension of the use of Refrigerating and Ice-making Machinery, in recent years, with the establishment in important centres of Cold Stores and Ice Factories, has led to the demand for a handy Pocket-Book which should contain in an accessible form such formulæ, data, tables, and memoranda as are constantly required by persons engaged or interested in the industries connected with Refrigeration and Cold Storage. The present little volume (which, since its first issue, has been revised and enlarged by the addition of fresh matter and diagrams) is designed to meet this demand.

The contents of the Pocket-Book may be briefly described as comprising amongst other matter the subjects of Refrigeration (in outline); Cold Storage; Ice-making and the Storing of Ice; Insulation;

the Testing and Management of Refrigerating Machinery; General Tables and Memoranda, etc., etc. There is also a carefully prepared Index, whereby reference may readily be made to the information furnished upon any particular subject.

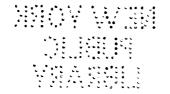


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THE POCKET-BOOK OF REFRIGERATION AND ICE-MAKING.

SECTION I. REFRIGERATION IN GENERAL.

THE MECHANICAL THEORY OF HEAT.

HEAT pervades every substance known. Lord Armstrong said, "According to the new theory, heat is an internal motion of molecules, capable of being communicated from the molecules of one body to those of another; the result of this imparted motion being either an increase of tempera-ture or the performance of work." The result of Joule's experiments was to demonstrate that under all circumstances the quantity of heat generated by the same amount of force is fixed and invariable. Professor Clerk Maxwell was of the opinion that heat, considered with respect to its power of warming things and changing their state, is a quantity strictly capable of measurement, and not subject to any variation of quality or kind.

The deductions to be arrived at on accepting this theory are, that if heat is a motion it must be an eternal one; the generation of heat in any substance must be additional to the heat that has been already generated in it or transferred thereto; heat can be lost or done away with to a degree only, as it is always of uniform quality, and it follows therefore that its annihilation must in every case be a definite part of the entire amount, and cannot be a reduction

in quality.

The rational conclusion to be come to from the above is that the reduction of temperature or cooling of any substance is simply the withdrawal or annihilation of a greater or lesser part of its own heat.

Refrigeration may be defined as the art of reducing the temperature of any body, or of maintaining the said

temperature below that of the atmosphere.

REFRIGERATING APPARATUS.

Widely, refrigerating apparatus may be classed under two main heads, viz. chemical and mechanical.

In the first, or apparatus working on the chemical system, the more or less rapid dissolution of a solid is utilised to abstract heat, and it is generally designated the liquefaction

process.

The second, or mechanical process, comprises apparatus operating on four different systems, viz.: cold-air machines, in which the air is first compressed, then cooled, and afterwards permitted to expand whilst doing work, that is to say, practically, by first applying heat to ultimately produce cold: vacuum machines, wherein the evaporation of a portion of the liquid to be cooled, assisted by the action of an air-pump, and of sulphuric acid, effects the abstraction of heat; absorption machines, in which the abstraction of heat is effected by the evaporation of a separate refrigerating agent of a more or less volatile nature, under the direct action of heat, which agent again enters into solution with a liquid; and lastly, compression machines, wherein the abstraction of heat is effected by the evaporation of a separate refrigerating agent of a more or less volatile nature, which agent is subsequently restored to its original physical condition by mechanical compression and cooling.

THE CHEMICAL OR LIQUEFACTION PROCESS.

During the change of the physical condition of a substance, for instance, whilst it is passing from a solid to a liquid form, the cohesive force is overcome by energy in the

form of heat, and this may be brought about without change in sensible temperature, provided the heat be absorbed as fast as it is supplied from the exterior, as in the case of melting ice, the temperature of which remains constant at 32° Fahr., any increase or decrease in the heat supplied simply hastening or retarding the rate of melting, but in no way affecting the temperature. Mixtures composed of some salts with water or acids, and of certain salts with ice, however, forming liquids having freezing points lower than the original temperatures of the mixtures, act in a different manner, the tendency to pass into the liquid form being in this case so strong that a more rapid absorption of heat takes place than is capable of being supplied from without, and consequently a consumption takes place of the store of heat of the melting substances themselves. The natural result of this action is that the temperature of the latter falls, until such time as the rate of melting and the rate at which heat is supplied from the exterior become equalised. The degree to which the temperature can be lowered depends to a certain extent on the state of hydration of the salt and the percentage of it present in the mixture. The salts used in ordinary freezing mixtures are generally those of certain alkalies which almost exclusively possess the necessary degree of solubility at low temperatures, and the following table gives the mixtures usually employed:-

TABLE OF PRINCIPAL FREEZING MIXTURES.

COMPOSITION OF FREEZING MIXTURES.	tempera	Reduction of temperature in degrees Fahr.	
	From	То	Amount of fall in de- grees Fahr.
Snow or pounded ice 2 parts; muriate of soda 1			
Snow 5; muriate of sodium 2; muriate of am-		- 5	
monia I		-12	
Snow 24; muriate of sodium 10; muriate of ammonia 5; nitrate of potash 5		-18	
Snow 12; muriate of sodium 5; nitrate of am-		_ 25	'
monia 5	+ 32	-25 -40	72
Snow I; chloride of sodium or common salt I	+ 32	0	32 82
Snow 2; muriate of lime crystallized 3 Snow 3; dilute sulphuric acid 2	+ 32 + 32	-50 -23	55
Snow 3: hydrochloric acid 5	+ 32	-27	59
Snow 7; dilute nitric acid 4	+ 32 + 32	-30 -40	62 72
Snow 2; chloride of calcium crystallized 3	+ 32	-50	82
Snow 3; potassium 4	+ 32	-51 - 5	83
Snow 5; chloride of sodium 2; chloride of am-			
monia I Snow 14; chloride of sodium 10; chloride of am-		-12	
monia 5; nitrate of potassium 5		-18	!
Snow 12; chloride of sodium 5; nitrate of ammonia 5		-25	ļ
Snow 2; dilute sulphuric acid 1; dilute nitric	1		١.
acid I Snow 12; common salt 5; nitrate of ammonia 5	-10 -18	-56 -25	46
Snow I; muriate of lime 3	-40	-73	33
Snow 8; dilute sulphuric acid 10	-68	-91	23
water 16	+ 50	+ 4	46
Nitrate of ammonia 1; water 1	+ 50	+ 4	46
sulphate of sodium 8; water 16	+ 50	+ 4	46
Sulphate of sodium 5; dilute sulphuric acid 4	+50	+ 3	47
Nitrate of sodium 3: dilute nitric acid 2	+ 50	- o - 3	50
Nitrate of ammonia 1; carbonate of sodium 1; water 1	-		
Sulphate of sodium 6; chloride of ammonia 4;	+50	- 7	57
nitrate of potassium 2; dilute nitric acid 4	+50	-10	60
Phosphate of sodium 9; dilute nitric acid 4 Sulphate of sodium 6; nitrate of ammonia 5;	+50	- I 2	62
dilute nitric acid 4	+50	-14	64

TABLE OF PRINCIPAL FREEZING MIXTURES-Continued.

COMPOSITION OF FREEZING MIXTURES. (Materials previously cooled.)	Reduction of temperature in degrees Fahr.		ount of I in de- es Fahr.
(Materials previously cooled.)	From	To	Amo fall grees
Phosphate of sodium 5; nitrate of ammonia 3; dilute nitric acid 4	0 -34 +20 0 -15 -10 0 -20 -40 -68	-34 -50 -48 -66 -68 -56 -46 -60 -73 -91	34 16 68 66 53 46 46 40 33 -23

COLD-AIR MACHINES.

This class of machine is based upon one of the simplest principles of physics, that is to say, that the compression of air or other gas generates heat, and the subsequent expansion of this air or gas, cold. Mechanical work and heat being respectively convertible, it naturally follows that if air or other gas be caused to perform certain work on a piston during expansion, the performance of this work will cause its store of caloric to become exhausted to a degree equal to the thermal equivalent of the work done, the air or other gas after expansion being at a lower temperature than that at which it was before expansion; that is, of course, provided always that no heat be supplied from any source to restore that so lost.

Cold-air machines all operate on the same general principle (see diagram, Fig. 1). The air is first compressed in a compressor, and the heat which is generated by this compression is removed by means of water, the cold air produced by expansion being employed for refrigeration. But there have been several notable

improvements during the past few years, practically removing most of the old defects, which make them compare favourably, with machines using more or less volatile agents, Cole's "Arctic" Machine being one that embodies important improvements.

The cycle of operations may be a perfect or closed one when the same air is in constant circulation, or where it is desirable to have pure air in the storage chambers, the air is rejected after once passing through the cycle, and fresh air is admitted at each stroke of the compressor.

Air machines, working at a comparatively low pressure, necessitate the compression and expansion cylinders being of a larger size than in compression machines using higher

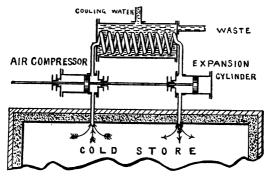


Fig. 1.—Diagram illustrating cold-air cycle.

pressures, but the total actual space occupied is no more, as cold-air machines are generally self-contained, there being no additional apparatus required in the form of expansion pipes, condensers, circulating pumps, etc., obviously, therefore, a simple, cold-air system, in which the defects of the old machines have been eliminated, has much to recommend it.

In the early days of cold air it was considered a disadvantage and uneconomical to reduce air to a very low temperature; but these objections are now entirely overcome by the improved methods of making the cold-air ducts or trunking, by which the loss is reduced to a minimum, and is almost inappreciable.

VACUUM MACHINES.

Vacuum machines, together with absorption machines, compression machines, and binary, or dual, or mixed, absorption and compression machines, all come under the category of vaporisation machines, that is to say, of machines which practically utilise the heat of vaporisation for purposes of refrigeration. In a vacuum machine the refrigerating agent or medium is, as has been already stated, water, its volatilisation at a temperature sufficiently low being effected by the means of a vacuum pump, assisted by sulphuric acid, by which the vapours are absorbed as soon as they are formed, and in this manner rendering the action of the vacuum very effective. The sulphuric acid can be again concentrated for use, and so on ad infinitum.

ABSORPTION MACHINES.

In its action the absorption machine resembles the vacuum machine, with this difference, however, that instead of water, some such liquid as anhydrous ammonia (NH₃), capable of evaporating at a low temperature without the assistance of a vacuum, is employed as a refrigerating agent or medium. Instead of sulphuric acid being employed to absorb the vapour, water is employed for that purpose, and from this water the vapour is again separated by distillation and is liquefied by the pressure which takes place in the still, and by the action of the condensing water. (See diagram, Fig. 2.)

In this manner absorption machines can be operated continuously, the ammonia solution or aqua ammonia being passed into a still or generator, usually heated by a steam coil or worm, and the ammonia vapour being conducted thence to a condenser in which it is cooled and becomes liquefied into anhydrous ammonia owing to the pressure due to its own accumulation. The anhydrous ammonia is kept in a liquid ammonia receiver, from which it passes to the coils of the refrigerator wherein it expands or evaporates, effecting an amount of refrigeration corresponding to its heat of vaporisation. After performing

this duty the vapour enters the absorber and is there brought into contact with the weak solution of ammonia coming from the bottom of the still, and is reabsorbed by it with generation of heat, which latter is removed by the cooling water. Both the rich and cold solution of ammonia coming from the absorber and going to the still, as well as the poor and hot solution coming from the still

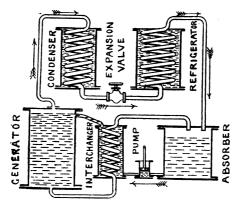


Fig. 2.-Diagram illustrating operation of absorption machine.

and going to the absorber, are passed through a device called an interchanger, by which their temperatures are equalised. The rich ammonia solution is pumped from the absorber into the still or generator.

THE COMPRESSION MACHINE.

Machines operating on the compression principle (see diagram, Fig. 3) utilise the latent heat of vaporisation of the substances having a low boiling point, and, whatever the refrigerating agent or medium that may be employed, they all practically act in the same manner; that is to say, the vapour or gas due to the expansion or vaporisation of the refrigerating agent or medium, in the refrigerating or expansion coils, passes into a compressor operated by any suitable power by which the gas or vapour is forced into the

coils of the condenser, and is there liquefied by the aid of the cooling water; the liquid thus formed then enters a liquid receiver, from which it is allowed to pass to the refrigerating coils through an expansion or flash valve or cock, by which the desired regulation can be effected. It will be seen that the process is a continuous one, representing a complete cycle of operations, inasmuch as the operating agent or medium periodically returns to its primary condition in a way that will more or less approach reversibility in accordance with the method of working peculiar to each machine.

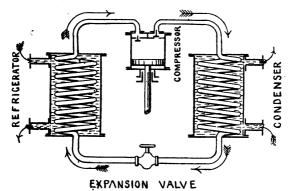


Fig. 3.—Diagram illustrating cycle wherein a volatile liquid and compression are employed.

A perfect reversible compression system comprises the following changes, viz.: An isothermal change due to the vaporisation or gasification of the refrigerating agent or medium at the constant temperature of the refrigerator; an adiabatic change, caused by the compression of the vapour or gas without the addition of heat; a second isothermal change, due to the condensation of the compressed gas or vapour at the constant temperature of the condenser; and, finally, a second adiabatic change, owing to the temperature of the liquid being reduced from that of the condenser to that of the refrigerator by a portion of the liquid being vaporised or gasified, and performing work by moving a piston, thus once more returning the refrigerating

medium or agent to its primary state, and thereby completing the cycle. It is presumed that the above changes take place in such a manner that the transfers of heat follow infinitesimal variations in temperature only, and the changes in volume occur in connection with infinitesimal variations of pressure. The changes can be likewise carried out in the obverse direction, the cycle being therefore a reversible one, and a refrigerating machine, which, it may here be observed, is the exact obverse to a heat engine, operated on this plan, will give as economical results as it is possible to obtain in practice.

For this reason it has been observed by Professor J. E. Siebel that the heat H, removed by a refrigerating apparatus operated strictly on the above-mentioned bases, has a certain and well-defined relation to the work or mechanical power, W, required to lift the same in the cycle of opera-If, in a refrigerating machine so operated, t_i is the temperature of the condenser and t_0 the temperature of the refrigerator (T₁ and T₀ designating the corresponding absolute temperatures), thermodynamics teach us that the following relations exist :-

$$\frac{H}{W} = \frac{t_0 + 460}{t_1 - t_0} = \frac{T_1}{T_1 - T_0}$$

Thermodynamically speaking, says the same authority, there should be no difference in economy on account of the nature of the circulating fluid if a perfect cycle of operation was carried out; but practically, this is not done. In all compression machines, the fourth operation, the reduction of the temperature of the liquid while doing work, is not carried out, but the liquid is cooled at the expense of the refrigeration of the system. No work is attempted, as the amount obtainable would not be in proportion to the expense involved in procuring the same.

The value of a circulating medium, it will be seen, is dependent upon its latent heat of vaporisation per pound, inasmuch as this quality governs its refrigerating effect. Regarding the choice of the circulating medium or agent, therefore, the above point must be taken into consideration, as well as the fact that the size of the compressor depends on the number of cubic feet of vapour that must be taken in to produce a certain amount of refrigeration, and that the strength of its parts will depend on the pressure of the circulating medium. Also that the loss of refrigeration, on account of cooling the liquid circulating medium, depends on the specific heat of the liquid as compared with the heat of volatilisation.

From the following table it will be seen that with ammonia the loss due to the cooling of the liquid, as shown in percentages for every degree difference in temperature of condenser and refrigerator, is less than in the case of other liquids, and total refrigerating effect per pound of liquid is largest, thus readily accounting for the preference generally given to ammonia as the circulating medium or agent. The only advantage possessed by sulphurous acid is the lower pressure of its vapour, and that of carbonic acid the smaller size of compressor necessary; the loss due to heating of liquid is very large in the latter case.

TABLE OF QUALITIES OF PRINCIPAL LIQUIDS EMPLOYED IN REFRIGERATION.—(Siebel.)

	Pressure in lbs. per square inch, at 0° F.	Heat of Vaporisation per lb., at 0° F.	Volume cubic feet per lb., at 0° F.	Specific Heat of Liquid.	Heat of Vaporisation per cubic foot.	Relative Volume of Compressor for Equal Refrigeration.	Loss due to Cooling Liquid.
Sulphurous Acid Carbonic Acid Ammonia	10 310 30	171·2 123·2 555·5	7:35 0:277 9:10	0.41 1.00 1.02	23·3 447· 61·7	61·70 3·24 23·3	Per cut. 0.24 0.81 0.18

THE APPLICATION OF THE ENTROPY, OR THETA-PHI, DIAGRAM TO REFRIGERATING MACHINES.

Entropy is the co-ordinate with the temperature of energy, that is to say, length on a diagram, the area of which is energy in heat-units, and the height of which is

absolute temperature; the abscissæ being the quotients found by the division of the heat quantity by the absolute temperature. Absolute temperature is denoted by the Greek letter theta, and entropy by the Greek letter phi, hence the temperature-entropy diagram is generally called the theta-phi (θ, ϕ) diagram.

In the case of an indicator diagram the co-ordinates are pressure and volume, the work done per stroke in footpounds being represented by the area. The theta-phi diagram represents the heat units as converted into work per pound of the working fluid, the area representing a quantity of heat in heat units, the vertical ordinates absolute temperatures, and the horizontal ordinates the quantity known as entropy. The special applicability of entropy diagrams to refrigeration was pointed out in 1892 by an American engineer, Mr. George Richmond, and they have also been used by Professor Linde for a considerable time

past.

The following application of the entropy diagram to refrigerators is abstracted from a useful little work (to which the reader is referred for fuller information on the subject) by Henry A. Golding, A.M.I.M.E., on "The Theta-phi Diagram," published by the Technical Publishing Co., Ltd., Manchester: "The cycle of operations in refrigerators is exactly the reverse of that in the Carnot hot-air engine. Instead of taking in heat at a high temperature τ_1 , and transforming part of it into work, and rejecting the remainder at a lower temperature τ_{ij} as in the heat-engine, the working substance in the refrigerator receives its heat at the lower temperature τ_2 , and discharges it at a higher temperature τ_1 , the extra energy required being obtained from external work done on the gas. The theoretically perfect cycle that is reversible is shown in Fig. 4 with pressure-volume ordinates, and in Fig. 5 with temperatureentropy ordinates. The first stage of the cycle, A to B, consists of the adiabatic expansion of a certain quantity of air, the temperature falling from τ_1 to τ_2 . From B to C the expansion is continued isothermally at constant temperature τ_2 , the air receiving heat from the body which it is desired to cool, the amount of heat abstracted being equal to the area EBCF (Fig. 5). Compression commences at C, and is at first carried on adiabatically at constant entropy (or isentropically) from C to D, the temperature rising from τ_2 to τ_1 , and is finally completed by isothermal compression from D to A, at constant temperature τ_1 , a quantity of heat being rejected to the water-jacket equal

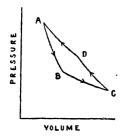


Fig. 4.—Diagram showing Theoretically Perfect Reversible Cycle, with Pressure Volume Ordinates.

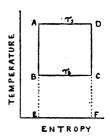


Fig. 5.—Diagram showing Theoretically Perfect Reversible Cycle, with Temperature-Entropy Ordinates.

to FDAE. The heat expended in the process is the equivalent of the work done on the gas, and is equal to the area ABCD in both diagrams. The heat absorbed from the substance to be cooled is equal to the rectangle EBCF (Fig. 5), and the efficiency, therefore (in its thermodynamic sense), is equal to the ratio—

$$\frac{EBCF}{ABCD} = \frac{\tau_2}{\tau_1 - \tau_2}$$

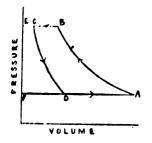
It is thus seen clearly how the efficiency is increased by reducing the difference of temperature between τ_1 and τ_2 , and as the ratio—

$$\frac{\boldsymbol{\tau}_2}{\boldsymbol{\tau}_1 - \boldsymbol{\tau}_2}$$

may sometimes be greater than unity, it is better known as "the coefficient of performance" (see Howard Lectures, by Professor Ewing, on "The Mechanical Production of Cold," Society of Arts, 1897).

The series of operations in air refrigerators with an open cycle is somewhat different, and is shown in Figs. 6 and 7.

In this case the air is taken from the cold room, and compressed adiabatically from A to B. It is then cooled at constant pressure, the temperature falling from B to C (Fig. 7), and contracting in volume from B to C (Fig. 6), after which it is passed into the expansion cylinder, where it expands adiabatically from C to D, and is discharged to the cold room again. The work done on the air in the compression cylinder is equal to the area EBAF (Fig. 6), or GCBH (Fig. 7), and that done by the air in the expansion cylinder is equal to ECDF (Fig. 6), or GDAH (Fig. 7); so that the net external work required is the difference of these



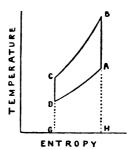


Fig. 6. - Diagram showing Operations in Air Kefrigerators with Open Cycle.

Fig. 7.—Diagram showing Operations in Air Refrigerators with Open Cycle.

two quantities, represented by the area enclosed by ABCD in both diagrams. The efficiency of the process will be represented by the ratio of the two areas—

$$\frac{\text{ECDF}}{\text{ECAF}}$$
 (Fig. 6)

but, as AB and CD are similar adiabatic curves, this will be equal to the ratio—

$$\frac{\mathbf{EC}}{\mathbf{EB}}$$
 or $\frac{\mathbf{FD}}{\mathbf{FA}}$

The following brief extracts from a paper on "The CTheory and Practice of Mechanical Refrigeration," by tempe T. R. Murray, Wh.Sc., read before the Institution of it is decers and Shipbuilders, Scotland, in December, 1897, equal to the interest:—The entropy diagram (Fig. 8) shows an

example of an application to the cold-air cycle, the air being taken in at a temperature t_1 of 18° Fahr., the temperature of the refrigeration chamber, and rejected at a temperature t_2 of 70° Fahr., which is the temperature of the air after being cooled by the cooling water; the temperature at which the cold air is discharged into the chamber to be taken as -85° Fahr., and the highest temperature to which it is heated in compression to be taken as 250° Fahr. Considering the machine to be theoretically perfect, then

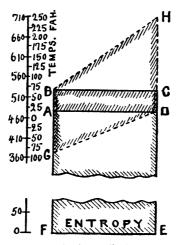
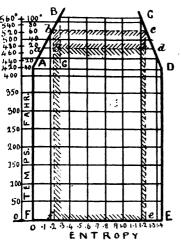


Fig. 8.—Entropy Diagram, showing Application to the Cold-air Cycle.

the diagram ABCD is obtained, in which D to C is the rise of temperature of the air during compression from 18° Fahr. to 70° Fahr.; CB represents the removal of heat in the cooler; B to A represents the cooling in expansion cylinder; and A to D, the collection of heat in the refrigerated chamber. The proportions of the areas ABCD and ADEF represent the proportion of work done to the refrigeration produced. The rectangle AE will be found to be 9'19 times the rectangle BD. In the working cycle, where the air is raised to 250° Fahr. in the compressor, this will be represented on the diagram by point H, and the fall in

temperature during cooling by HB. The temperature being again lowered in expansion cylinder to -85° Fahr., is represented by the vertical line BG, and the collection of heat in the chamber by GD. The diagram of work is now BHDG, which is about 3.75 times the theoretical amount, and when compared with the refrigeration done, now represented by area GDEF, gives an efficiency of only a little over 2. Losses by friction, moisture, etc., reduce this in practice to a little over $\frac{3}{4}$.

Fig. 9 is an entropy diagram for 1 lb. of saturated



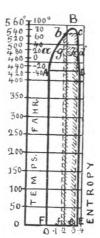


Fig. 9.—Entropy Diagram for 1 lb. of Saturated Ammonia Vapour from -40° to +100° Fahr.

Fig. 10.—Entropy Diagram for 1 lb. of Saturated Carbonic Acid Vapour from -40° to +100° Fahr.

ammonia vapour, from the temperature of -40° Fahr. to $+100^{\circ}$ Fahr. FE is the basis line, the temperature at this point being absolute zero, -460° Fahr.; A, the absolute temperature at -40° Fahr. = 420° Fahr. = T_1 .; B, the absolute temperature at, $+100^{\circ}$ Fahr. = 560° Fahr. = T_2 ; AD = the entropy at T_1 ; and considering that a unit weight of ammonia, say 1 lb. is being dealt with, the length

AD can be determined by taking $\frac{L}{T} = \frac{603.45}{420} = 1.436$. In

the same way, BC = $\frac{L_2}{T_2}$ - 0.922. The point G has still to

be determined in order to find the position of point B. Considering, however, that DC represents the compression in compressor, CB the giving out of heat to the condenser, BA the expansion through the orifice of expansion valve, and AD the taking in of heat in the refrigerator, it will be understood that AG really represents the entropy of the liquid heat carried into the refrigerator; and its length may

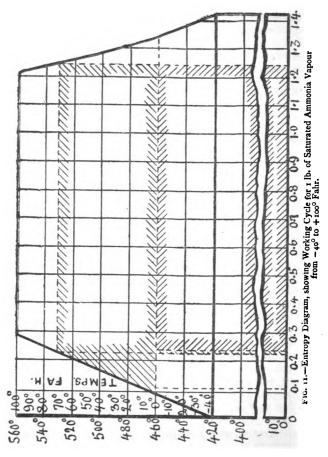
be found by the expression $AG = c \log_c \frac{T_2}{T_1}$, where c = mean specific heat of liquid between T_1 and T_2 . A simpler formula is $AG = \frac{h}{T_1 + T_2}$, where h = liquid heat $T_2 - liquid$

heat T1.

By calculating these values for various temperatures between T₁ and T₂, the points through which to draw the line BA are found. For ammonia it will be found to be practically a straight line, so that it is quite near enough to find the point B only and draw a straight line between A and B. By plotting as abscissæ the values of the entropy of the latent heat at same temperatures, the curve CD will be formed.

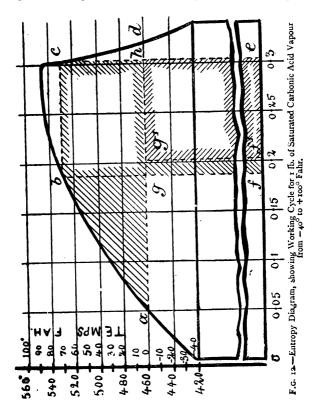
Fig. 10 is an entropy diagram for 1 lb. of saturated carbonic acid vapour from the temperature of -40° Fahr. to $+100^{\circ}$ Fahr., the same construction also applying in this case, but the formation being a continuous curve with a rounded top. To find the efficiency, by means of these diagrams, of a machine working with the same temperatures T_1 and T_2 as taken with the cold-air cycle, and considering, in the first place, the cycle as being the Carnot or perfect one, compression and expansion will both be adiabatic, therefore they will be represented by vertical lines, and the giving up of heat to the condenser, as well as the collection of same in the refrigerator, being isothermal, then will be shown as horizontal lines. Draw horizontals ad and be, and verticals bgf and che. Then the area bh will represent the work of the compressor, and the area ge the refrigeration done.

These equal respectively $bc \times T_2 - T_1$, and be $\times T_1$. The efficiency will therefore $= \frac{be \times T_1}{be \times (T_2 - T_1)} = 9.19$ as before.



In considering how nearly the actual working cycle approaches the above in practice, it must first be remembered

that the cooling agent simply circulates in pipes through the chambers being cooled, and must of necessity be colder in order to secure a transference of heat. The difference in temperature depends on the cooling surface, or length of



piping, as compared with the cubic capacity of the chamber, and may be in practice from 10° to 25° Fahr. Suppose that allowance be made for a difference of 18° Fahr., then the lower temperature T₁ will correspond to 0° Fahr. Again, the working cycle falls away from the Carnot cycle in not being

reversible, owing to expansion taking place through a small orifice instead of by means of an expansion cylinder. Thus the liquid carries a certain amount of heat into the refrigerator, which goes to heat up the expanded gas, rendering part of it unavailable for refrigeration. The amount of this liquid heat varies for each agent, and the entropy diagrams, Figs. 11 and 12, to a larger scale, show the working cycle in each case. In these, the areas agb represent the additional work that the use of an expansion cycle would have obviated. The heat which ought to have been spent in producing this work is carried by the liquid into the refrigerator, and this therefore falls to be deducted from the refrigeration done, so that the latter is now represented by the area $g_1 hef_1$, being less than before by the rectangle gf_1 , which is equal to area agb.

COMPARATIVE EFFICIENCY OF REFRIGERATING MACHINES.

Professor Ewing estimates the efficiency of the absorption machine at from two and a half to three times that of the cold-air machine, and the efficiency of the vapour-compression machine at from five to six times that of the cold-air machine, and from two and a half to three times that of the absorption machine.

In comparing one system with another, the theoretical values obtained at the machines are not sufficient, as the combined losses in piping, brine cooling, circulating pumps, fans, and any other auxiliary apparatus, must be considered, and only the actual net useful duty performed taken into account. And further, an amount must be added to the capital interest in a plant for recharging with gas (except air machines), including incidentals such as calcium chloride and other items necessary to the system.

Refrigerating machines, to be efficient, must be efficient when working in hot weather or tropical climates. Some systems fall off considerably when the cooling water is about 60° Fahr., and the atmosphere above 70° Fahr., and in some the cost of working is so high under tropical conditions as to render their use almost prohibitive. The coldair system does not fall off in the same ratio, and for many purposes is the most economical. All the losses under this system are in the machine, as the air after leaving the

machine does not pass through any secondary process, but is conducted direct to the storage or cooling chamber without the use of brine, circulation pumps, fans, etc.

RATIO OF PRESSURE OF SO₂, NH₃, and CO₂.

(From Landolt & Bornstein's Physico-Chemical Tables, Lister & Co., Ltd., Catalogue.)

T	Pressure expressed in pounds per square inch.							
Temperature in Degrees Fahr.	Sulphurous Acid. SO ₂ .	Ammonia. NH3.	Carbonic Acid.					
-4		12	276					
+ 5	-	18	325					
14	0	27	374					
23 32	4	35	435					
32	8	3 5 46	502					
41	11	59	566					
50	18	73	660					
5 9 68	25	90	750					
	32	108	840					
77 86	41	129	950					
86	51	152	1,060					
95	62	180	1,280					
104	75	208	1,320					

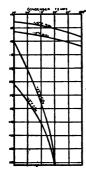


Fig. 13.—Diagram showing Loss of Efficiency with NH₃ and CO₂ owing to use of Expansion Valve.—(Murray, Inst. Engrs. and Shipbuilders, Scotland, 1897.)

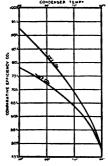


Fig. 14.—Diagram showing Percentage of Efficiency of Working Cycle of CO₂ as compared with NH₃.—(Murray, Inst. Engrs and Shipbuilders, Scotland, 1897.)

RESULTS OF TEST EXPERIMENTS WITH COLD-AIR MACHINES.

	Haslam.*	Bell- Coleman.+	Cole's". No. 4 Size.	Arctic"‡ No. 1 Size.
Diameter of comp. cy. in ins. Diameter of exp. cy. in ins Stroke of each Revs. per minute Air pres. in receiver (abs.) in lbs. per sq. in Temp. of air entering comp. cy.	25 ¹ (2 cy.) 19 ¹ ,, 36 72 64	28 21 24 63·2	9 12 96 65	63 54 8 160 75
(cont. vapour up to 88 per cent. of sat.) in deg. Fahr	_ 	65.5	48 35_	46 —
Temp. of air after expansion, Fahr. Init. temp. of cooling water, Fahr. I. H.P. in comp. cy I. H.P. in exp. cy Per cent. of I. H.P. of comp. retained	-85 - 346·4 176·2	-52 -58.5 58.5	-81 62 14·5 7·8	-98 41 3·28 1·68
in expander	51	47	54	51

EFFECTIVE COOLING POWER OBTAINABLE FROM THE EX-PENDITURE OF ONE POUND OF STEAM IN THEORETI-CALLY PERFECT MACHINES.—(Tuxen & Hammerich's Cat.)

Ammonia by the absorption system. Thermal Units 294 equal to 24 lbs. of ice per lb. of coal consumed.

Carbonic Anhydride ... 652 equal to 26 lbs. of ice per lb. of coal consumed.

Ammonia by the compression system 978 equal to 40 lbs. of ice per lb.

of coal consumed.

* "Proceedings, Manchester Society of Engineers," 1894.

‡ A. J. Wallis-Tayler, A.M.I.C.E., 1902.

[†] Prof. Schroeter, "Untersuchungen an Kaeltemaschieren Verschiedener Systeme," 1881.

TESTS OF AMMONIA AND CARBONIC ACID MACHINES.

(Schroeter, Experimental Refrigerating Station, Munich, Germany.)

	AMM	ONIA	МАСІ	HINE.	CARBONIC ACID MACHINE.*			
No. of test-	1	2	3	4	5	6	7	8
Temperature in brine tank, de- grees Celsius	-6.1	-6.4	-6.4	-4.8	-4.0	-4.8	-4.8	-6.7
Temperature in condenser, de- grees Celsius	21.4	21.4	21.4	34 ·9	20.9	21.5	22.2	30
Temperature before expan- sion valve, de- grees Celsius		11.6	18.4	28.3	-7:9	10.0	16.8	28.8
Refrigeration per hour, per horse power of steam - engine in calories	3897	3636	3508	2237	3832	3178	2867	1477

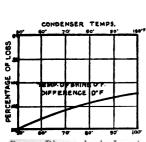


Fig. 15.—Diagram showing Loss of Efficiency with Brine Circulation compared with Direct Expansion of NH₃.—(Murray, Inst. Engrs. and Shipbuilders, Scotland. 1897.)

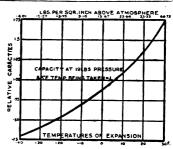


Fig. 16.—Diagram showing Relative Compressor Capacity with NH₃ at various Expansion Pressures and Temperatures.—(Murray, Inst. Engrs. and Shipbuilders, Scotland, 1897)

• Dr. Mollier has since proved these results to be incorrect. See "Zeitschrift für Die Gesammte Kalte Industric,"

THE PRODUCTION OF VERY LOW TEMPERATURES.

The idea of self-intensive refrigeration, or the regenerative process, seems to have occurred to Siemens, Coleman, Solway, and others many years ago, the first-named having applied for a patent in Germany for such a process as long ago as 1857; and in 1885 the latter patented a similar device and made an apparatus by means of which, however, he was only able to obtain a temperature as low as —140° Fahr., and was not successful in liquefying air. The first perfect self-intensive refrigerating methods are due to Professor Linde and Dr. William Hampson.

The methods primarily employed for the production of intense cold were arranged to operate upon what is known as the cascade system; that is to say, carbonic acid, methyl chloride, nitrous oxide, or any other gas capable of being easily liquefied, is first compressed by a pump, then cooled by water, and finally allowed to pass through a contracted orifice or expansion valve, at lower pressure and reduced to a temperature of, say for instance - 110° Fahr., and back again to the compression pump,—in fact, a precisely similar cycle to that of the ammonia compression machine. The low temperature liquid and vapour thus produced then performs a second cycle, taking the place which water takes in the first, and is used to effect the cooling and condensation of a gas of a more volatile nature, such as ethylene, which latter, on passing the orifice or expansion valve, liquefies and vaporises at a still lower temperature, of, say, about -155° Fahr., the exact degree varying according to the pressure maintained on the suction side of the compressor pump. By the ethylene, compressed air or oxygen is cooled in a like manner, and the pressure of the liquid air or oxygen being reduced by passing through an expansion valve, becomes partly vaporised by its own heat, that portion remaining a liquid under atmospheric pressure being reduced to the boiling point of air.

In the self-intensive, or regenerative, method of producing very low temperatures, only one circuit of gas is required, viz. that of the air to be liquefied. This air, starting at an ordinary temperature, with the assistance of only water as a refrigerant, lowers by degrees its own temperature of expansion, by returning over the coils of compressed gas

in the above-mentioned manner, until it reaches the boiling point of air, the liquid then commencing to collect at the

pressure of the atmosphere.

The improved apparatus of Dr. Hampson is founded on the well-known fact that any gas, when expanding through a small aperture, will perform such work upon itself as to effect a reduction of temperature, and this effect with air, although not large, is still appreciable. The whole of the gas expanded is used to lower, to a small extent, the temperature of the gas passing to the expansion aperture. This results in the gas expanded being somewhat lower in temperature than that previously expanded, and consequently the succeeding gas is cooled to a further reduced temperature, proceeding thus until the gas attains such a temperature that it commences to liquefy, or until such time as the removal of the heat within the apparatus becomes counterbalanced by the access of heat from the exterior thereof.

The apparatus employed is mainly composed of a series of long, well-insulated, fine copper coils, through which the gas passes to the expansion valve, the arrangement being such that the expanded gas has to flow over the entire external surface of the coils before being removed, so as to abstract as much heat as practicable from the entering gas.

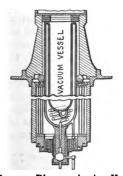


Fig. 17.—Diagram showing Hampson's Apparatus for the Production of very Low Temperatures.

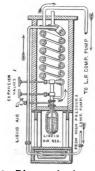


Fig. 18.—Diagram showing Linde's Apparatus for the Production of very Low Temperatures.

CAPACITY OF REFRIGERATING MACHINES.

Refrigerating machines are rated in two ways, viz. ice-making capacity, or tons of ice they will produce in one

day of twenty-four hours; and refrigerating capacity, or cooling work done by one ton of ice melting per day of twenty-four hours. Roughly, the first or ice-making capacity of a machine may be taken to be about one-half of the refrigerating capacity. This, however, is only an approximation, as the tons of ice a refrigerating machine is capable of making depends upon the initial temperature of the water to be frozen. The unit of capacity is one ton of ice made from water at 32° Fahr. into ice at 32° Fahr. per day, which, according to practice here, is equal to 318,080 lbs. of water cooled one degree, or to 318,080 heat units or thermal units; and, according to American practice, is equal to 284,000 lbs. of water cooled one degree, or 284,000 heat units or thermal units; and this is the tonnage basis for refrigerating capacity as well as for ice-making capacity when ice is made from water at 32° Fahr. The difference between English and American practice is due to 2240 lbs. being taken to the ton in the former, and 2000 lbs. in the latter case.

The real ice-making capacity of a machine is dependent upon the temperature of the water to be frozen, and is calculated as follows: I lb. of ice in melting into water at 32° Fahr. will take up 142 positive units of heat, it follows, therefore, that water at 32° Fahr. will require 142 negative units of heat to make it into ice. Say that if the water to be frozen, for instance, be at a temperature of 72° Fahr., it must first be cooled down to 32° Fahr. before freezing commences; therefore $72^{\circ}-32^{\circ}=40^{\circ}+142=182$ heat units per pound of water frozen. Ice made artificially is usually much below 32° Fahr., as the temperature of the bath in which it is made ranges about 20° below freezing point, and consequently this work has also to be added. Taking into account the specific heat of ice, this additional negative heat approximately equals 10 units,

which added to 182 = 192; therefore $\frac{142 \times 100}{192} = 73.963$,

or nearly 74 per cent. tons of ice made per ton refrigerating capacity. For greater accuracy, allowances must also be made for losses by ice tank and can exposure, wastage, thawing out of moulds, etc., etc.

TABLE OF COMPRESSOR CAPACITY IN CUBIC INCHES.

(Norman Selfe, "Machinery for Refrigeration.")

The tabular number multiplied by strokes per minute and divided by 1,728 gives cubic feet per minute theoretical capacity of the cylinder.

	Cylinder Diameter in inches.		1 1 4 4 W 4 N 0 1 - 80 0 0
	02	C. Ins.	7.854 17.672 31.416 49.087 70.686 195.56 195.35 282.74 384.84 502.65 636.17
	6	C. Ins.	7.068 15.905 28.274 44.178 63.617 176.71 254.35 452.38 706.86
	80	C. Ins.	6.283 14.137 25.132 39.269 59.549 157.08 226.19 307.87 402.12 508.93
INCHES.	7	C. Ins.	5.948 12.370 21.991 34.36 49.480 87.962 137.94 197.92 269.39 351.85 445.32
STROKE IN INCHES.	9	C. Ins.	4.712 10.602 18.849 29.452 42.411 17.396 117.81 169.64 230.90 301.59 381.70
OF	'n	C. Ins.	3.927 8.835 15.705 24.543 35.343 62.830 98.175 192.42 192.43 251.32 392.70
LENGTH	4	C. Ins.	3.141 7.068 12.566 19.634 28.274 28.274 78.540 113.93 153.93 201.06 254.47
	8	C. Ins.	2.356 5.301 9.425 14.726 21.206 23.698 84.825 115.45 115.45 110.85 235.62
	8	C. Ins.	1.571 3.534 6.283 9.817 14.137 25.132 36.548 76.968 100.53 157.08
	н	C. Ins.	0.785 1.767 3.147 4.908 7.068 12.566 19.035 28.274 38.484 38.484 50.265 63.617
meter i	Cylinder Diameter in inches.		1, 2, 2, 2, 2, 2, 2, 2, 2, 2, 2, 2, 2, 2,

Table of Compressor Capacity in Cubic Inches.—(Continued.)

neter	er Diar inches	Cylind	11	12	13	14	15	91	17	18	19	20	22	24	56	28	30	32	34	36
	OI	C. Ins.	950.33	6.0211	1327.2	1539.3	1.2921	2010.6	2269.8	2544.6	2835.2	3141.6	3801.3	4523.9	5309.3	6157.5	9.8904	8042.4	2.6206	0.2101
	6	C. Ins.	855.29	8.2001	2.4611	1385.3	1590.3	1809.5	2042.8	1.0622	2551.6	2827.4	3421.1	4071.5	4778.3	5541.7	6361.7	7238.1	8171.2	9153.7
	∞	C. Ins.	200.56	604.72	8.1901	1231.4	1413.6	1608.4	1815.8	2035.6	2268·I	2513.2	3041.0	3619.1	4247.4	4926.0	5654.8	6433.6	7263.3	8136.6
INCHES.	7	C. Ins.	665.23	29.162	11.626	1077.5	1236.9	1.407.4	1588.8	1781.2	9.4861	1.6612	6.0992	3166.7	3716.5	4310.2	0.8464	9.6295	6355.4	7119.5
STROKE IN I	9	C. Ins.	61.025	678.54	796.38	923.28	2.0901	1206.3	1361.8	1526.7	1.10/1	6.4881	2280.8	2714.3	3185.5	3694.5	4241.1	4825.4	5447.5	6102.4
OF STRO	25	C. Ins.	475.16	565.45	9.899	29.692	883.55	1005.3	26.406	1272.3	9.211	1570.8	9.0061	6.1922	5654.6	3078.7	3534.3	4021.2	4539.6	5085.4
LENGTH	4	C. Ins.	380.13	452.36	530.92	615.72	706.84	804.24	1134.9	8.2101	1134.0	1256.6	1520.5	1809.5	2123.7	2463.0	2827.4	3216.9	3631.6	4068.3
	6	C. Ins.	585.09	339.27	398.19	62.194	530.13	603.18	680.64	763.38	850.56	945.48	1140.4	1357.1	1592.7	1847.2	2120.5	2412.7	2723.7	3051:2
	2	C. Ins.	90.061	226.18	265.46	307.86	353.42	402.12	453.96	508.92	567.04	628.32	200.56	84.18	8.1901	1231.5	1413.7	1608.4	1815.8	2034.1
	н	C. Ins.	95.033	60.811	132.73	153.93	12.921	201.01	226.98	254.46	283.52	314.16	330.13	452.39	530.93	615.75	98.904	804.24	26.206	8.2101
weter	ler Diar	Cylind	11	12	13	14	15	91	17	18	61	20	22	24	26	28	30	32	34	36

TABLE OF COMPRESSOR CAPACITY IN CUBIC INCHES.—(Continued.)

moeter s.	ler Dia	baily O ai	1 1 a a w 4 w 0 5 2 0 1 a w
	Ť	C. Ins.	18.84 73.399 117.81 117.81 117.81 117.81 117.84 17.24 17.26 18.84 17.26 18.84 18.84 31.85 31.85
	22	C. Ins.	17:279 38:877 69:113 107:90 107:90 107:90 107:90 107:90 107:90 107:90 107:90 107:00 10
	80	C. Ins.	15.708 35.343 62.834 62.834 98.174 141.37 392.70 392.70 165.68 1000.6 2261.6
INCHES.	81	C. Ins.	14.137 31.809 56.549 88.356 127.23 226.19 353.43 508.93 508.93 508.71 1145.1 1413.7 1710:5
STROKE IN 1	92	C. Ins.	12.566 28.274 50.265 78.539 113.09 201.05 314.106 452.38 6015.74 804.24 1017.8 1780.5
OF	13	C. Ins.	26.507 47.124 73.630 188.49 294.52 724.11 577.26 757.26 757.26 757.26 757.26 757.26 757.26 766.4 1696.4
LENGTH	71	C. Ins.	10.995 24.740 43.982 68.721 68.721 175.92 274.89 336.83 336.43 1099'5 11330'4 1588'3
	£.	C. Ins.	10.110 22.973 40.841 63.813 61.892 163.85 255.25 500.29 653.44 827.02 1021.0
	13	C. Ins.	9.425 21.206 37.699 58.904 84.823 150.79 235.62 339.29 603.18 763.40 763.40 140.3 1357.1
	11	C. Ins.	8-639 9-439 34-557 53-995 138-22 215-98 311-01 423-32 552-91 6699-78 863-94 1045-3
meter	Cylinder Diameter in inches.		11 2 2 2 3 2 4 3 3 2 4 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1

TABLE OF COMPRESSOR CAPACITY IN CUBIC INCHES.—(Continued.)

meter	er Dia	Daily O ai	14	201	11	81	19	20	77	54	56	28	30	32	34	36
	42	C. Ins.	3694.5	4241.1	5447.5	2.2019	6804.7	7539.8	9123.1	10857.0	12742.0	0.8241	0. 19691	0.10261	21,790.0	24418.0
	22	C. Ins.	3386.6	3007.7	4993.5	5598.3	6237.6	9.1169	8362.9	9952.5	0.08911	13546.0	15550.0	17693.0	0.42661	22383.0
	8	C. Ins.	3078.7	3534.3	4539.6	5089.3	5670.5	6283.2	9.2092	9047.8	10618.0	12315.0	14137.0	16085.0	18158.0	20347.0
INCHES.	81	C. Ins.	2770.8	3100.0	4085.6	4580.4	5103.5	5654.8	6842.3	8143.0	9556.7	0.89011	12723.0	14576.0	13642.0	18311.0
LENGTH OF STROKE IN INCHES	16	C. Ins.	2463.0	3216.9	3631.6	4071.5	4536.4	5026.5	1.2809	7238.2	8494.8	9852.0	11309.0	12868.0	14526.0	16275.0
OF STR	15	C. Ins.	2309.0	3015.0	3404.7	3817.0	4252.9	4712.4	6.1025	6785.8	6.8962	9236.3	0.20901	12063.0	13618.0	15258.0
LENGTH	14	C. Ins.	2155.1	2814.8	3177.7	3562.5	3969.4	4398.2	5321.8	6333.4	7433.0	8620.5	0.9686	11259.0	0.01/21	14240.0
	13	C. Ins.	1.1002	2.2622	2650.7	3308.0	3685.8	4084.0	4941.7	5881.0	0.2069	8004.7	1.6816	10455.0	11802.0	13232.0
i	12	C. Ins.	1847.2	2412.7	2723.7	3053.6	3402.3	3769.9	4561.5	5428.6	6371.1	7389.0	8482.3	6.0596	0.56801	12214.0
	11	C. Ins.	1693.2	2211-6	2496.8	0.6622	3118.7	3455.7	4181.4	2.9/64	5840.2	6773.2	7775.4	8846.6	1.2866	0.28111
Cylinder Diameter in inches.		14	16.5	17	20	61	8	22	24	56	82	ဇ္	32	34	36	

MEAN PRESSURE OF COMPRESSOR.

The following table from the De La Vergne catalogue admits of the mean pressure in the compressor, and indirectly the work of the compressor being approximately ascertained from the refrigerator and condenser pressure and temperature :---

105%	60.99	72.08	82.97	91.29
	64.08	75.84	86.18	93.19
	68.09	79.61	88.91	94.52
1			∞ ∞ ∞	288
8	58·54	68·81	78·59	85.58
	61·40	72·22	81·39	86.98
	65·14	75·61	83·68	87.78
95°	56.11	65.53	74.24	79.88
	58.86	68.62	76.60	80.77
	62.16	71.62	78.46	81.02
306	53.68	62.25	69.86	74.17
	56.08	65.00	71.81	74.56
	59.20	67.66	73.23	74.28
825	51.23	58.97	65.51	68.46
	53.40	62.40	67.02	68.35
	56.25	63.67	67.98	67.52
8	48·77	55.70	61.13	62.75
	50·74	57.78	62.23	62.14
	53·29	59.68	62.75	60.76
75.	46.34	\$2.42	56.77	57.05
	47.90	54.16	57.44	55.92
	50.33	55.70	57.53	54.02
702	43.91	49.15	\$2.40	51.34
	45.38	50.56	\$2.67	49.71
	47.38	51.73	\$2.30	47.26
025	41.46 42.72 44.40	45.86 46.94 47.74	48°04 47°88 47°08	45.06 43.16 40.52
emperature. Refrigerator Temperature.	1 1 1 1 20	໙ິ ໕໙ິ I	20,25	25° 30° 35°
Condenser T Refrigerator Pressure.	49 0	13 16 20	33 84	39 51
The second secon	Temperature.	41.46 43.91 46.34 48.77 51.23 53.68 56.11 5 44.40 47.38 50.33 53.29 56.25 59.20 62.16 6	41.46 43.91 46.34 48.77 51.23 53.68 56.11 54.40 47.78 50.74 53.40 56.08 58.86 64.40 47.38 50.33 53.29 56.25 59.20 62.16 64.40 47.8 53.40 55.70 58.97 62.25 65.53 65.64 65.00 68.62 77 55.70 59.08 63.67 67.66 71.62 7	41.46 43.91 46.34 48.77 51.23 53.68 56.11 54.70 47.38 50.33 53.29 56.25 59.20 62.16 66.44.40 47.74 50.35 57.08 58.97 62.25 65.53 66.94 50.94 50.50 54.16 57.78 62.40 65.00 68.62 74.65 57.78 62.40 65.00 68.62 74.65 57.78 62.40 65.00 68.62 74.65 77.83 52.70 59.73 65.51 69.86 74.24 77.84 52.30 57.53 67.02 71.81 76.60 87.24 77.85 52.30 57.53 62.75 67.98 73.23 78.46 88

Table Giving Number of Cubic Feet of Gas that must be Pumped Per Minute at DIFFERENT CONDENSER AND SUCTION PRESSURES TO PRODUCE ONE TON OF REFRIGERATION IN 24 HOURS.

(Professor Siebel, "Compend of Mechanical Refrigeration.")

				1	_				_	_	_			_	_	_	
	105		218		2.88	6.43	5.83	2.08	4.44	3.61	3.46	3.12	2.82	2.51	2.24	10.2	1.85
	100	ch.	200		62.2	6.30	5.77	5.05	4.40	3.87	3.45	3.09	2.80	5.49	2.55	3.00	1.83
	.thr. 95	er square in	184		2.20	6.23	5.70	4.62	4.35	3.83	3.41	3.00	5.76	2.46	2.50	16.1	18.1
•	Temperature of the Gas in Degrees Fahr. 80 85 90	Corresponding Condenser Pressure (Gauge) 1bs, per square inch.	168	,	2.62	91.9	2.64	16.4	4.30	3.78	3.38	3.05	2.73	2.44	2.17	56.1	62.1
	the Gas in	Pressure (Ga	153		7.54	60.9	2.28	4.86	4.25	3.74	3.34	5.66	2.71	2.41	2.15	1.93	1.77
,	nperature of 80	Condenser]	139		2.46	6.03	5.25	4.81	4.51	3.70	3.30	96.2	3.68	2.38	2.12	16.1	92.1
•	. Ter 75	rresponding	127		7.37	2.66	2.46	4.26	4.17	3.66	3.27	2.63	5.65	2.36	2.10	1.89	1.74
	70	ပိ	115		7.3	6.5	5.4	4.73	4.12	3.63	3.54	5.6	19.2	2.34	2.08	1.87	1.72
,	65		103		7.22	5.84	5.35	4.66	60.4	3.29	3.50	2.87	2.29	2.31	90.2	1.85	02.1
	Saibnoc Pressure, aq. in,	[noitou	s	G. Pres.	-	4	٥	6	13	91	20	24	28	33	39	45	SI
	ire of Gas es Fahr.	mperati Pegre	:5T :i		-27	- 20	- 15	01 -	-5	0	2	o _I	15	20	25	30	33.

Approximate Allowances per Ton Capacity to be made when selecting a Machine for Refrigerating Purposes.—(Triumph Ice Machine Company.)

Beer wort: 15 barrels per ton on Baudelot cooler. One thousand gallons of sweet water per ton from 70° to 40°. Six beeves, 600 to 700 lbs. each, per ton. Ten to twenty hogs. per ton. One thousand cubic feet of space per ton for small machines up to 2 tons. Four thousand cubic feet of space per ton for machine from 10 to 15 tons. Ten thousand cubic feet of space per ton for larger machines used for general purposes.

The above will serve as a guide, but it must be borne in mind that the climate, construction, and exposure of buildings that are to be refrigerated, character of the insulation, management and method of handling work, all have to be taken into consideration. (See also Section

on Cold Storage.)

CONDENSERS.

On the efficiency of the condenser largely depends the economical working of the machine. Condensers are of two kinds or classes, viz. the submerged and the open air, or atmospheric, the latter being the more economical in the matter of cooling water, but occupying the larger amount of space.

According to Professor Siebel, under average conditions (incoming condenser water 70°, and outgoing condenser water 80°, more or less), for each ton of refrigerating capacity (or for one half-ton of ice-making capacity) 40 square feet of condenser surface, corresponding to 64 running feet of 2-inch pipe, and to 90 running feet of 1½-inch pipe, will be required in a submerged condenser. The amount of cooling water used varies from 3 to 7 gallons per minute per ton ice-making capacity in twenty-four hours. The pipe required in an open air condenser is 40 square feet per ton of refrigerating capacity (or for one half-ton of ice-making capacity), equivalent to 64 running feet of 2-inch pipe, or 90 running feet of 1½-inch pipe. The amount of cooling water used is about 50 per cent. less than with condensers of the submerged type.

Double pipe condensers are made which are claimed to possess the best qualities of both submerged and open air condensers. This condenser consists of a coil made up with one pipe inside another of larger diameter, the cooling water circulating through the internal pipe, and the compressed gas in the annular space or clearance between the two pipes. The gas is thus exposed to the action of both cooling water and the atmosphere.

EVAPORATION OF LIQUIDS .- (Lightfoot.)

Liquid or gas.	Water.	Anhydrous Ammonia.	Sul- phuric ether.	Mythylic ether.	Sulphur diox- ide.	Pictet's liquid.
Specific gravity of vapour, compare with air = 1.000	o·622	0.29	2.54	1.61	2.54	_
	Fahr.	Fahr.	Fahr.	Fahr.	Fahr.	Fahr.
Boiling point a atmospheric pre	t 212°	-37·3°	96°	-10.5	14°	- 2·2°
sure . Latent heat of vapo isation at atmo pheric pressure		900	165	473	182	_
Absolute vapour tensions in lbs, r square inch at different tem-ratures.	r. lbs. — 0° — 0° — 0° — 0° 0·089 0° 0·122 0° 0·254 0° 0·503 0° 0·942 0° 1·685	lbs. ————————————————————————————————————	lbs	lbs. ————————————————————————————————————	lbs.	lbs. ————————————————————————————————————

Table showing Pressure and Boiling Point of some of the Liquids available for Use in Refrigerating Machines.—(Ledoux.)

			`	<u>′</u>							
Tempera- ture of Ebullition.	Tension of Vapour, in pounds per square inch, above Zero.										
Deg. Fabr.	Sulphuric Ether.	Sulphur Dioxide.	Ammonia.	Methylic Ether.	Carbonic Acid.	Pictet Fluid.					
(1)	(2)	(3)	(4) 10·22	(5)	(6)	(7)					
-40	_	_	13.23			-					
-31 -22		5.26	16.95	11.12		_					
-13	_	7.23	21.21	13.85	251.6						
- 4	1.30	9.27	27:04	17.06	292.9	13.5					
5	1.20	11.76	33.67	20.84	340·í	10.2					
14	2.19	14.75	41.28	25.27	393.4	19.3					
23	2.79	18.31	50.01	30.41	453.4	22.9					
32	3.22	22.23	61·85	36.34	520.4	2 6·9					
4 I	4.42	27.48	74.22	43.13	594.8	31.5					
50	5.24	33.26	89.21	50.84	676.9	36.2					
59 68	6.84	39.93	105.99	59.56	766.9	41.7					
	8.38	47.62	125.08	69·35 80·28	864.9	48·1					
77 86	10.19	56·39 66·37	146 64	92.41	971·1	55.6					
	12.31	77.64	197.83	92.41	1207.9	64.1					
95 104	17.59	90.32	227.76	=	1338.3	73·2					

TABLE OF SPECIFIC GRAVITIES AND PERCENTAGE OF AMMONIA.—(Carius.)

Degrees Beaumé.	Specific Gravity.	Percentage.	Degrees Beaumé.	Specific Gravity.	Percentage.
10	1.000	O	21	0 9271	19.1
11	0.9929	1.8	22	0 921	21.4
12	0.9859	3.3	23	0.912	23.4
13	0.979	5.0	24	0.000	25.3
14	0.9722	6.7	25	0.0032	27.7
15	0.9655	8.4	26*	0.8974	30.1
15 16	0.9589	100	27	0.8917	32.2
17	0.9523	11.9	28	o.886	35.5
17 18	0.9459	13.7	29	0.8802	
19	0.9392	15.5	30	o·875	
2Ó	0.9333	17.4	1 1	••	1

^{*} Known by the trade as 29} per cent.

Note.—The specific gravity of pure anhydrous ammonia is .623.

BOILING POINT, LATENT HEAT, ETC., OF ANHYDROUS AMMONIA.—(Redwood.)

at.	Latent He	500 8 493 9 493 9 493 3 493 3 483 4 471 6 471 6 465 4
.tai	Boiling Po.	885.0 993.0 993.0 104.0 113.0 113.0 140.0
ure.	-Эзпко	154 °00 161 °00 168 '10 190 °00 200 '44 242 '50 278 '50 318 40 352 '50
Pressure.	Absolute.	168.70 175.70 182.80 194.80 204.70 215.14 224.40 237.20 333.10 377.20
at.	Latent He	531'5 530'6 530'6 530'6 520'2 522'3 524'3 522'3 521'1 521'1 517'2 517'3
•1ui	Boiling Po	886 400 400 400 400 400 400 400 400 400 40
ure.	Gauge.	56.30 66.33 66.33 67.30 67.30 67.30 88.33 88.33 88.33 89.30 100.30
Pressure.	Absolute.	71'00 74'07 75'00 76'00 76'00 76'00 95'00 95'00 95'00 100'00 116'00 116'03
at.	Latent He	5550.5 549.3 548.0 546.3 546.3 547.3 547.1 547.1 547.1 540.0
.tai	od Pailiog •rdsH °	8.2 10.0 10.0 11.0 11.0 11.0 11.0 11.0 11
ure.	Gauge.	23.33 24.35 27.53 27.53 29.32 39.33 33.32 33.33 33.35 34.35 36.35 36.35 36.35 36.35
Pressure	Absolute.	33.00 33.00 33.00 44.00 44.00 50.00
.16	Latent He	579.7 579.1 579.1 575.3 573.3 573.3 573.3 568.9 568.9 567.0 567.0 567.0 567.0 567.0
.tai	od gniliod .nds4 °	1 1 1 2 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
Pressure.	Gsuge.	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
Pres	Absolute.	10.69 12.33 13.00 14.13 14.70 15.00 16.71 16.71 16.71 16.72 19.00 22.99 21.27 22.21 22.23

BOILING POINT, LATENT HEAT, EIC., OF ANHYDROUS AMMONIA.—(Redwood.) (Continued.)

Boiling Point. o Fabr. Latent Heat,

Latent Heat.

Boiling Point.

Pressure.

Pressure.

Pressure.

Pressure.

Gauge.

bsolute.

Gauge.

bsolute.

Latent Heat.

Boiling Point.

Gauge.

psolute.

Latent Heat.

Boiling Point.

Gange.

bsolute.

SOLUBILITY OF AMMONIA IN WATER AT DIFFERENT TEMPERATURES.—(Sims.)

Degrees Fahr.	Sb. of NH ₃ to 1 lb. of Water.	Volume of NH ₃ in 1 Volume of Water.	Degrees Fahr.	Sb. of NH ₃ to 1 lb. of Water.	Volume of NH ₃ in 1 Volume of Water.
32·0 35·6 39·2 42·8 46·4 50·0 53·6 57·2 60·8 64·4 68·0 71·6 75·2 78·8 82·4 86·2 93·2 96·8 100·0 107·6 111·2 111·8	0·899 0·853 0·809 0·765 0·724 0·684 0·646 0·611 0·578 0·546 0·518 0·490 0·407 0·426 0·408 0·378 0·363 0·378 0·363 0·350 0·315 0·326 0·315	1,180 1,120 1,062 1,005 951 898 848 802 759 717 683 643 613 585 559 536 516 496 478 459 444 399 386	125.6 129.2 132.8 136.4 140.0 143.6 147.2 150.8 154.4 158.0 161.6 165.2 168.8 172.4 176.0 179.6 183.2 186.8 190.4 194.0 201.2 204.8 208.4	0·274 0·265 0·256 0·247 0·238 0·229 0·220 0·211 0·202 0·194 0·186 0·178 0·170 0·162 0·154 0·146 0·138 0·130 0·122 0·114 0·106 0·098 0·090 0·082	359 348 336 324 312 301 389 277 265 254 244 234 222 202 192 181 170 160 149 139 128 118 107
122.0	0.584	373			

THE FORECOOLER.

This is a supplementary condenser through which the compressed ammonia passes before reaching the main condenser, and cooled by the overflow water from the latter. If composed of one coil, it should be the same size as discharge pipe from compressor; if of a number of coils, the manifold pipe, and the aggregate area openings of small pipes, should be equal to that of the discharge pipe.

SOLUBILITY OF AMMONIA IN WATER AT DIFFERENT TEMPERATURES AND PRESSURES.—(Sims.)

1 lb. of water (also unit volume) absorbs the following quantities of ammonia:—

Absolute Pressure	32°	F.	68°	F.	104	° F.	212	· F.
in lbe. per sq. in.	lbs.	vols.	lbs.	vols.	lbs.	vols.	grms.	vols.
14.67 15.44 16.41 17.37 18.34 19.30 20.27 21.23 22.19 23.16 24.13 25.09 20.06 27.02 27.99 28.95 30.88 32.81 34.74 36.67	0·899 0·937 0·936 1·029 1·077 1·126 1·283 1·336 1·388 1·442 1·496 1·549 1·556 1·758 1·861 1·966	1·180 1·231 1·287 1·351 1·414 1·478 1·615 1·685 1·754 1·823 1·965 2·034 2·175 2·309 2·444 2·582 2·718	0·518 0·535 0·556 0·574 0·594 0·013 0·632 0·651 0·669 0·685 0·702 0·741 0·761 0·842 0·842 0·881 0·919	0.683 0.703 0.730 0.734 0.781 0.805 0.835 0.835 0.878 0.948 0.924 0.924 0.924 1.106 1.157 1.207	0·338 0·349 0·363 0·378 0·391 0·404 0·415 0·425 0·434 0·463 0·472 0·479 0·486 0·493 0·511 0·530 0·555	0.443 0.458 0.476 0.496 0.513 0.531 0.5543 0.570 0.584 0.596 0.609 0.619 0.629 0.647 0.671 0.696 0.718	0.074 0.078 0.088 0.088 0.092 0.096 0.101 0.115 0.125 0.130	0·97 0·102 0·103 0·115 0·120 0·126 0·139 0·140 0·151 0·157 0·177
38·60 40·53		::	0.992	1.302	o·579 o·594	o·764 o·780	::	::

SOLUBILITY OF AMMONIA IN WATER AT DIFFERENT TEMPERATURES.—(Roscoe.)

Degrees Celsius.	Degrees Fahrenheit.	lbs. of NHs to 1 lb. of Water.	Degrees Celsius.	Degrees Fahrenheit.	lbs. of NH ₃ to 1 lb. of Water.
0	32·0	0·875	8	46·4	0·713
2	35·6	0·833	10	50·0	0·679
4	39·2	0·792	12	53·6	0·645
6	42·8	0·751	14	57·2	0·612

SOLUBILITY OF AMMONIA IN WATER AT DIFFERENT TEMPERATURES.—(Roscoe.) (Continued.)

Degrees Celsius.	Degrees Fahrenheit.	lbs. of NH ₃ to 1 lb. of Water.	Degrees Celsius.	Degrees Fahrenheit.	lbs. of NH ₃ to 1 lb. of Water.
16 18 20 22 24 26 28 30 32 34	60·8 64·4 68·0 71·6 75·2 78·8 82·4 86·0 89·6 93·2	0·582 0·554 0·526 0·499 0·474 0·449 0·426 0·403 0·382 0·362	36 38 40 42 44 46 48 50 52 54 56	96·8 100·4 104·0 107·6 111·2 114·8 118·4 122·0 125·6 129·2 132·8	0°343 0°324 0°307 0°290 0°275 0°259 0°244 0°229 0°214 0°200 0°186

STRENGTH OF LIQUOR AMMONIA.

Percentage of Ammonia by Weight.	Specific Gravity.	Degrees Beaumé, Water, 10.
0	1.000	10.0
2	0.986	12.0
1	0.979	13.0
4 6	0.972	14.0
8	0.966	15.0
10	0.960	16·o
12	0.953	17.1
14	0.945	18.3
16	0.938	19.5
18	0.931	20.7
20	0.925	21.7
22	0.919	22.8
24	0.913	23.9
26	0.907	24.8
28	0.902	25.7
30	0.897	26.6
32	0.892	27.5
34	0.888	28.4
36	o·884	29.3
38	0.880	30.3
	!	

YIELD, ETC., OF ANHYDROUS AMMONIA FROM AMMONIA SOLUTIONS.—(Redwood.)

s	OLUTION	•	ANI	HYDROUS	6 АММО	VIA.
Weight	of Ice.		32° Fahr., pressure) the Solu-	Į,		
Degrees Beaumé.	lbs. per Gallon.	Boiling Point.	Volume of Gas (at 32° I and Atmospheric press in one volume of the tion.	lbs. in one gallon of the Solution.	Per cent, by Volume.	Per cent, by Weight.
34·7 32·8 31·0 29·0 27·2 26·0 25·6 23·7 22·2	7.09 7.17 7.25 7.34 7.42 7.48 7.50 7.59 7.67	26° 38° 50° 52° 74° 83° 86° 98°	494 456 419 382 346 320 311 277 244	3.077 2.841 2.610 2.379 2.156 1.993 1.726 1.520	59.5 54.9 50.7 46.0 41.7 38.5 37.5 33.4 29.4	43.4 39.6 36.0 32.5 29.1 26.6 25.8 22.8

TEMPERATURES TO WHICH AMMONIA GAS IS RAISED BY COMPRESSION.

Temperature	Absolute Con-	AB	SOLUTI	E SUCT	TION F	RESSU	RE.
of Suction.	densing Pressure.	20	25	30	35	40	45
o° Fahr.	90	199	165	138	116	98	83
	100	216	181	153	131	113	97
	110	232	196	166	145	120	109
	120	245	211	181	158	138	121
	130	261	222	193	169	150	132
	140	273	235	205	181	161	143
	150	285	246	216	191	171	153
	160	296	257	226	202	181	163
	, ,		l	į		ļ	

TEMPERATURES TO WHICH AMMONIA GAS IS RAISED BY COMPRESSION.—(Continued.)

Temperature	Absolute Con-	AB	SOLUT	E SUC	TION I	PRESSU	RE.
of Suction.	densing Pressure	20	25	30	35	40	45
5° Fahr.	90	266	172	145	123	104	89
	100	223	186	160	138	119	103
	110	239	203	174	151	132	115
	120	254	218	188	163	145	127
	130	268 281	230	200 212	176 188	156	139
	140 150	293	242 254	212	198	167 178	150 160
	160	305	265	234	209	188	170
10° Fabr.	90	213	178	151	129	011	96
10 1 11111	100	231	195	167	144	125	100
	110	247	210	181	158	139	122
	120	261	226	195	171	151	134
	130	275	237	207	183	163	145
	140	289	250	219	195	174	156
	150	301	262	231	205	185	167
	160	313	273	24 I	216	195	176
15° Fahr.	90	22[185	158	135	117	101
	100	238	202	173	151	131	115
	011	254	217	188	164	145	128
	120	269	233	202	178	158	140
	130	283	245	214	191	170	152
	140	297	257	226	202	181	163
	150	309 321	269 281	238 249	213	192 202	173 183
20° Fahr.	90	228	192	164	141	123	106
20 Tam.	100	245	200	180	157	137	121
	110	202	224	195	171	150	134
	120	277	240	209	185	164	146
	130	291	252	222	197	176	158
	140	305	265	234	209	188	169
	150	317	277	245	22Ó	198	18ó
	160	329	288	256	230	209	190
25° Fahr.	. 90	235	199	171	148	129	111
	100	252	216	187	163	144	127
	110	269	230	200	178	155	140
	120	284	247	216	191	171	153
	130	299	259	229	204	183	165
	140	313	27 I 284	241	216	191	176
	150 160	325	204 296	253 264	227	205 216	187
	100	338	290	204	237	210	197

TEMPERATURES TO WHICH AMMONIA GAS IS RAISED BY COMPRESSION.—(Continued.)

Temperature	Absolute Con-	ABS	SOLUTE	SUCT	ION P	RESSU	RE.
of Suction.	densing Pressure.	20	25	30	35	40	45
30° Fahr.	90	242	206	177	154	134	118
•	100	260	223	193	170	150	133
	110	277	239	208	184	164	147
	120	292	255	223	198	177	159
	130	307	267	236	211	190	17í
	140	321	280	248	223	201	183
	150	334	292	260	234	212	193
	160	346	304	271	245	223	203
. 32° Fahr.	90	245	209	179	157	137	121
	100	263	225	196	173	153	135
	110	280	241	211	187	167	149
	120	295	256	226	201	180	162
	130	310	270	239	213	192	174
	140	324	283	251	226	204	185
	150	337	295	263	237	215	196
1	160	350	307	274	248	226	206
35° Fahr.	90	249	213	182	160	141	124
	100	268	229	200	176	156	139
	110	286	246	215	191	170	153
	120	300	260	230	205	184	166
	130	315	274	243	217	196	178
	140	329	288	255	230	208	189
	150	341	3co	268	241	219	200
	160	354	312	279	252	230	210

THE ANALYSER.

The analyser is placed in upper part of still or generator of absorption machine, and serves as a dehydrator, also increasing temperature of rich liquor from 150° to 170°, at which it arrives, to about 200°.

The device consists essentially of superimposed shelves down which the rich ammonia liquor is delivered and over which it trickles, whilst the heated vapour from generator passes over them in an upward direction. In this manner

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- 50	154 11	£54.70	1759	0.0272	133.41
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- 95	195:37	455 29	1-48	0-277	183-67
+100	215-14	451.50	1.30	0-279	200.44
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VOLUME OF ONE POUND OF ALMONIA GAS AT VARIOUS PRESSURES AND TEMPERATURES.

	01	15	50	25	30	35	
		Volume in (Cubic Feet of (Volume in Cubic Feet of One lb. of Ammonia Gas.	nonia Gas.		
23	20.036	20.263	20.490	20.703	20.930	21.156	21.37
75	19.382	109.61	13.851	20.02	20.246	50.466	20.672
69	692.81	18.982	19.194	19.410	209.61	618.61	20.019
66	18.193	18.399	18.605	18.799	19.005	112.61	19.405
63	12.651	17-865	18.051	18.239	18.439	18.639	18.828
16.958	17.141	17.355	17.529	112.21	906.41	101.81	18.283
181	16.658	16.847	17.036	17.215	17.403	165.21	17.769
620	16.202	16.386	16.570	16.743	926.91	011.21	17.283
12.602	15.770	15.949	16.128	16.296	16.475	16.654	16.824
96	15.360	15.534	15.209	15.873	16.047	16.522	16.386
115	14.61	15.141	15.311	15.471	15.642	118.51	126.51
144	14.600	14.771	14.932	15.088	15.52	15.420	15.226
- 96	14.549	14.410	14.572	14.725	14.887	15.049	15.201
13.763	13.612	14.070	14.228	14.377	14.535	14.693	14.843
147	13.594	13.747	13.301	14.047	14.201	14.356	14.501
13.143	13.285	13.436	13.288	13.730	13.881	14.032	14.174
351	12.993	13.141	13.288	13.428	13.576	13.723	13.863
226	12.712	12.857	13.001	13.137	13.286	13.427	13.263
015	12.444	12.585	12.727	158.21	13.004	13.144	13.277
12.055	12.186	12.325	12.464	12.594	12.733	12.872	13.005
=	11.939	12.075	12.211	12.339	12.473	119.21	12.73

PRESSURES AND TEMPERATURES. ONE POUND OF AMMONIA GAS AT VARIOUS -(Continued. Q VCLUME

11.783 11.365 11.363 11.154 10.959 10.770 10.588 10.412 120.01 9.762 9.467 9.055 40 11.664 644.11 11.242 11.042 10.662 10.482 10.307 10.139 9.975 9.817 9.515 FAHRENHEIT. 12.227 11.755 11.538 11.325 11.120 10.922 10.731 10.547 10.368 10.196 9.867 111.6 9.559 9.412 9.269 9.132 8.997 8.866 Volume in Cubic Feet of One lb. of Ammonia Gas. 30 11.857 1.412 1.202 10.803 10.432 616.6 9.759 9.454 9.309 9.168 666.01 8.899 DEGREES. 23 11.735 9.816 9.816 9.558 9.505 9.356 11.294 11.085 10.885 10.691 10.504 9.072 8.938 8.806 8.677 Z 20 TEMPERATURE 11.835 11.604 11.382 11.167 10.962 10.763 10.572 10.386 9.868 9.550 9.399 9.251 601.6 8.838 8.757 8.580 10.921 9.756 9.756 9.757 9.292 9.006 8.870 8.738 8.608 11.042 10.838 10.642 10.452 10.369 11.576 11.135 10.923 10.527 10.340 10.159 9.984 9.981 9.965 9.965 9.979 9.192 8.799 8.799 8.799 8.799 8.799 8.799 8.799 8.799 10.722 20 lbs. per Square Inch Absolute Pressure.

VOLUME OF ONE POUND OF AMMONIA GAS AT VARIOUS PRESSURES AND TEMPERATURES. —(Continued.)

		H	FEMPERATURE	IN	DEGREES, FAH	FAHRENHEIT.		
Square Inch Absolute	ın	oi	15	50	25	30	35	40
1			Volume in C	ubic Feet of Or	olume in Cubic Feet of One lb. of Ammonia Gas.	nia Gas.		
353	8.271	8.361	8.457	8.553	8.643	8.739	8-834	8.925
36	8.155	8.244	8.338	8.433	8.521	919.8	8.711	8.799
363	8.041	8.129	8.222	8.315	8.403	8.496	8.589	8.679
37.	126.4	8.017	8.109	8.201	8.288	8.379	8.471	8.528
373	7.823	2.008	666.4	8.089	8.172	8.265	8.356	8 44
385	612.2	7.803	7.892	7.982	990.8	8.155	8.245	8.326
383	919.4	669.2	2.7.88	7.876	656.2	240.8	8.136	8.219
39	2.516	7.599	2.686	7.774	7.856	7.943	8.030	8.113
393	7.421	7.501	7.587	7.673	7.754	018.2	2.6.2	8.007
40	7.326	2.406	164.2	7.576	7.656	144.7	7.826	2.60
403	7.234	7.313	7.397	7.480	2.260	7.643	7.727	7.806
41	7.144	7.222	7.305	7.388	2.466	7.549	7.632	7.710
413	950.4	7.134	7.215	7.297	7.374	7.456	7.538	19.1
42	126.9	2.00.2	7.129	7.209	7.286	7.366	7.448	7.52
423	6.888	296.9	7.043	7.123	661.2	7.279	7.358	7.43
43	908-9	188.9	6.6.9	7.039	7.113	7.192	7.271	7.34
433	6.727	008.9	6.820	6.957	7.030	7.108	981.4	7.260
44	619.9	6.722	662.9	9.8.9	6,649	7.026	7.103	9/1./
443	6.573	6.645	6.721	6.798	6.870	946.9	7.022	1.094
45	861.9	692.9	6.652	6.721	6.792	6.867	6.943	7.017

Volume of Ammonia Gas at High Temperatures. —(Redwood.)

		TEX	IPERATU	JRE OF C	GAS.	
GAUGE PRESSURE	60°	74°	80°	840	90°	95°
	voi	UME OF	1 LB. OF	GAS IN	CUBIC F	EET.
80 85 90 95 100 105 115 120 125 130 145 140 145 150	3·470 3·292 3·131	3.035 2.900 2.785	2·695 2·590 2·490	2·418 2·333 2·252	2·204 2·134	2·088 2·037
BRITISH THERMAL UNITS "STATEMENT PROPERTIES AND THE STATEMENT OF THE STAT		N H s	PR F S S S S S S S S S S S S S S S S S S		0 30 2010 0 -10 30	CO

Figs. 19 and 20.—Diagrams showing C rves of Latent Heat of Vaporisation (1 lb. each Saturated Vapour), and Curves of Absolute Pressure for Saturated Vapours of NH3, SO₂, and CO₂, from -40° to +100° Fahr. 1 lb. each Saturated Vapour.—(Murray, Inst. Engrs. and Shipbuilders, Scotland, 1897.)

WOOD'S TABLE OF SATURATED AMMONIA. (Re-ealculated by George Davidson, M.E.)

ie.	ntsnemeT I særged	1 33 33 34 36 37	3334	1 2 2 2 3 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
mi bing c foot.	Weight of Lic lbs. per cubi	42.589 42.535 42.483 42.427 42.391	42.337 42.301 42.265 42.213 42.176	42.052 42.052 42.000 41.946 41.893
ni noot o	Weight of Var lbs. per cubi	0.0410 0.0421 0.0433 0.0444 0 0457	0.0469 0.0482 0.0495 0.0507	0.0535 0.0549 0.0563 0.0577
nid per	Volume of Liq	0.02348 0.02351 0.02354 0.02357 0.02359	0.02362 0.02364 0.02366 0.02368 0.02371	0.02374 0.02378 0.02381 0.02384 0.02387
our per	Volume of Vap	24.388 23.735 23.102 22.488 21.895	21.321 20.763 20.221 19.708 19.204	18.693 18.225 17.759 17.307 16.869
sation,	Heat of Vapori	579.67 579.07 578.42 577.88 577.27	576.68 576.08 575.48 574.89 574.39	573.69 573.08 572.48 571.89 571.28
	Gauge Press lb. per sq. ir	- 4.01 - 3.70 - 3.38 - 3.06	-2.39 -1.68 -1.32 -0.95	-0.57 -0.17 +0.22 +0.63 +1.05
sure lute,	Lbs. per sq. inch. p.	10.69 11.32 11.64 11.98	. 12.31 12.66 13.02 13.38	14.13 14.53 14.92 15.33
Pressure Absolute.	Lbs. per sq. foot. P.	1539'90 1584'43 1630'03 1676'71	1773'43 1823'50 1874'73 1927'17	2035.69 2091.83 2149.23 2207.94 2267.97
rature.	Absolute.	420.66 1 2 3	425.66 6 7 8 8	430·66 1 2 3 4
Temperature.	Degrees F.	1 33 33 36 36 36 36	-35 33 31 31 31	0 6 8 8 8 8 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9

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1	ni binpi Jook sid	Weight of L lbs. per cal	41.858	41.754	41.649	41.615	41.511	41.410	41.37.4	41.322	41.271	41.237	+
·	mi moq	Weight of Va	†290.0 8090.0	01:90.0	2 290.0	6890.0	0.0725	0.0742	0.0440	86//00	0.0818	0.0838	0.0020
`.m	quid per	Volume of Lic	0.02389	0.02395	0.02401	0.02403	0.02400	0.02411	11760.0	0.02420	0.02423	0.02425	0.02420
AMMONIA.	com ber	Volume of Va	16.446	15.633	14.875	14.50,	12.807	13.475	.5.5.	12.527	12.230	11.939	11.059
SATURALED		Heat of Vapor thermal unit	570.68	569.48	508.27	29.295	202.00	565.85	505 65	504 04	563.43	562.82	562.21
OF SALU	sure, nch.	Gauge Pres lb. per sq. i	+ 1.47	33.	3.27	+3.75	4.54	5.54	5.75	40.56	7.38	7.94	8.52
WOOD'S IABLE	ure ıte,	Lbs. per sq. inch. &	21.91	17.05	17.50	18.45	18:94	19.94	20.40	50.08	22.08	55.64	23.52
WOOD'S	Pressure Absolute.	Lbs. per sq. foot. P.	2329.34	2456.23	2520.45	2657.23	2727.17	2871.61	21.0162	3022.31	31000/	3260.52	3343.29
	rature.	Absolute.	435.66	· ~	∞ o	99.044	-	м w	4	445.66	7.0	-∞	6
	Temperature	Degrees F.	-		22		61	17		15			

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ure.	rreqmeT essrgeU	0 6% 7.9	74881	0 1 4 2 4
ni biupi Lood sie	Weight of L lbs. per cul	41.135 41.084 41.034 41.000 40.950	40°900 40°845 40°799 40°749 40°700	40.650 40.601 40.551 40.502 40.453
ni ruoq riool sid	Weight of Va lbs. per cub	0.0878 0.0899 0.0921 0.0943 0.0965	0.0988 0.1011 0.1034 0.1058 0.1083	0.1107 0.1133 0.1159 0.1186 0.1212
red per	Volume of Lic	0.02431 0.02434 0.02437 0.02439 0.02442	0.02445 0.02448 0.02451 0.02454	0 02461 0 02463 0 02466 0 02469 0 02472
t. v.	Volume of Vap	11.385 11.117 10.860 10.604 10.362	9.894 9.669 9.449 9.234	9.028 8.825 8.630 8.436 8.250
	Heat of Vapor thermal unit	561.61 560.99 559.78 559.77	558.56 557.94 557.33 556.73 556.11	555.50 554.88 554.27 553.65 553.04
sure, nch.	Gauge Pres	+ 9.10 9.70 10.31 10.94 11.57	+ 12.22 12.89 13.56 14.25	+15.67 16.40 17.14 17.90 18.68
ire ite.	Lbs. per sq. inch. \$.	23.80 24.40 25.01 25.64 26.27	26.92 27.59 28.26 28.95 29.65	30.37 31.10 31.84 32.60 33.38
Pressure Absolute,	Lbs. per sq. foot. P.	3427.75 3513.97 3601.97 3691.75 3783.37	3876·85 3972·62 4069·48 4168·70 4269·90	4373.10 4478.32 4485.60 4694.96 4806.46
ature.	Absolute.	450.66 2 3	455.66 7 8 8	460·66 1 2 3 4
Temperature	Degrees F.	0 6 8 7 9	N4881	+ 0 = 4 W 4

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ni bing toot 5	Weight of Lic lbs. per cubi	40.404	40.274 40.274 40.225	40.160 40.064 40.064 40.016 39.968	39.920 39.872 39.777 39.729
ni ruoo .1001 o	Weight of Vai	0.1240	0.1324	0.1383 0.1413 0.1444 0.1474 0.1507	0.1541 0.1573 0.1607 0.1641 0.1676
uid per	Volume of Liq.	0.02475	0.02483	0.02490 0.02493 0.02496 0.02499	0.02505 0.02508 0.02511 0.02514 0.02517
our per	Volume of Vap	8.070	7.553	7.229 7.075 6.924 6.786 6.632	6.491 6.355 6.222 6.093 5.966
noites.	irogsV do 189H etinu lsmrədt	552.43	550.58 549.56	549.35 548.73 548.11 547.49 546.88	546.26 545.63 545.01 544.39 543.74
Gauge Pressure, lb. per sq. inch.		+ 19.46	21.93	+23.64 24.53 25.43 26.34 27.28	+28·24 29·20 30·18 31·19 32·21
ure ute.	Lbs. per sq. inch. \$.	34.16	36.63	38.34 39.23 40.13 41.04 41.98	42.94 43.90 44.88 45.89 46.91
Press	Lbs. per sq. .9. foot.	4920.11	5274.28 5274.28 5396.83	5521.71 5649.48 5778.50 5910.52 6044.96	6182°00 6321°24 6463°24 6607°77 6754°90
rature.	Absolute. T	465.66	~ % 6	470.66 1 2 3 3	475.66 6 7 8 9
Тепре	Degrees F.	+ 65	~∞ o	+ 10 11 13 14	+15 16 17 18
	sation, "" "" "" "" "" "" "" "" ""	Absolute. Lbs. per sq. foot. P. Lbs. per sq. inch. p. Thermal units. A. Weight of Vapour per Thermal units. A. Weight of Vapour in The per sq. inch. The pe	Absolute. Absolute. Libs. per sq. Lips. per cubic feet. Thermal units. A. Weight of Vapour per Thermal units. A. Thermal	Pressure Absolute. Absolute. Absolute. Absolute. Absolute. Absolute. Absolute. Lbs., per sq., foot. Lbs., per sq. inch., inch., sq. inch. Lbs., per sq. inch. Lbs., per sq. inch. Lbs., per sq. inch. Cauge Pressure. Lbs., per sq. inch. Lbs., per sq. inch. Cauge Pressure. Acieght of Vapour per thermal units. A. Weight of Vapour in lbs. per cubic foot. Apper sq. inch. Cauge Pressure. Cauge Presu	Emperature. Absolute. Liba. per sq. Liba. per sq. Liba. per sq. Ciauge Presente. Absolute. Ciauge Presente. Absolute. Ciauge Presente. Absolute. Ciauge Presente. Absolute. Ciauge Presente. Apper sq. Theat of Vapour per tipe to Vapour in the cubic feet. Apper sq. Apper

Wood's Table of Saturated Ammonia.—(Continued.)

Temperature.	rature.	Pressure Absolute,	ire ite.		ation,	nt per	id per	ni Tuo 3001 :	ni bin .1001 :	•
Degrees F.	Absolute.	Lbs. per sq.	Lbs. per sq.	Gauge Pressi lb. per sq. in	Heat of Vaporis.	Volume of Vapo lb: cubic feet,	Volume of Liqu lb, cubic feet.	Weight of Vap lbs. per cubic	Weight of Liq lbs. per cubic	Temperatur Degr <i>ees</i> F
+ 20	480.66	6904.68	47.95	+33.25	543.15	5.843	0.02520	0.1711	39.682	+
21	-	7057.15	10.64	34.31	542.53	5.722	0.02523	0.1748	39.635	2
22	8	7211.33	60.05	35.39	541.90	5.605	0.02527	0.1784	39.572	5
23	6	7370.27	81.15	36.48	541.28	5.488	0.02529	0.1822	39.541	21
24	4	7530.96	52.30	37.60	240.66	5.378	0.02533	0.1860	39.479	24
+25	485.66	7694.52	53.43	+38.73	540.03	5.270	0.02536	2681.0	39.432	+ 22
2 1	۰	52.0022	24.29	36.86	539.41	5.103	0.02539	0.1937	39.380	× ;
, v	~~	8030-16	55.70	41.00	538.78	5.058	0.02542	9102.0	39.339	67 6
29	6	8377.56	58.17	43.47	537.53	4.858	0.02548	0.5020	39.246	67
+30	99.064	8555.74	59.42	+ 44.72	16.982	4.763	0.02351	0.5066	39.500	+3
31	_	8736.96	29.09	45.67	536.28	4.668	0.02554	0.2142	39.115	33
32	81	92.1268	61.95	47.25	535.66	4.577	0.02557	0.2185	39.108	32
33	3	12.8016	63.25	48.55	535.03	4.486	0.02561	0.5550	39.047	33
75	4	9299.32	64.58	40.88	534.40	4.400	0.02564	0.2273	30.001	8

WOOD'S TABLE OF SATURATED AMMONIA.—(Continued.)

iure.	snegmeT seergeU	+ 35 36 37 38 39	+ 0 + 4 + 4 + 4 + 4 + 4 + 4 + 4 + 4 + 4 +	+ 45 47 47 48 49 49
ni biupi toot sid	Weight of L lbs. per cul	38.940 38.894 38.850 38.789 38.729	38.684 38.639 38.595 38.550 38.499	38.461 38.417 38.373 38.328 38.284
ni ruoqi Goot	Weight of Value of Va	0.2318 0.2362 0.2413 0.2458 0.2507	0.2554 0.2605 0.2655 0.2706 0.2757	0.2809 0.2863 0.2917 0.2974 0.3027
puid per	Volume of Lic lb, cubic fee	0.02571 0.02571 0.02574 0.02578 0.02582	0.02585 0.02588 0.02591 0.02594	0.02600 0.02603 0.02609 0.02609
	Volume of Var	4.314 4.234 4.157 4.068 3.989	3.915 3.839 3.766 3.695 3.627	3.559 3.493 3.428 3.362 3.303
noitssi.	roqsV do Vapor tinu lsmrədt	533.78 533.13 532.52 531.89 531.26	530.63 529.99 529.36 528.73 528.10	\$27.47 \$26.83 \$26.20 \$25.57 \$24.93
sure,	Gauge Presi lb. per sq. ii	+ 51.22 52.59 53.98 55.39 56.83	+ 58·29 59·78 61·29 62·82 64·38	+ 65.96 67.57 69.20 70.86 72.55
ıre ıle.	Lbs. per sq. inch. 🌶.	65.92 67.29 68.68 70.09 71.53	72.99 74.48 75.99 77.52	80.66 82:27 83:90 85:56 87:25
Pressure Absolute,	Lbs. per sq. foot. P.	9493.07 9690.04 9890.75 10093.91	10511'16 10724'95 10942'18 11162'93 11387'21	11615'12 11846'64 12081'80 12320'71 12563'36
ature.	Absolute.	495.66 6 7 8 8 9	500-66 I 2 3.3	505.66
Temperature.	Degrees F.	+ 35 36 37 38 38	+ 41 43 43	+ 45 46 47 49

WOOD'S TABLE OF SATURATED AMMONIA.--(Continued.)

utsraqmaT I sangaU	+ 50 51 52 53 54 54	+ 55 50 57 58 58 59	+ 61 63 63 63
Weight of Liq lbs. per cubic	38.226 38.167 38.124 38.080 38.037	37.994 37.936 37.893 37.835 37.793	37.736 37.678 37.622 37.579 37.523
Weight of Vap	0.3084 0.3143 0.3201 0.3258 0.3320	0.3380 0.3442 0.3505 0.3568 0.3588	0.3697 0.3762 0.3831 0.3898 0.3968
Volume of Liqu lb. cubic feet.	0.02620 0.02620 0.02623 0.02623	0.02632 0.02636 0.02639 0.02643 0.02643	0.02651 0.02654 0.02658 0.02661 0.02665
Volume of Vapo	3.242 3.182 3.124 3.069 3.012	2.958 2.905 2.853 2.802 2.753	2.705 2.658 2.610 2.565
iroqsV of Vaporistinu lamredt	\$24.30 \$23.66 \$23.03 \$22.39 \$21.76	521.12 520.48 519.84 519.20 518.57	517.93 517.29 516.65 516.01 515.37
Gauge Press lb. per sq. in	+74.26 77.76 79.55 81.37	+83.22 85.10 87.00 88.94 90.90	+92.89 94.91 96.96 99.05 101.16
Lbs. per sq. inch. A.	88.96 90.70 92.46 94.25 96.07	97.92 99.80 101.70 103.64 105.60	107.59 109.61 111.66 113.75 115.86
Lbs. per sq.	12809.91 13080.21 13314.43 13572.52 13834.64	14100.74 14370.92 14645.18 14923.98 15206.28	15493.09 15784.23 16079.67 16379.51 16683.75
Absolute.	510·66 1 2 3 3	515.66 6 7 8 8	520.66 1 2 3 3
Degrees F.	+ \$52 \$3 \$4	+ 55 57 59 85 89	+60 61 63 64
	Absolute. Lbs. per sq. foot. P. Lbs. per sq. linch. A. Cauge Press lb. per sq. in thermal units Weight of Vapori Db. cubic feet. Volume of Vapori thermal units Toulouse of Lid lbs. per cubic sw. Weight of Lid lbs. per cubic sw. Temperatur	2 1 13080.21 90.70 1289.90	Absolute. 510-66 12809.91 88.96 +74.26 524.30 3.242 0.02616 0.3084 38.226 1.3080.21 90.70 7.776 522.39 3.242 0.02622 0.3143 38.124 0.02622 0.3268 38.080 0.3242 0.3261 38.037 0.3201 38.037 0.3201 38.037 0.3201 38.037 0.3201 38.037 0.3201 38.037 0.3201 38.037 0.3201 38.037 0.3201 38.037 0.3201 38.037 0.3201 38.037 0.3201 38.037 0.3201 38.037 0.3202 0.3202 0.3380 0.3202 0.3202 0.3380 0.3202 0.3380 0.3202 0.3380 0.3202 0.3380 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.3202 0.

WOOD'S TABLE OF SATURATED AMMONIA. -- (Continued.)

	Тетрегаtи Гевгеез Г	+ 65 66 68 69	+ 70 17 72 73 74	+ 75 77 78 79
ni bin tool a	Weight of Liq lbs. per cubi	37.481 37.439 37.383 37.341 37.285	37.230 37.188 37.133 37.079 37.037	36.995 36.954 36.900 36.845 36.805
ni ruo toot o	Weight of Vap lbs. per cubi	0.4039 0.4110 0.4189 0.4254 0.4329	0.4401 0.4479 0.4558 0.4645 0.4712	0.4791 0.4873 0.4957 0.5012 0.5123
uid per	Volume of Liquible feet.	0.02668 0.02671 0.02675 0.02678 0.02682	0.02686 0.02689 0.02697 0.02700	0.02703 0.02706 0.02710 0.02714 0.02717
our per	Volume of Vape lb. cubic feet	2.476 2.433 2.389 2.351 2.310	2.272 2.233 2.194 2.153 2.122	2.087 2.052 2.017 1.995 1.952
aciion,	Heat of Vapori thermal units	514.73 514.09 513.45 512.81 512.16	511.52 510.87 510.22 509.58 508.93	508·29 507·64 506·99 506·34 505·69
	Gauge Press lb. per sq. in	+ 103'33 105'48 107'68 109'92 112'16	+ 114'49 116'84 119'20 121'61 124'04	+126.52 129.02 131.56 134.14 136.75
ure ute.	Lbs. per sq. inch. 🎤.	118°03 120°18 122°38 124°62 126°89	129.19 131.54 133.90 136.31	141.22 143.72 146.26 148.84 151.45
Pressure Absolute,	Lbs. per sq. foot. P.	16992°50 17305°70 17623°45 17945°89 18272°81	18604.53 18941.00 19282.21 19628:32 19979:22	20335·16 20696·00 21061·85 21432·82 21808·85
ature.	Absolute. T	525.66 6 8 8 8	530.66 1 2 3 3	535.66 6 7 8 8
Temperature	Degrees F.	+ 65 67 69 69	+ 7 0 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	+ 77.77

WOOD'S TABLE OF SATURATED AMMONIA.—(Continued.)

	1		
Temperatu Degrees	+ 82 83 83 84	+ 865 87 89 89	+ 8 2 2 2 2 4 2 4 4 4 4 4 4 4 4 4 4 4 4 4
Weight of Lid	36.751 36.696 36.657 36.603 36.549	36.509 36.456 36.407 36.350 36.311	36.258 36.219 36.166 36.114 36.075
Weight of Var lbs. per cubi	0.5205 0.5294 0.5382 0.5473 0.5558	0.5649 0.5744 0.5834 0.5927 0.6024	0.6120 0.6219 0.6317 0.6418 0.6518
Volume of Liq lb, cubic feet	0.02721 0.02725 0.02728 0.02732	0.02739 0.02743 0.02747 0.02751	0.02758 0.02761 0.02765 0.02769
Volume of Vap lb. cubic feet	1.921 1.889 1.858 1.827 1.799	1.770 1.741 1.714 1.687 1.660	1.634 1.608 1.583 1.558 1.558
Heat of Vapori stinu lamredt	505.05 504.40 503.75 503.10 502.45	501-81 501-15 500-50 499-85 499-20	498.55 497.89 497.24 496.59 495.94
Gauge Press lb. per sq. in	+139.40 142.08 144.80 147.56	+ 153.18 156.05 158.96 161.91	+ 167.92 1,70.99 174.09 177.24 180.43
Lbs. per sq. inch. \$.	154.10 156.78 159.50 162.26 165.05	167.88 170.75 173.66 176.61 179.59	182.62 185.69 188.79 191.94 195.13
Lbs. per sq. Goot.	22190.15 22576.51 22968.88 23365.38 23767.81	24175.61 24588.92 25co7.80 25432.16 25862.14	26297-88 26739-88 27186-56 27639-43 28098-26
Absolute. T.	540.66 1 2 3 3	545.66 6 7 8 9	550.66 1 2 3 4
Degrees F.	+ 80 81 82 83 84	+ 85 86 87 88 89	+ 92 93 94
	Absolute. L.bs. per sq. foot. P. inch. A. Libs. per sq. libs. per sq. b. per sq. Thermal units Weight of Vaport b. cubic feet lbs. per cubi	22066 22190.15 1	Absolute. Absolute. 1. Lbs. per sq. 1. Lbs. per sq. 1. Lbs. per sq. 2. 22556.51 2. 22556.51 2. 22556.51 2. 22556.51 3. 3 23365.38 4. 4 23767.81 1.50.52 1.50.52 1.70 1

WOOD'S TABLE OF SATURATED AMMONIA.—(Continued.)

.ar	Temperatu Degrees I	+ 99 99 100 100
ai bing Loot o	Weight of Lic lbs. per cubi	36.023 35.971 35.881 35.881 35.881
ni moo	Weight of Vap lbs. per cubi	0.6622 0.6729 0.6835 0.6934 0.7047
uid per	Volume of Liq.	0.02776 0.02780 0.02784 0.02791 0.02791
our per	Volume of Vap	1.510 1.486 1.463 1.442 1.419
noitses.	iroqsV de Vapori estinu lamrəds	495.29 494.63 493.97 493.32 492.66
ure, ich.	Gauge Press lb. per sq. in	+ 183.65 186.92 190.24 193.59 196.98 + 200.42
iure ute,	Lbs. per sq. inch. p.	198'35 201'62 204'94 208'29 211'68
Pressure Absolute.	Lbs. per sq. foot. P.	28563.00 29033.86 29510.69 29993.52 30482.52
rature.	Absolute. T.	555.66 6 8 8 9 9
Temperature	Degrees F.	+ 95 96 97 98 99 + 100

TABLE SHOWING REFRIGERATING EFFECT OF ONE CUBIC FOOT OF AMMONIA GAS AT DIFFERENT CONDENSER AND SUCTION (BACK) PRESSURE IN B. T. UNITS.-

(Professor Siebel, " Compend of Mechanical Refrigeration.")

				-		_	_										
	105		218		25.05	30.94	33.82	38.80	44.35	50.40	56.50	63.10	92.69	78.31	98.48	97.73	106.49
	8	-á	, 8		25.30	31.30	34.20	39.23	44.84	96.09	57.12	63.80	70.53	21.62	18.88	62.86	107.64
Ei	8	er souare inc	184		25.29	31.64	34.58	39.62	45.34	51.52	57.75	64.49	62.12	80.02	26.68	99.85	62.801
ın Degrees	8.	auge) Ibs. po	168		25.87	31.99	34.60	40.10	45.83	52.08	58.37	61.59	22.06	80.88	22.06	16.001	109.94
Temperature of the Liquid in Degrees F.	85	Corresponding Condenser Pressure (Gauge) lbs. per square inch.	153		91.92	32.34	35.34	40.24	46.33	52.64	29.00	65.88	72.82	81.73	89.16	26.101	60.111
mperature o	&	Condenser	139		56.44	32.70	35.72	40.62	46.82	53.20	29.65	92.99	73.59	82.59	92.63	103.03	112.24
Te	22	rresponding	127		26.73	33.04	36.10	41.41	47.32	53.76	52.09	67.27	74.35	83.44	63.26	104.09	123.39
	6	ပိ	115		10.72	33.40	36.48	48.14	18.44	54.32	28.09	26.29	75.12	84.30	94.24	105.15	114.54
	. 65		103		27.30	33.74	36.36	42.58	48.31	54.88	61.50	99.89	75.88	85.15	95.20	100.51	69.511
•9.	gaibao Tessur sq. in.	d noite	ons	G. Pres.	-	4	9	6	13	91	20	24	200	33	39	45	51
sst	o 10 91 .H 899	peratu 139U t	məT ii		-27	- 20	-15	011	1 5	0	2	0	15	20	25	30	35

USEFUL EFFICIENCY OF AMMONIA.

(Denton and Schroeter.)

No. of	Temperature in Degrees Fahr. Corresponding to Pressure of Vapour.		See Melting Capacity per Pound of Coal, assuming Three Pounds per Hour per Horse-power.		
Test.	Con- denser.	Suction.	Theoretical Friction • included.	Actual.	Per Cent. Loss due to Cylinder Super-heating.
1 2 3 4 24 26 25	72·3 70·5 69·2 68·5 84·2 82·7 84·6	26.6 14.3 0.5 11.8 15.0 -3.2 -10.8	50·4 37·6 29·4 22·8 27·4 21·6 18·8	40·6 30·0 22·0 16·1 24·2 17·5 14·5	19.4 20.2 25.2 29.4 11.7 19.0 22.9

^{*} Friction taken at figures observed in the tests, which range from 14 per cent. to 20 per cent. of the work of the steam cylinder.

LIQUID RECEIVER.

This is a vessel placed between the condenser and the expansion valve to receive and store the liquefied ammonia. The dimensions of the liquid receiver should be sufficient to hold about $\frac{1}{2}$ gallon for each ton of refrigerating capacity in 24 hours. The liquid receiver also serves as an additional oil trap. If, as is sometimes the case, the liquid receiver is intended to act as a storage vessel for all the charge of liquefiable ammonia in the plant in case of repairs, etc., it should be provided with valves, which should not be closed when the receiver is over two-thirds full. Preferably the receiver should be made large enough to contain twice the charge of ammonia to avoid explosions. The receiver is provided with oil and liquid gauges.

TABLE SHOWING EFFICIENCY OF AMMONIA COMPRESSION PLANT UNDER DIFFERENT CONDITIONS.

(Professor Siebel, "Compend of Mechanical Refrigeration.")

NO. OF TEST-	H	8	£	+
Talet des Ella				
Temperature of refrigerated brine Timet, deg. Fall	45.194	20.344	15.952	6/2.0-
Contiet, deg. Fant.	37.054	22.005	0.777	62.04
Specific heat of brine (per unit of volume)	0.8008	0.8508	0.8427	0.8374
Quantity of brine circulated per hour, cubic feet	1039.38	908.84	633.86	414.98
Cold produced, B.T.U. per hour	342.909	263.620	172.776	121.474
Temperature of cooling water in condenser / Inlet, deg. Fahr	48.832	49.426	48.931	49.098
1 cmperature of cooming water in condense (Outlet, deg. t.c. F.	60.724	68.013	67.282	67.267
Quantity of cooling water per hour in cubic feet	338.76	260.83	92. 201	139.66
Heat eliminated by condenser B.T.U. per hour	378.358	301.404	214.796	158.926
I.H.P. in compressor cylinder	13.82	62.41	13.53	86.11
I.H.P. in steam engine cylinder	12.80	16.47	15.58	14.54
Consumption of steam per hour in lbs	311.21	335.98	305.87	278.79
(Per I.H.P. in comp. cyl	24.813	18.471	12.770	10.140
Cold produced per hour B.T.U. Per I.H.P. in steam cyl	21.703	16.026	11.307	8.530
(Per lb. of steam	8.0011	282.6	6.495	435.82

PROPERTIIS OF SATURATED CARBONIC ACID GAS.

(Denton and Jacobus.*)

Density of Vapour or Weight of One Cubic Foot.	2.321 2.323 3.265 3.265 3.365 5.331 6.265 10.356 112.482 115.475
Increase of Volume during Evaporation.	0.4138 0.3459 0.2901 0.2435 0.2042 0.1711 0.1777 0.0960 0.0763 0.0577 0.0391
Heat Equivalent of External Work.	16.20 16.20 15.80 15.80 15.80 15.93 13.93 13.14 12.15 10.91 7.06 7.06
Latent Heat of Evaporation,	136·15 131·65 126·79 121·50 115·70 100:37 94·52 85·64 75·37 46·89 19·28
Heat of Liquid reckoned from 32° Fahr.	137.80 132.51 125.91 120.92 17.60 8.33 17.60 8.40.86 84.44
Total Heat reckoned from 32° Fahr.	98'35 99'14 99'88 100'58 101'81 102'84 103'84 103'84 103'84 103'95
Absolute Pressure in lbs. per sq. in.	2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
Temperature of Ebullition in Degrees Fahr.	1 1 2 4 3 3 3 4 5 4 3 3 3 4 5 4 5 6 5 5 6 6 6 6 6 6 6 6 6 6 6 6 6

* Iransformed to English units from a metric table computed by Prof. Schweter.

SATURATED SULPHUR DIOXIDE GAS.

(Ledoux.)

Density of Vapour or Weight of One Cubic Foot.	lbs.	0.076 9.097 0.123 0.153 0.190 0.232 0.232 0.340 0.407 0.407 0.609 0.750
Increase of Volume during Evaporation.	Cubic Feet.	13.17 1027 8.12 8.12 6.50 6.50 2.93 2.93 2.93 2.93 1.75 1.27 1.09
Heat equivalent of External Work.	B.T.U.	13.59 14.05 14.06 14.46 14.46 14.84 15.01 15.17 15.50 15.71 15.82
Latent Heat of Evaporation.	B.T.U.	176.90 1772.89 170.82 168.73 168.73 166.63 160.23 158.07 153.70 153.70 147.02
Heat of Liquid reckoned from 32° Fahr.	B T.U.	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
Total Heat reckoned from 32° Fabr.	B.T.U.	157.43 158.64 159.84 161.03 161.03 162.20 164.51 165.65 166.90 170.00 171.17
Absolute Pressure in lbs. per sq. in. P+144	lbs.	5.55 9.223 11.76 11.76 11.76 12.53 33.25 33.25 56.36 90.31
Temperature of Ebullition in deg. F.	Deg. Fahr.	2 1 1 2 2 2 4 5 4 5 5 5 5 5 5 5 5 5 5 5 5 5 5

USEFUL EFFICIENCY OF SULPHUR DIOXIDE.

(Schroeter.)

No.	Temperature in Degrees Fahr. corresponding to Pressure of Vapour.		Ice Melting Capacity per Pound of Coal, assuming Three Pounds per Hour per Horse-power.				
of Test.	Condenser.	Suction.	Theoretical Friction • included.	Actual.	Per Cent. Loss due to Cylinder Super-heating.		
11 12 13 14	77·3 76·2 75·2 80·6	28·5 14·4 -2·5 -15·9	41·3 31·2 23·0 16·6	33·1 24·1 17·5 10·1	19.9 22.8 23.9 39.2		

* Friction taken at figures observed in the tests which range from 14 per cent. to 20 per cent. of the work of the steam cylinder.

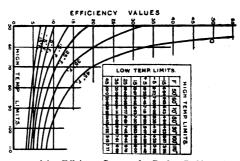


FIG. 21.—Diagram giving Efficiency Curves of a Perfect Refrigerating Machine at Various Limits of Temperature.—(Murray, Inst. of Engrs. and Shipbuilders, Scotland, 1897.)

TABLE SHOWING PROPERTIES OF SATURATED VAPOUR OF ETHER. (Professor Siebel, "Compend of Mechanical Refrigeration.")

Weight in lbs. of one cubic foot.		0.048 0.073 0.107 0.154 0.234 0.294 0.392 0.515 0.705 0.705 1.350
Specific Volume.		0.278 0.844 0.574 0.574 0.287 0.158 0.0120 0.057 0.057
Heat equivalent of external work.	B. T. Units.	30.20 31.80 33.32 33.32 34.68 35.24 35.24 35.68 35.32 37.32
Heat equivalent of internal work.	B. T. Units.	345.80 341.48 336.52 330.88 324.60 317.64 317.64 317.64 291.28 274.48 264.52
to IsaH Vaporisation.	B. T. Units.	376.00 372.48 368.32 368.32 357.94 357.94 357.92 337.20 310.32 320.00 310.32
Total Heat.	B. T. Units.	376.00 393.76 418.00 444.44 460.44 476.00 491.12 505.00 532.76 547.12
Heat of the Liquid.	B. T. Units.	0.00 21.28 44.80 64.56 86.45 88.76 131.20 173.92 176.94 223.44
Pressure in lbs. per square inch.		3.54 8.51 8.51 12.20 17.40 24.32 33.17 44.32 74.96 95.25 119.51
Temperature, Degrees Fahr.		33 88 86 86 86 102 112 115 115 115 115 115 115 115 115 11

The following particulars regarding an ether machine are given * by Mr. Lightfoot as being the result of actual experiments made in this country, and serving to show what may be expected under ordinary conditions:—

Production of ice per twenty-four hours ... 15 tons. per hour .. 1,400 lbs. Heat abstracted in ice-making, per hour ... 245,000 units ** Indicated horse-power in steam cylinder, excluding that required for circulating the cooling water and for working cranes, etc. 83 I.H.P. Indicated horse-power in ether pump ... 461 I.H.P. Thermal equivalent of work in ether pump, 119,261 units ** Ratio of work in pump to work in ice-making I to 2.05 Temperature of water entering condenser 52° Fahr.

Mr. Frederick Colyer, C.E., M.I.C.E., states + that he obtained the following results with a first-class apparatus when testing the working of some of the leading ether machines, viz.: "In an ether machine made by Messrs. Siebe, Gorman and Co., capable of cooling 3,200 gallons of water from 60° down to 50°, or abstracting 320,000 heat units ** per hour, the average experiments gave 4,250 gallons per hour cooled to 10° Fahr. The temperature of the water at the inlet was 54°, and that of the water used for condensing purposes was the same. The maximum cooling effected was 449,437 heat units ** abstracted per hour, being from 35 to 40 per cent. above the nominal power of the machine. The condensing water used per hour was 1,262 gallons, or about 3-10ths of a gallon for every gallon of water cooled. The coal consumed was $3\frac{1}{4}$ cwts. per hour; it was of indifferent quality, or the consumption would have been smaller. The steam cylinder was 21 in. diameter and 27 in. stroke; the air-pump 24 in. diameter and 27 in. stroke. The speed of the engine was 58 revolutions per minute, with 48 lbs. of steam cut off at onethird of the stroke. The indicated power of the engine was 53 horse-power, and of the air-pump 29'2 horse-power. The boiler was 7 ft. diameter and 24 ft. long, and gave an ample supply of steam."

^{* &}quot;Proceedings, Institution of Mechanical Engineers," 1886, p. 214. ** A thermal unit is that amount of heat required to raise the temperature of 1 lb. of water 1° by the Fahr, scale when at 39.4°.

† "Proceedings, Institution of Mechanical Engineers," 1886, p. 248.

Efficiency of Ether Machines.

Output of 15 tons of ice in twenty-four hours. Abstraction of heat per hour, 245,000 B.T.U. Indicated horse-power of engine, 83; of which 46 I.H.P. was used for the ether compressor, balance in pumping water, working cranes, friction, etc. Temperature of cooling water, 52°.

Ice production, about 8:3 tons of ice per ton of coal

consumed.

PICTET'S LIQUID.

Temperature Degrees Fahr.	Pressure (Absolute) in Atmospheres.	Temperature Degrees Fahr.	Pressure (Absolute) in Atmospheres.
-22 -13 -4 -2·2 5 14 23 32	0·77 0·89 0·98 1·00 1·18 1·34 1·60 1·83	50 50 68 77 86 95 104 113 122	2·55 2·98 3·40 3·92 4·45 5·05 5·72 6·30 6·86

FORMULA FOR CALCULATING THE AMOUNT OF AIR DE-LIVERED PER HOUR BY COLD-AIR MACHINES, WHEN THE REVOLUTIONS AND THE SIZE OF THE COMPRES-SORS ARE KNOWN.

(Haslam's Catalogue of " Ice-making and Refrigerating Machinery.")

Air discharged per hour =
$$\frac{A \times N \times 2R \times S \times 60}{1728} \times C$$

Where A =area of each compressor, in inches.

N = number of compressors.

2R = strokes per minute (or twice the revolutions).

60 = minutes per hour.

S = stroke in inches.

 τ_{728} = cubic inches in one foot.

C = factor of efficiency which is taken as o'8 for short strokes, and o'85 for long strokes.

SECTION II.

COLD STORAGE.

COLD storage may be defined as the preservation of perishable articles by keeping them in rooms or chambers maintained constantly at a low temperature by refrigeration; and refrigeration may be defined as the maintenance of any place at a lower temperature than that of the atmosphere.

A most important point in the construction of a cold store is the insulation, and it is almost superfluous to observe that the aim is to render this latter as perfect as possible, so as to afford as great a protection as is practicable against the escape of the cold air from the interior and the transmission of heat from the exterior.

The refrigeration of cold stores may be carried out on the brine circulation system, the direct expansion system, and the air-blast system. In the first, refrigerated or cooled brine is circulated through cooling pipes, or their equivalent, arranged in the cold store; and in the second the ammonia or refrigerating medium is allowed to expand direct in the above pipes. In the third, or air-blast system, air reduced to a low temperature by passing it over cooled pipes or surfaces, or by means of a cold-air machine, is admitted to the store.

The dimensions of cold stores vary, from that of a few cubic feet space, such as those in private houses, hotels, butchers' shops, etc., up to those of several millions of cubic feet. In the case of a large store it is found most advantageous to arrange for the delivery of goods to or from the store to take place from the highest part of the building, as by this means greater obstacles are offered to the transmission of heat from the exterior to the interior

of the store, and also to the escape of the cold air therefrom, which latter, owing to its being heavier than the surrounding atmosphere, and to its consequent tendency to sink to the lowest level, will not escape from above, whilst it does so readily from any open aperture at a lower level.

AMOUNT OF REFRIGERATION REQUIRED.

The refrigeration required will be governed by the size of the store, the amount of and frequency with which the goods are brought into the store and removed from it, the temperature of the goods, and their specific heat, the mean external temperature, the greater or lesser perfection of the insulation, and various other matters, which render it totally impossible to lay down any hard-and-fast rules.

A very usual practice is to provide 1 foot run of 2-inch pipe for every 7 cubic feet of space contained in the store, but sometimes the proportion used is as much as one to five, whilst again it is occasionally reduced to one to twelve. For refrigerating meat, in which case it is not desirable to cool the exterior too rapidly before the interior has had time to cool to a certain extent, the best proportion to employ is one to ten.

Amount of Refrigerating Pipes necessary for Chilling, Storage, and Freezing Chambers.

Chilling-rooms or Chambers, refrigerated on the direct expansion system, I ft. run of 2-in. piping for each 14 c. ft. of space; on the brine-circulation system, I ft. run of 2-in. piping for each 8 c. ft. of space.

Freezing-rooms or Chambers, refrigerated on the direct expansion system, I ft. run of 2-in. piping for each 8 c. ft. of space; on the brine-circulation system, I ft. run for

each 3 c. ft. of space.

Storage-rooms or Chambers, refrigerated on the direct expansion system, I ft. run of 2-in. piping for each 45 c. ft. of space; on the brine-circulation system, I ft. run of 2-in. piping for each 15 c. ft. of space.

THE FOLLOWING TABLE GIVES THE EXTREME LIMITS OF CUBIC FEET OF SPACE PER RUNNING FOOT OF 2-INCH PIPING.—American Practice.

Breweries-Medium insulation.			
Chip and Stock Rooms	• •	• •	I to 22
Fermenting and Settling Rooms	••	• •	I " 20
Packing Rooms			1 ,, 18
Hop Rooms	• •	• •	I " 25
Packing House.			
Chill Rooms for Beef	• •	• •	I ,, I2
Hogs	• •		
Freezing Rooms		• •	1,, 6 or 7
Cold Storage.			
Cold Storage Rooms	••	• •	I ,, 25 or 30
Cold Storage House and Freezin	g Roo	ms	Ι,, 8
For Eggs, brine preferred			I " 12
Cold Storage			I,, 25
Ice Storage			I ,, 20
Fish Freezing (Direct Expansion)			Ι,, 2

The following five tables are given by Prof. Siebel in the "Compend of Mechanical Refrigeration."

LINEAL FEET OF 1-INCH PIPING REQUIRED PER CUBIC FOOT OF COLD STORAGE SPACE.

e of ing in : Feet, or less.	ation.	TEMPERATURE, DEGREES FAHR.						
Siza Buildi Cubic more	Insulation	o ^o .	10°.	20°.	30°.	40°.	50°.	
100	Excellent.	3·o	1.78	o·48	0.36	0.24	0.12	
ļ	Poor.	6.0	1.20	0.90	o.66	0.48	0.30	
1,000	Excellent.	1.0	0.26	0.19	0.15	0.08	0.02	
1	Poor.	2.0	0.20	0.30	0.55	0.19	0.10	
10,000	Excellent.	0.61	0.16	0.10	0.072	0.022	0.032	
	Poor.	1.5	0.33	0.50	1.12	0.11	0.02	
30,000	Excellent.	0.2	0.13	0.08	0.06	0.040	0.052	
- '	Poor.	1.0	0.22	0.12	O. I I	0.03	0.02	
100,000	Excellent.	o·38	0.10	0.06	0.042	0.03	0.000	
1	Poor.	0.75	0.50	0.15	0.09	0.06	0.018	
			1			<u> </u>	1	

Note.—The above quantities of pipe refer to direct expansion, and should be made one and one-half times to twice the length for brine circulation. To find the corresponding lengths of 1½-inch pipe, divide by 1.25 or multiply by 0.8; of 2-inch pipe divide by 1.08, or multiply by 0.55.

Number of cubic feet covered by one foot of 1-inch Iron Pipe.

e of ing in Feet or less.	tion.	TEMPERATURE, DEGREES FAHR.						
Size Buildi Cubic more o	Insulation	o°.	10°.	20°.	30°.	40°.	50°.	
100	Excellent.	0.3	1.3	2·I	2.8	4.5	7.0	
1,000	Poor. Excellent.	0·15	0·7 4·0	6.0 I.I	1·5 8·4	2·1 12·4	3.2	
10,000	Poor. Excellent.	0.2	6.0 6.0	3·2 10·0	4.2 13.0	18·0	28·0	
30,000	Poor. Excellent.	0·85 2·0	8.0	5.0 14.0	18·0	9.0 25.0	14·0 40·0	
100,000	Poor. Excellent.	1.0 5.6	4.0	7.0 17.0	9.0 9.0	33.0	20.0	
•	Poor.	1.3	5·0	8.2	11.0	17.0	55·o	

NOTE.—The above figures refer to direct expansion, from one-half to two-thirds of the spaces only would be covered by the same amount of pipe in case of brine circulation. To find the corresponding amounts of cubic feet of space which would be covered by one lineal foot of 1\frac{1}{4}-in. pipe, multiply by 1.25 or divide by 0.8; of 2-in. pipe, multiply by 1.08 or divide by 0.55.

Number of cubic feet covered by 1-ton Refrigerating Capacity for 24 hours.

ng in Feet,	Insulation.	TEMPERATURE, DEGREES FAHR.							
Siz Build Cubic more		0°.	10°.	20°.	30°.	40°.	50°.		
100	Excellent.	150	600	800	1000	1600	3000		
	Poor.	70	300	400	600	900	2000		
1,000	Excellent.	500	2500	3000	4000	6000	12000		
	Poor.	250	1500	1800	2500	5000	10000		
10,000	Excellent.	700	3000	4000	6000	9000	18000		
	Poor.	300	1800	2500	3500	7000	14000		
30,000	Excellent.	1000	5000	6000	8000	13000	25000		
	Poor.	500	3000	3500	5000	11000	20000		
100,000	Excellent.	1500	7500	9000	14000	20000	40000		
	Poor.	800	4500	5000	8000	16000	35000		

TABLE OF REFRIGERATING CAPACITIES.

3	SIZE OF BU	BUILDING.		Number	Number of Cubic Feet per Ton of Refrigeration at Temperature given	ect per To	n of Refrig	eration at	Temperatu	re given.
Dimensions of	Contents:	Surface	Ratio: Cubic			Te	Temperatures	·s.		
Building.	Cubic feet.	in Square feet.	feet to Square feet.	%	&	.91	240	320	%	48%
X X X X X X X X X X X X X X X X X X X	181	130	1.3	8	1,100	1,300	1,500	1,700	1,900	2,100
8x rox ro	800	520	59.0	1,800	2,200	2,600	3,000	3,400	3,800	4,200
10 X 10 X 10	000,1	8	9.0	1,940	2,376	2,808	3,240	3,670	4,104	4,530
25× 40× 10	10,000	3,300	0.33	3,600	4,400	5,200	0,000	6,700	2,600	8,400
20 × 50 × 20	20,000	4,800	0.54	4,860	5,940	7,020	8,100	9,180	10,260	11,340
30× 50× 20	30,000	0,200	0.500	5,670	0,930	8,190	9,650	10,710	0/6'11	13,230
40× 50× 20	40,000	2,600	61.0	6,300	2,700	9,100	10,500	006'11	13,300	14,700
50× 50× 20	20,000	000,6	0.18	6,480	2,920	9,360	10,800	12,240	13,680	15,120
60× 50× 20	000,000	10,400	0.17	6,840	8,360	088,6	11,400	12,920	14,440	15,960
80X 50X 20	%,000 %	13,200	0.105	7,200	08,80	10,700	12,000	13,600	15,200	16,800
100 × 50 × 20	100,000	16,000	o.10	7,200	8,800	10,400	12,000	13,600	15,200	16,800
100 X 100 X 20	200,000	28,000	0.14	8,100	006'6	11,700	13,000	15,300	17,100	18,900
100 × 100 × 30	300,000	32,000	91.0	11,030	13,486	15,938	18,390	20,840	23,290	25,740
100 X 100 X 40	400,000	36,000	80	13,050	15,950	18,850	21,750	24,650	27,550	30,450
100 X 100 X 50	500,000	40,000	8.0	14,400	17,600	20,800	24,000	27,200	30,400	33,600
100 × 100 × 60	000'009	44,000	0.073	16,200	19,800	23,400	27,000	30,600	34,200	37,800
100 × 100 × 70	200,000	48,000	0.0	16,650	20,350	24,050	27,750	31,450	35,150	38,850
100 × 100 × 80	800,000	52,000	0.002	18,000	22,000	26,000	30,000	34,000	38,000	42,000
00 × 001 × 001	000,000	26,000	0.005	18,900	23,100	27,300	31,500	35,700	29,000	44,100
100 X 100 X 100	1,000,000	000'09	90.0	19,350	23,650	27,950	32,250	36,550	40,850	45,150
Lineal feet.	Cubic feet.	Square feet.	Ratio.	Cubic feet.	Cubic feet.	Cubic feet.	Cubic feet.	Cubic feet.	Cubic feet.	Cubic feet.
								_		

ROUGH ESTIMATE OF REFRIGERATION IN BREWERIES.

A ready method of obtaining a rough estimate in tons of the amount of refrigeration required in a brewery is to divide the capacity of the brewery in barrels by 4.

REFRIGERATING CAPACITY IN B.T.U. REQUIRED PER CUBIC FOOT OF STORAGE ROOM IN TWENTY-FOUR HOURS.

Ī	of ing in Feet, or less.	ation.	TEMPERATURE, DEGREES FAHR.						
	Sign Build Cubic more	Insulation	00.	10°.	20°.	30°.	40°.	50°.	
	100	Excellent. Poor.	1,800 4,000	480 960	360 480	284 470	180 330	95 140	
	1,000	Excellent. Poor.	,100	110 190	95 165	70	47	24 28	
	10,000	Excellent. Poor.	400 900	95 160	70 110	47 81	55 30 40	16 20	
	30,000	Excellent. Poor.	280 550	55 95 38 63	47 81	35 55	22 26	11 14	
	100,000	Excellent. Poor.	190 350	38 63	30 55	20 35	14 18	7	

Variation in Capacity, etc., of a Refrigerating Machine.

The following diagram (Fig. 22) and table (on page 75), showing the variation in capacity, etc., of a refrigerating machine, and the economy of direct expansion, is drawn up by the De La Vergne Company:—

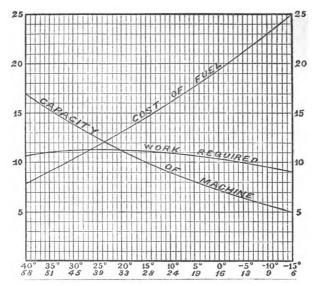


Fig. 22.—Diagram showing Variation in Capacity, Cost of Fuel, and Work Required of a Refrigerating Machine.—(De La Vergue Company.)

In the above diagram the line marked "capacity of machine" shows the diminished capacity as the back pressure is reduced. If the machine has a capacity of ten tons at a return pressure of 28 pounds, as shown by vertical height of the curve, it has a capacity of five tons only with a return pressure of six pounds. Under the same circumstances the cost of fuel per ton is increased in the ratio of the vertical heights to the curve marked "cost of fuel," namely, from 14.5 to 25. In other words, the cost per ton is nearly doubled while the capacity is halved. The work, as seen by the curve marked "work required," diminishes very slowly.

This shows very plainly the economy of direct expansion. The ammonia in the coils of the brine tank must be cooled below the brine or the directly expanded ammonia. If the difference be 10°, say 5° instead of 15°, then the capacity of the machine is reduced in the ratio of 10 to 8, or 20 per cent., and the cost for fuel increased in the ratio of from 14'5 to 17'5, or 20 per cent.

These are physical facts which cannot be explained away, and the economy of direct expansion in practice over both brine and air circulation is usually greater than the diagram and table illustrates.

CUBIC FEET OF AMMONIA GAS PER MINUTE TO PRODUCE ONE TON OF REFRIGERATION PER DAY.

CONDENSER.

103 168 185 115 127 139 153 200 218 65° 70° 75° 80° 85° 900 95° 1000 p 105° 5.84 5.9 5.96 6.03 6.09 6.19 6.23 6.30 6.43 -20° 4 REFRIGERATOR -15° 5.35 5.52 5.28 5.70 5.4 5.46 5.64 5.83 5.77 4.81 -10° 4.66 4.76 4.86 4.97 9 4.73 4.91 5.05 5.08 -5° 4.09 4.12 4.17 4.21 4.25 4:30 4.35 13 4.40 4.44 00 3.63 3.66 3.70 3.83 3.87 16 3.74 3.78 3.59 3.01 5° 20 3.20 3.24 3.27 3.30 3:34 3.38 3.41 3.45 3.49 100 2.87 2.0 2.93 2.96 2.99 3.06 24 3.02 3.09 3.12 2.73 28 15° 2.59 2.61 2.65 2.68 2.71 2.76 2.80 2.82 33 20° 2.31 2.34 2.36 2.38 2.41 2.44 2.46 2.49 2.51 25° 2.06 2.08 2.10 2.12 2.15 2.17 2.20 39 2.22 2.24 30° 1.85 1.87 1.89 1.97 1.91 1.93 1.95 2.00 2.01 45 1.79 35° 1.70 1.72 1.74 1.76 1.77 1.81 1.83 1.85 51

DETERMINATION OF MOISTURE IN AIR.—(Siebel.)

The moisture in the atmosphere may be determined by a wet-bulb thermometer, which is an ordinary thermometer, the bulb of which is covered with muslin kept wet, and which is exposed to the air, the moisture of which is to be ascertained. Owing to the evaporation of the water on the muslin, the thermometer will shortly acquire a stationary temperature, which is always lower than that of the surrounding air (except when the latter is actually saturated with moisture). If t is the temperature of the atmosphere, and t_1 the temperature of the wet-bulb thermometer in degrees Celsius, the tension e, of the aqueous vapour in the atmosphere, is found by the formula—

$$e = e_1 - 0.00077(t-t_1)h_1$$

 e_1 being the maximum tension of aqueous vapour for the temperature t_1 as found in table, and h the barometric length in millimeters. (See table, p. 77.)

If e_2 is the maximum tension of aqueous vapour for the temperature t, the degree of saturation, H, is expressed

by—

$$H = \frac{e}{e_2}$$

and the dew point is also readily found in the same table, it being the temperature corresponding to the tension e.

PSYCHROMETERS.

Instead of the wet-bulb thermometer alone, it is more convenient to use two exact thermometers combined (one with a wet bulb and the other with a dry bulb, to give the temperature of the air), to determine the hygrometric condition of the atmosphere, or of the air in a room. Instruments on this principle can be readily bought, and are called psychrometers. If they are arranged with a handle, so that they can be whirled around, they are called "sling psychrometers." These permit a quicker correct reading of the wet-bulb thermometer than the plain psychrometer, in which the thermometers are stationary and are impracticable at a temperature below 32° Fahr., while the sling instrument can be read down to 27° Fahr.

The following table can be used to ascertain the degree of saturation or the relative humidity of air:-

RELATIVE HUMIDITY-PER CENT.—(U.S. Weather Bureau.)

Ē	(L)ry iner.)	8 2 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8
	6.0	££\$688 6 4 4 4 4 4 4 8 8 8 8 8 8 8 8 8 8 8
	52	8 0 1 8 2 7 8 0 1 2 4 8 8 8 9 1 8 9 1 8 9 9 9 9 9 9 9 9 9 9 9
(i)	20.0	£44440.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.2.
Difference between the Dry and Wet Thermometers (t-t_1).	4°.5	6622.853.85.85.85.85.85.85.85.85.85.85.85.85.85.
Тьегшош	4%0	25.78.000 5.00 68.00 60 60 60 60 60 60 60 60 60 60 60 60 6
d Wet 7	3°.5	65 67 70 70 72 72
Dry an	3%.0	29 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
veen the	2°.5	1 2 E 4 4 2 C 5 C 6 C 6 C 6 C 6 C 6 C 6 C 6 C 6 C 6
nce bety	20.0	7,7,7,7,7,7,7,7,7,7,7,7,7,7,7,7,7,7,7,
Differe	10.5	28848888888888888888888888888888888888
	0.01	92 2 2 2 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3
	0.5	44488888888888
	f(Dry Ther.)	8 2 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8 8

The hygrometer of Professor Marvin is a sling psychrometer of improved construction.

HYGROMETERS.

While the term "hygrometer" applies to all instruments calculated to ascertain the amount of moisture in the air, it is specifically used to designate instruments on which the degree of humidity can be read off directly on a scale without calculation and table. Their operation is based on the change of the length of a hair, or similar hygroscopic substance under different conditions of humidity.

Table giving weights of aqueous vapour held in suspension by 100 lbs. of pure dry air when saturated, at different temperatures, and under the ordinary atmospheric pressure of 29'9 in. of mercury.—(Box and Lightfoot.)

Temper- ature.	Weight of vapour.	Temper- ature.	Weight of vapour.
Fahr. degs.	lbs.	Fahr. degs.	lbs.
-20	0.0320	102	4.242
-10	0.0574	I 1 2	6.253
0	0.0 918	122	8.584
+10	0.1418	132	11.771
20	0.2262	142	16·17 0
32	0.379	152	22.465
42	0.261	162	31.713
52	0.819	172	46.338
62	1.179	182	71.300
72	1.680	192	122.643
89	2.361	202	280.230
92	3.580	212	Infinite

N.B.—The weight in lbs. of the vapour mixed with 100 lbs. of pure air at any given temperature and pressure is given by the formula—

$$\frac{62.3E}{29.9-E} \times \frac{29.9}{2}$$

Where E = elastic force of the vapour at the given temperature, in inches of mercury (to be taken from Tables).

p = absolute pressure in inches of mercury. = 29.9 for ordinary atmospheric pressure.

CORRECT RELATIVE HUMIDITY FOR A GIVEN TEMPERA-TURE IN EGG ROOMS.—(Madison Cooper.)

TEMPERATURE IN DEGREES FAHR.	RELATIVE HUMIDITY PER CENT.
28	80
2 9	78
30	76.
31	74
32	71
33	69
34	67
35 36	67 65 62
37	60
37 38 ·	58
39	58 56
40	53
l	1

SPECIFIC HEAT AND COMPOSITION OF VICTUALS.

	Water.	Solids.	Specific Heat above Freezing Calc.	Specific Heat below Freezing Calc.	Latent Heat of Freezing Calc.
Lean beef Fat beef Veal Veal Fat pork Eggs Potatoes Cabbages Carrots Cream Milk Oysters White fish Eels Lobsters Pigeons Poultry	72.00 51.00 63.00 39.00 70.00 74.00 91.00 83.00 59.25 87.50 80.38 78.00 62.07 76.62 72.40	28·00 49·00 37·00 61·00 30·00 26·00 9·00 17·00 30·75 12·50 19·62 22·00 37·93 23·38 27·60 26·30	0.77 0.60 0.70 0.51 0.76 0.80 0.93 0.87 0.68 0.90 0.84 0.82 0.69 0.81	0.41 0.34 0.39 0.40 0.42 0.48 0.45 0.45 0.47 0.43 0.43 0.42	102 72 90 55 100 105 129 118 84 124 111 88

TEMPERATURES ADAPTED FOR THE COLD STORAGE OF VARIOUS ARTICLES.

Degrees Fahrenheit.

Ale	Article.		Wallis- Tayler.	Siebel.	Siebel. Schmidt.	Getty.	Ice and Refrigera-	Ice and Cold Storage.	Rane.	Madison Cooper.
	:	:	ı	33—42	ı	1	I	ı		1
Apples	:	:	32—36	33	32—36	32	32-36	33—36	1	31
Apples (Summer)	:	:	1	ļ	1	1	1	I		ı
Apples (Winter)	:	:	I	1	ı	١	ı	i	32—35	1
Apple and Peach	h Butter	:	١	1	ı	40	l	ı	I	42
Asparagus	:	:	34	34	34—35	34	34	35	34	33
Bananas	:	:	4045	34—36	34	35	40-45	40-45	1	30
Beans (dried)	:	:	32-40	1	ı	32-40	i	32-40	1	4
Beef (fresh)	:	:	١	1	ı	37—39	1	ı	1	35
Beef (dried)	:	:	1	1	i	30-45	1	١	1	١
Beer (in casks or barrels)	arrels)	:	33-42	33—42	33-35	.	33-42	3340	ı	I
Beer (in bottles)	:	:	45	45	45	l	45	45	1	45
Berries (fresh, for	ten days)	:		l	1	35	١	36-40	1	9
Buckwheat flour	:	:		1	1	1	١	9	ı	45
Butter	:	:		32—35	18-25	32 - 35	32-38	25-30	ı	14
Butter (to freeze)	:	:		1	1	20	١	I	١	I
Butterine.	:	:	35		1	I	1	35	1	20
Cabbages	:	:	34	ı	1	33		35	ı	32
Captaloupes	:	:	9	1	1	I	1	9	ı	9
	:	:	34			34	1	35	1	33

Trierpatings Adapted for the Cold Storage of Various Articles.—(Continued.)

	TEMPERATURES ADAPLED FOR 1112	RATO	4	1	1	;	1	1						
1		Ar	Article.				Wallis- Tayler.	Siebel.	Siebel. Schmidt.	Getty.	Ice and Refrigera-	Ice and Cold Storage.	Kane.	Madison Cooper.
	Colours				:	=	12-34	33—35	34—35	34	32-34	35		32
	: Celety	:	•		:	:	,,	22-22	28-24	21-32	32-33	32-33	I	35
_	Cheese	:	•		:	:	5,00	50	10		3 1	22,22		04
	Chestnuts	•	•		:	:	33	1		ç		S		- I
	Chocolate (to cool	(to coo	· -		:	:	40	1	1	1	١	,		,
_	Cider	:	٠.		:	:	30-40	30-40	30-35		30-40	35-40	!	3,5
	Cigars	:	•		:	:	35	1		35	1	35	ľ	24
_	Clarets	•	•	•	:	:		4550	1	1	1	1	 	;
	Corn Meal	:	•	•	:	:		1	1	1 :	1	;		1:
	Corn (dried)	€ :	•	•	:	:	35	I	1	35		35,	1	45
	Cranberries		•	٠	:	:	34-30	1		1	I	34-30		ડ
_	Cream	•	•		:	:	35	1		1			78	82
	Cucumbers	•	•	•	:	:	ı		l				30	, c
	Currants	:	•		:		I		i	l	l	;		7.
	Dates	•	•		:	:	55		1	1	1	55,	١.	\$ 6
	Eggs	•	•	•	:	:	33—35	32—33	31-33	i	32—35	33—35		Ş≪
-	Ferns	•	•		:	:	l		l	;	1			1
	Figs	:	•	•	:	:	55		1	35	1	- ا ا		×
	Fish (fresh	•	•	•	:	:	25—30		50	25	25-30	25-30		1 2
	Fish (fresh water, frozen)	water,	frozer	<u>ج</u>	:	:				I	1	1		
_	Fish (salt water	vater, f	rozen)		:	:	I	1	1		1		1	:
_	Fish (cann	ed)	•		:	:	١	١	ı	S,	;	;		Ş
	Fish dried	: -	•	•	:	:	35	35	35—30.		35	35	!	,
_	Fish (to freeze)	eze)		•	:	:	l	I	1	•	9	l		ا ٥
G	Flour, &c.	•	•		:	:	1	\$	30-40	0	-			
_	Fruits	•	•	•	:	:	26—55		1		1	,		ç
	Fruits (dried)	eg)	•	•	:	:	35-40	1		ۍ <u>;</u>	1	35 40		÷ 5
	Fruits (canned	ned)	•		:	=	35	1	1	33		33		

TEMPERATURES ADAPTED FOR THE COLD STORAGE OF VARIOUS ARTICLES—(Continued.)

Arti	Article.			Wallis- Tayler.	Siebel.	Siebel. Schmidt.	Getty.	Ice and Refrigera- tion.	Ice and Cold Storage.	Rane.	Madison Cooper.
dressed)	:	:		35	12		35	35		ı	35
Furs (dressed)	: :	: :	:	25-72	25—32	28—35	25-72	25-72	¥	J	2 2
Game (frozen)	: :	: :	:	25-28	25-28	25-28	27.2	25-28	25-28	١) (20)
Game (to freeze)	:	: :	:	15-28	, 1	, }	Ĭ	, 1	15—28	ı	1
long storage	: (a)	:	:	, 1	ı	ı	, 1	1		ı	2
:	:	:	:	36—38	32-40	34—36	32-40	36—38	36-38	3840	
ringer ale	:	:	:	36	36	1	1	1		1	30
:	:	:	:	-	1	1	30 - 35	1	1	1	2
:	:	:	:	1	1	1	30-33	1	1	ļ	I
:	:	:	:	33—40	33—36	32—40	35	33-40	35-40	1	35
(frozen)	:	:	:	١	1	1	1	1	88	1	1
:	:	:	:	45	36-40	45	37-40	45	45	ı	45
:	:	:	:		1	1	34-45	: [1	1	: 1
emons	:	:	:	36—40	36-45	33—36	35-45	3640	36-40	1	3 2
:	:	:	:	1	I	l	20	1	1]	20
Maple syrup sugar	:	:	:	1	1	l	40-45	1	1	1	45
Margarine	:	:	:	1	35	18-25	1	35	1	١	:
rined)	:	:	:	1	:	ı	35-40	3	I	1	!
(canned)	:	:	:	35	1	1	35	1	35	į	ç
resh)	:	:	:	35	35	35—40	1	34	35	1	. 1
(for 3 or 4 weeks)	weeks)	:	:	: 1	3	1	i	1	1	I	35
:	:	:	:	1	l	1	32	1	1	1	!
futton (fresh)	•	;	_	J	i	ı	37-26	١	į		1

TEMPERATURES ADAPTED FOR THE COLD STORAGE OF VARIOUS ARTICLES.—(Continued.)

25—28 35—38 35—40 35—38 35 35 — — — — 34 — — — — 34—40 32—33 36 32 34—40 35 — — — — 45—50 36 34—36 35—36 45—50 32 — — — — 33 — — 34—40 45—55 35—45 34—36 33—45 45—55 46 — — — — 40 — — — — 40 — — — — 40 — — — — 40 — — — — 40 — — — — 13-40 34-36 34-36 34-36 34-36 140 — — — — 13-40 — — — — 18-20 38-36 34-36 34-36 35-40 18-21 — — — — 18-22 — — — — 18-22 <t< th=""><th>Article,</th><th></th><th>Wallis- Tayler.</th><th>Siebel.</th><th>Schmidt.</th><th>Getty.</th><th>Ice and Refrigera-</th><th>Ice and Cold Storage</th><th>Rane.</th><th>Madison Cooper.</th></t<>	Article,		Wallis- Tayler.	Siebel.	Schmidt.	Getty.	Ice and Refrigera-	Ice and Cold Storage	Rane.	Madison Cooper.
Strain Control Contr			6							
n shells)	Mutton (frozen)	:	25-28	١	1	1	;	;	1	:
argarine	Nuts (in shells)	:	35	35—38	35-40	35—39	35	35	1	0
### starting control of the following control of the following starting control of the following starting control of the following cont	Oatmeal	:	40		ļ		1	9		42
\$\text{in tubs}\$\tag{5}\$ \$\text{sin shells}\$\tag{5}\$ \$\text{sin shells}\$\tag{5}\$ \$\text{sin shells}\$\tag{7}\$ \$\tex	Oleomargarine	:	35	I		l	1	35	I	20
s (in tubs) s (in tubs) s (in tubs) s (in shells) s (in sh	Oil	:	35			35	1	35	1	45
s	Onions	:	34—40	32-33		32	34—40	35—40	34—40	32
\$ (in tubs) \qquad \qquad \qquad \qquad \qquad \qquad \qquad \qquad \qqqq \qqqqq \qqqqq \qqqqq \qqqqq \qqqqq \qqqqq \qqqqq \qqqqq \qqqqq \qqqqqq	Oranges	:	45—50	30		35 - 36	45—50	45-50		34
s (in tubs) s (in tubs) s (in shells) s (in shells) s (in shells) s (in shells) s	Oysters	:	33—35	ı	I	ļ	1	33—35	1	33
s (in shells)	Oysters (in tubs)	:	25	1		35	1	25	ı	35
s	Oysters (in shells)	:	33	1		40	I	30	1	43
55	Ox tails	:	I	1	I	32	ı	l		1
is	Parsnips	:	34	I	I	34	ı	35	۱,	32
ined)	Peaches	:	4555	35—45	34—36	35—45	45—55	45—55	30–38	36
Hried) 40	Pears	:	34—30	33—30	34-30	38	34—30	35	33 - 38	33
es	Peas (dried)	:	9	1	l	40	l	40	! ,	45
	Plums	:		1	l	1	1	I	38—40	32
34 34 34 34 35 35 35 35 35 35 35 35 35 35 35 35 35	Porter	:		3342	I	I	ı	I	1	I
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	Pork	:	34	1	l	1	١,	١,	1	I
)	Potatoes	:	36—40	34—30	1	35	30—40 30—40	30-40	30-40	34
ze)18—22 — — 5—10 —	Poultry (frozen)	:	28—30	28—30	20—28	5 0	28-30	28-30	l	28
	Poultry (to freeze)	:	18—22	1	i	5—10	1	18-22	I	ı
	Poultry (long storage) .	:	1	1	l		ı	I	ı	0
35 - - -	Sardines (canned)	:	35	1	_		-	35	1	40

TEMPERATURES ADAPTED FOR THE COLD STORAGE OF VARIOUS ARTICLES.—(Continued.)

Art	Article.			Wallis- Tayler.	Siebel.	Schmidt. Getty.	Getty.	Ice and Refrigera- Cold tion. Storage.	Ice and Cold Storage.	Rane.	Madison Cooper.
Sauerkraut Sausage casings Sugar, &c Sweet com Syrup Trederloin, butts, ribs Tobacco Veal Veal Water-melons Wheatflour Wheatflour Wines Woollens, &c	::::::::::::::::::::::::::::::::::::::	:::::::::::::::::::::::::::::::::::::::	:::::::::::::::::::::::::::::::::::::::	35—38 35—38 35—35 35—35 36—45 36—45 37—40 37	34-35	38-42	36—38 30—35 30—35 35 35 36—35 36—36 10—10—10—10—10—10—10—10—10—10—10—10—10—1		35—38 40—45 35 35 35 35 40 40 45—50 25—30	38 42	88 02 4 5 1 4 4 1 1 6 4 4 4 1 1 4 4 4 1 1 1 1 1 1

MEAN TEMPERATURES OF PRINCIPAL CITIES OF THE WORLD.

CITIES.	Spring.	Summer.	Autumn.	Winter.	Annual.
ENGLAND. Birmingham Bristol Liverpool London Manchester	Degs. Fahr. 48.0 49.7 48.8 49.0 48.0	Degs. Fahr. 62.0 63.0 62.9 62.8 62.0	Degs. Fahr. 50.0 51.5 51.8 51.3 50.5	Degs. Fahr. 34.2 40.0 39.8 39.5 34.8	Degs. Fahr. 48·2 51·05 50·8 50·6 48·8
SCOTLAND. Edinburgh Glasgow	45°7 47°9	57·9 60·9	48·0 50·5	39·5	47°5 49°8
IRELAND. Belfast Dublin	=	=	=	=	50·1
FRANCE. Bordeaux Boulogne Marseilles Nice Paris			 -63·0	 48·7	57.0 54.4 58.3 60.1 51.3
GERMANY. Berlin	46·4 — — — — — — — — 53·8 49·5	63·1 — — — — — — 71·5 63·9	47·8 — — — — — — — 56·6 52·8	30·6 — — — — — — — — 39·5 39·9	47.5 46.7 47.5 49.6 48.0 46.4 48.4 55.8
ITALY. Florence Genoa Milan Naples Palermo Rome Turin Venice	59·5 59·5 57·4 53·1	74.5 74.5 73.2 71.6	 62·5 65·9 61·7 53·8		59·2 61·1 55·1 61·6 63·1 59·7 53·1

MEAN TEMPERATURES OF PRINCIPAL CITIES OF THE World.—(Continued.)

CITIES.	Spring.	Summer.	Autumn.	Winter.	Annual.
Spain & Portugal.	Degs. Fahr.	Degs. Fahr.	Degs. Fahr.	Degs. Fahr.	Degs. Fahr.
Barcelona		-		_	63.0
Madrid	57.6	74·1	56.4	42 · I	57.6
Lisbon	59.9	71.1	62.5	52.3	61.4
SWITZERLAND.	l				
Berne	45.8	60.4	47:3	30.4	46.0
Geneva			- -	J- T	52.7
		ĺ			
Holland.	r				
Amsterdam	-	-	_	_	49.9
Rotterdam	–	_	_	_	21.0
BELGIUM.	1				
Brussels					50.7
	1				30 7
NORWAY & SWEDEN.					
Christiania	39 ·2	61.0 29.2	42.4	25.2	41.7
Stockholm	38.3	61.0	43.8	25.4	42·I
Davis			ľ		
DENMARK. Copenhagen	43.7	63.0	48.5	31.2	46∙8
Copennagen	43 /	030	40 5	31 5	40-0
Russia.					
Moscow	43.3	62.6	34.9	13.2	38.5
Nicolaief	49.3	72.2	50.0	25.9	48.7
St. Petersburg	35.1	60.3	40.5	16.6	38.3
Warsaw	44.6	63.5	46.4	27.5	45.2
T					
TURKEY. Bucharest				_	46.4
Constantinople.	51.8	73.4	60.4	40.6	46·4 56·7
Constantinopie.	51.0	/34	00 4	400	50.7
PALESTINE.					
Jerusalem	60.6	72.6	66.3	49.6	62.2
_				.,	
EGYPT.					
Cairo	71.6	84.6	74.3	58.2	72.3
Algeria.					
Algiers	63·o	74.2	70.5	50.4	64.6
Tunis	-5	74 3	/_3	30 4	68.8
					00 0
					<u>`</u>

MEAN TEMPERATURES OF PRINCIPAL CITIES OF THE WORLD.—(Continued.)

CITIES.	Spring.	Summer.	Autumn.	Winter.	Annual.
North America.	Degs. Fahr.	Degs. Fahr.	Degs. Fahr.	Degs. Fahr.	Degs. Fahr.
Baltimore	60.0	83.0	64.6	43.2	54.9
Boston	48·o	66.0	53.0	28·ŏ	49.ó
Chicago	52.8	74.2	61.3	38.2	45.9
Cincinnati	ĕ3∙2	81.8	66.4	46.6	54.7
Mexico	53.6	63.2	65∙i	60.2	60.5
Montreal	44.2	69. I	47.1	17.5	43.7
New Orleans	73.0	84·o	72.0	58·ŏ	72.0
New York	50.0	72.0	56.0	33.0	53.0
Philadelphia	.52.0	76· o	57.0	34.0	55·o
Quebec	, J	ı <u>'</u> —	3,	"	40.3
San Francisco	58∙0	59 ·0	60.0	53.0	57.5
St. Louis	84.6	67.8	44.6	46.0	55.0
Washington	69.0	79.0	58·o	38.0	59.0
South America.					
Buenos Aires	59.4	73.0	64.6	52.2	62.5
Lima	63.0	73.2	69.6	59.0	66.2
Quito	60.3	60∙1	62.5	59.7	60.1
Rio Janeiro	72.5	79 ·0	74.5	59.7 68.5	73.6
Valparaiso	_	1 -		_ `	64.0
EAST INDIES.					_
Bombay		_			81.3
Calcutta	82.6	83.3	80·0	67.8	78.4
Madras	i —	_	_	-	81.9
WEST INDIES.	1				
Havanna	-0.0	8-10		-7-	79°I
Kingstown	78.3	81.3	80.0	76.3	79.0
Port of Spain	_	_	_	_	81.2
China.				i _	
Canton	69.8	82.0	72.9	54.8	69.8
Pekin	56.6	77.8	54.9	29.0	52.6
Australasia.					
Melbourne	-			-	57·0
Paramatta	66.6	73.9	64.8	54 ·5	64.6
Sydney		-	-		65.8
	١ _				
Funchal	63.2	70.0	67.6	61.3	65.7
NEW ZEALAND.				ł	
Auckland	60.1	66.7	58∙0	53.5	59.6
l_			, ,	1 33 3	3,

MEAN TEMPERATURE BY SEASONS AND EXTREMES, FOR THE YEAR, OF TWENTY STATIONS IN THE ARGENTINE REPUBLIC.—(Degrees Fahrenheit.)

(Especially compiled by the Argentine Meteorological Office.)

3		Winter. Spring. Annual. Max. Min.	51.8 61.4 62.3 104.0 28.4	47.0 59.5 59.3 105.8 23. 0	50.5 63.1 63.0 111.1 17.7	55.4 66.2 66.1 107.6 30.2 54.8 65.0 65.6 107.6 30.2	61.3 71.0 70.7 107.6 37.4	51.8 64.4 62.7 111.1 15.8	57.8 68.0 66.6 11111 26.6	54.2 66.2 63.6 95.0 24.8	58.5 72.8 70.3 109.4 28.4
	Extre	Max.	104.0	8.501	1.111	9.201	9.201	1.111	1.111	0.56	109.4
		Annual.	62.3	59.3	63.0	9.59	20.2	62.7	9.99	9.89	70.3
		Spring.	61.4	2.65	63.1	66.2 65.0	0.12	64.4	0.89	2.99	72.8
	1	Winter.	51.8	47.0	20.2	55.4 54.8	61.3	51.8	8.25	54.2	58.5
0		Autumn.	9.29	29.0	0.79	65.0 65.0	0.12	61.3	9.59	9.29	2.69
- Carried Commenter		Summer.	73.4	9.1.2	2.92	76.5	79.4	73.4	75.5	9.11	9.08
Gaman			:	:	:	::	:	:	:	:	:
2		Station.	Capital of the Republic. Buenos Aires	Province of Buenos Aires. Bahia Blanca	Province of Santa-Fe. Rosario	Province of Entre-Kios. Paraná Concordia	Province of Correntes. Corrientes	Province of Coraoba. Córdoba	Province of Iucuman. Tucumán	Province of Salia. Salta	Pronnce of Santiago del Estero.

Mean Temperature by Seasons and Extremes, for the Year, of Twenty Stations in the Argentine Republic.— $(Degrees\ Fahrenheit,)$

(Especially compiled by the Argentine Meteorological Office.)

	-					
7	Yattamir.	winter.	·Burnge.	Annual.	Max.	Min.
7						
	8.09	48.2	64.4	0.29	9.201	9.41
1	64.4	51.5	0.89	65.4	1.111	28.4
· · · · · · · · · · · · · · · · · · ·	70.4	26.5	72.8	2.02	0.401	30.5
··· ·· ·· ·· ·· ·· ·· ·· ·· ·· ·· ·· ··	2.99	9.89	2. 69	8.99	0.401	28.4
il Chubut.	26.5	49.5	63.2	9.19	102.2	23.0
	8.99	54.6	71.4	67.3	109.4	32.0
Territorio Marianal Manaila	54.5	42.8	57.2	55.7	102.2	14.0
Chos Malal 71.6	9.95	45.5	57.2	9.25	102.2	14.0
Posadas 79.2	72.2	9.69	73.2	0.12	100.4	32.6
Formosa 80.0	0.12	63.1	9.12	4.1.4	0.701	30.5

COLD STORAGE CHARGES (England).

Cambria Cold Storage and Ice Co., Ltd.

MEAT.

1	First 24 Hours.		Each succeeding 24 hours.	Per Week.
	1/-		6d.	2/-
	6d.		3d.	1/6
	1/- `		6d.	2/-
ach	1 d. per	wee	k or any par	rt thereof.
,,	īd.	,,	,	,
,,	ıd.	,,	,	,
	4d.	,,	,	,,
			1	,,
	ach	24 Hours I/ 6d I/ 6ch I½d. per ,, Id. ,, Id 4d ½d. per lb.	24 Hours. 1/ 6d 1/	#HST. succeeding 24 hours. 1/ 6d 3d. 1/ 6d 3d. 1/ 6d 3d. 1/ 6d. 1/

Minimum Charge, 3d.
FISH, GAME, AND POULTRY.
Fish (wet), small quantities 9d. per cwt. per week or any part thereof.
", large quantities 6d. ", ", ", ", ", Kippers & Finnon, per box 2d. each and upwards per week or any part thereof.
Loose Fish
Poultry and Game I/- per cwt. per week or any part thereof.
Frozen Poultry, in large
quantities20/- per ton for 28 days ,,
Chickens, loose 1 d. per couple per week ,,
Rabbits, in hampers 9d. per cwt. per week ,,
Rabbits, loose id. per couple per week
Rabbits, Frozen, in cases, small quantities, 6d. per case per week or any part thereof.
Rabbits, Frozen, large quantities, 17/6 per ton for 28 days or any part thereof.
Pheasants, 11d. per brace 1st week, 1d. per brace each succeeding week.
Partridge and Grouse, 1d. per brace per week or any part thereof.
Hares Turkeys and Geese 2d each
Minimum Charge and

Minimum Charge, 3d. PROVISIONS.

Butter,	small qu					r any part thereof.
,,					r 20 days o	r any portion thereof.
_ ,,	2 tons a	nd upward	ls, 16/-	,,	,,	,,
Bacon	,,	,,	14/-	,,	,,	",
Cheese	,,	,,	12/6	,,	,,	,,
Lard	,,	,,	15/-	,,	,,	"

CONDITIONS OF DEPOSIT AND REGULATIONS.

The Conditions of Deposit are as follows:—

- The Cambria Cold Storage and Ice Co., Ltd., receive goods on the following conditions only:—
- I.—No goods will be given up without the production of a ticket, which is delivered to the person when goods are brought to Stores, or satisfactory evidence of ownership.
- 2.—All consignments to the Stores must be plainly marked with the owner's name and address, and date.
- All payments for storage must be made when the goods are delivered.
- 4.—The Company will not be responsible for any loss or damage to goods stored by them, through maintaining too high or too low a temperature in the Stores, failure of machinery, fire, or any other cause whatsoever; but the Company will always, and all times, use their utmost endeavours to prevent any such damage, and will render all assistance in their power to properly preserve and keep goods entrusted to their care.
- 5.—The Company reserve to themselves the right to refuse any goods that, in the opinion of the Manager, or his representative, are unfit to store.
- 6.—The Company will hold all goods stored by them subject to a general lien for all debts due by Depositors on account of Storage.
- 7.—Stores open for receiving and delivering goods:—"Week-days, 6 a.m. to 5 p.m.; Saturday, 6 a.m. to 5 p.m., and 10.30 p.m. to 11.30 p.m."

COLD STORAGE CHARGES (United States).

Substance.	Temperature. Degrees.	Month.	For the Season.	Remarks.
Salt meat Dried beef Fresh meat Veal Lamb Game Venison and	32 to 36 32 to 36 32 to 36 38 38 36 36 32 to 36 Below 20	25 to 35 cents 20 to 25 ,, 35 ,, 25 ,, 25 ,, 15 ,,		Per tierce. Per barrel. — Per pound. Per quarter. Per pound. "" Per lb. gross.
poultry Ducks, grouse, and quail Quails Fish Storage Room	Below 20 32 to 35 Below 20 25 to 30	1/2 ,, ———————————————————————————————————	15 ,, 15 ,, —	Per dozen. Per 1,000 cubic feet

COLD STORAGE CHARGES.—(United States.)
(Compend of Mechanical Refrigeration.)

Season Ends.	May 1.
Season Rate per Barrel of 100 lbs.	\$0.45
In Large Quantities. Per Month.	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
Each Succeeding Month.	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
First Month.	60.15 0.15 0.15 0.10
goods and quantity.	Apples, per bbl. Bananas, per bunch Beef, Mutton, Pork, and Fresh Meat per lb. Beer and Ale, per ½ bbl. Beer and Ale, per ½ bbl. Beer and Ale, per ½ bbl. Beer, bottled, per bbl. Berries, fresh of all kinds, per quart Berries, fresh of all kinds, per stand Butter and Butterine, per lb. Cabbages, per case. Cabbages, per case. Calves, per bbl. Cabbages, per case. Calves, per lb. Calves, per lb. Calves, per lb. Calves, per lb.

COLD STORAGE CHARGES.—United States. (Continued.)

GOODS AND QUANTITY.	First Month.	Each Succeeding Month.	In Large Quantities. Per Month.	Season Rate per Barrel of 100 lbs.	Season Ends.
Cheese, per lb	0.00 0.025 0.025 0.025 0.025 0.025 0.025 0.033 0.033 0.033 0.033	0.00 0.10 0.10 0.00 0.10 0.10 0.10 0.10	0.00 1.5 0.10 0.00 0.10 0.10 0.10 0.10 0	\$0.50 0.50	Jan. 1.

COLD STORAGE CHARGES.—United States.—(Continued.)

GOODS AND QUANTITY.	First Month.	Each Succeeding Month.	In Large Quantities. Per Month.	Season Rate per Barrel of 100 lbs,	Season Ends.
Grapes, Malaga, etc., per keg.,	\$1.0\$	\$0.12 ³	8 0.12⅓	 es	
Hops, per lb	00.0	00.0	00.0		
Lard, per tierce	0.25	0.50	0.50	00.1	Nov. 1.
Lard Oil, per cask		0.50		00.1	Nov. 1.
Lemons, per box		0.12		05.0	Nov. I.
Macaroni, per bbl		0.15		, 1	1
Maple Sugar, per lb		0.00		0.40-0.20	Nov. 1.
Maple Syrup, per gallon		\$10.0		· ·	١
Meats, fresh, per lb		00.0		١	1
Nuts of all kinds, per lb.		9.00		0.40-0.20	Nov. 1.
Oatmeal, per bbl		0.15			1
Oil, per cask	0.25	0.50	1	1	
Oil, per hhd	00.1	0.80	ı	1	1
Oleomargarine, per lb	100.0	₹00.0	₹00.0	ı	1
Onions, per bbl	0.15	0.12	0.10	09.0-05.0	May 1.
Onions, per box	0.12	0.10	ì		. 1
Oranges, per box	0.15	0.12	0.10	0.20	Nov. I.
Oysters in tubs, per gal.	50.0	0.0	1	, 1	!
Oysters in shells, per bbl.	05.0	0.40	0.30	1	1
Peaches, per basket	0.10	80.0	20.0	2.00	Jan. I.
Pears, per box	0.50	51.0	. 1	09.0	May 1.
Pears, per bbl	0.40	0.30	i	1.20	May 1.

COLD STORAGE CHARGES.—United States.—(Continued.)

GOODS AND QUANTITY	ry.	First Month.	Each Succeeding Month.	In Large Quantities. Per Month.	Season Rate per Barrel of 100 lbs.	Season Ends.
Pigs' Feet, per lb.	:	{ 00.0 	₹00.0 \$	₹00.0\$	00.1	Nov. 1.
Pork, per tierce	:	0.50	0.15	0.15	!	1
Potatoes, per bbl	:	0.52	0.50	0.50	1	1
Preserves, jellies, jams, etc.,	per lb	1 00.0	1 00.0	00.0	1	ı
Provisions, per bbl	: :	0.52	0.50	0.50	1	1
Rice Flour, per bbl	:	0.50	0.15	0.12	1	ŀ
Sauerkraut, per cask	:	0.52	0.50	0.15	0.60-0.75	Nov. 1.
Sauerkraut, per 3-bbl	:	0.15	0.12	0.10	1	1
Syrup, per bbl	:	0.30	0.52	0.50	8.1	Oct. I.
Tobacco, per lb.	:	100.0	1 00.0	0.00	1	1
Vegetables, fresh, per bbl.	:	0.52	0.50	0.15	1	1
Vegetables, fresh, per case	:	0.15	0.IO	80. 0	1	1
Wine, in wood, per bbl.	:	0.52	0.52	l	i	1
Wine, in bottles, per case	:	0.10	0.10	ı	ı	ı

RATES FOR FREEZING POULTRY, GAME, FISH, MEATS, BUTTER, EGGS, ETC., UNITED STATES.

The rates for freezing goods, or for storing goods at a freezing temperature when they are already frozen, are as follows:—

POULTRY, GAME, ETC., IN UNBROKEN PACKAGES.

Poultry, including turkeys, fowl, chickens, geese, etc.,

and rabbits, squirrels, and ducks when picked.

Four rates, A, B, C, and D, for storing poultry, and the rate to be charged will be determined by the amount of such goods as may be frozen and stored during a season of six months, usually from October or November 1st to April or May 1st.

RATE A.—For customers storing fifty or more tons of poultry, the rate to be one-third cent per pound for the first month stored, and one-fourth cent per pound for each month or fraction of a month, including the first month,

if stored for more than one month.

RATE B.—For customers storing five or more, but less than fifty tons of poultry, the rate to be one-third cent per pound for the first month stored, and one-fourth cent per pound for each month or fraction of a month thereafter.

RATE C.—For customers storing one or more, but less than five tons of poultry, the rate to be three-eighths cent per pound for the first month stored, and one-fourth cent per pound for each month or fraction of a month thereafter.

RATE D.—For customers storing less than one ton of poultry, the rate to be one-half cent per pound for the first month stored, and three-eighths cent per pound for each month or fraction of a month thereafter.

Venison, etc., and ducks when unpicked, one to one-half cent per pound per month, according to quality and length

of time stored.

Grouse and part ridges, three cents to five cents per pair per month. Woodcock, one cent to two cents per pair per month.

Squabs and pigeons, four cents to six cents per dozen

per month. Quail, plover, snipe, etc., three cents to five

cents per dozen per month.

When a portion of the goods is removed from a package, storage to be charged for the whole package as it was received, until the balance of the package is removed from the freezer.

For goods received loose, when to be taken out of the packages in which they are received, or when to be laid

out, the following rates to be charged:-

Poultry, including turkeys, chickens, geese, etc., and rabbits and squirrels, one-half cent to one-fourth cent per pound extra, according to quality and length of time stored.

Grouse, partridges, woodcock, squabs, pigeons, quail, plover, and snipe, 50 per cent. more than the rates as

above specified.

Ducks weighing less than two pounds each, two cents to three cents each per month. Ducks weighing two pounds or more each, three cents to four cents each per month.

For all kinds of poultry and birds not herein specified, the rate from one cent to one-half cent per pound per month, according to quantity and length of time stored.

SUMMER FREEZING RATES.

Freezing rates for the summer months, 50 per cent. more than the specified winter rates for the first month stored, and the same as the winter rates for the second and succeeding months.

STORING UNFROZEN POULTRY, ETC.

For holding poultry, game, etc., which are not frozen, at a temperature which shall be about 30° Fahr., the rate to be one-fifth cent to two-fifths cent per pound according to quantity, for any time not exceeding two weeks.

FREEZING RATES FOR FISH AND MEATS.

Salmon, blue fish, and other fresh fish in packages, onehalf cent per pound for the first month stored, threeeighths cent per pound per month thereafter.

Fresh fish of all kinds when to be hung up or laid out, three-fourths cent per pound for the first month stored, one-half cent per pound per month thereafter.

Fish in small quantities, 50 per cent, more than the

above rates.

Special rates for large lots of large fish.

Scallops, three-fourths cent per pound, gross, per month. Sweetbreads, and lamb fries, one cent per pound, gross,

per month.

Beef, mutton, lamb, pork, veal, tongues, etc., three-fourths cent to one-half cent per pound, net, for the first month stored, one-fourth cent to three-eighths cent per pound per month thereafter.

BUTTER FREEZING RATES.

For freezing and storing butter in a temperature of 20° Fahr, or lower, the rate to be charged will be determined by the amount of such goods that may be frozen and stored during the season of eight months from April 1st to December 1st, or from May 1st to January 1st. There will be three rates, A, B, and C.

RATE A.—For customers storing thirty-five (35) or more tons of butter, the rate to be fifteen cents per 100 pounds, net, per month.

RATE B.—For customers storing five or more, but less than thirty-five tons of butter, the rate to be eighteen cents

per 100 pounds, net, per month.

RATE C .- For customers storing less than five tons of butter, the rate to be twenty-five cents per 100 pounds, net, per month.

EGG FREEZING RATES.

For freezing broken eggs in cans, the charge to be onehalf cent per pound, net weight, per month, and for a season of eight months the rate to be one and one-half cents per pound, net weight.

RENT OF ROOMS.

For freezing temperatures, four cents to five cents per cubic foot per month.

TERMS OF PAYMENT OF COLD STORAGE AND FREEZING RATES.

All the above rates are to be charged for each month, or fraction of a month, unless otherwise specified; and in all cases fractions of months to be charged as full months.

Charges to be computed in all cases when possible upon the marked weights and numbers of all goods at the time they are received.

All storage bills are due and payable upon the delivery of a whole lot, or balance of a lot of goods, or every three months, when goods are stored more than three months.

Unless special instructions regarding insurance accompany each lot of goods, they are held at owner's risk.

COLD STORAGE CHARGES (France).

Public Abattoir, Chambery.

Rent of cold storage chamber 500 francs (£20) per annum. An ordinary cold storage chamber contains 17 or 18 hooks, each capable of supporting about 100 kilogrammes (220.4 lbs.) of meat, and 17 or 18 S-hooks, each capable of receiving 10 kilogrammes (22.04 lbs.), in small pieces. The weights of the meat suspended from the hooks and S-hooks are never to exceed the above. In all cases where such weights are exceeded the butchers will be held responsible for any damage and breakages which may result.

Where a cold storage chamber is let to a number of persons, the rent to be per hook, at the rate of 40 francs (32 shillings) a year, that is to say, for the time during which the cold store is in operation. The S-hook situated above is included with each hook.

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SECTION III.

ICE-MAKING AND STORING ICE.

ICE-MAKING.

ARTIFICIAL ice is either what is known as clear, transparent, or crystal ice, or milky, opaque, or tombstone ice. The latter is generally used where appearance is of no consequence, and cheapness is the main consideration, and it does not necessarily possess any unwholesome qualities, but it has the objection of very considerably reduced keeping powers, and should be used immediately. The opacity of ice is mainly due to rapid freezing preventing the air contained in solution in the water from

escaping.

Clear or crystal ice can be made by using distilled or de-aërated water, or by agitation of the water during the freezing process. This latter has been carried out in a number of different ways, of which the most common and practical is the reciprocating movement of agitators or paddles in the ice can or mould, or in the ice-box, accordingly as the can system or the stationary cell system is in use. Many other devices have, however, been used, amongst which may be mentioned the imparting of a rotary motion to the freezer, rods or plungers moving up and down in cans, oscillating rods or agitators, forcing cold air through the freezing water, shaking cans or moulds, removing water and refilling it by pumping, water injection with pressure reduction, taking water from one point of one can and pumping it into another, rotating stirrer or agitator, freezing ice in very cold air, freezing ice very slowly, freezing ice in very thin slabs.

A white core in ice is due to the presence of carbonite of lime and magnesia or other minerals in the water. A red core in ice is due to the separation of oxide of iron in ice which was maintained in solution in the water in the form of carbonate of iron, and the sediment usually comes from

the iron of the plant. Pure distilled, carefully filtered water should be alone used for making ice intended for domestic consumption. The three most used types of ice-making apparatus are those working on the can system, the stationary cell system, and the plate or wall system.

In ice-making, where it is important to secure the maxi-

In ice-making, where it is important to secure the maximum production at the minimum cost, it is necessary to work both day and night so as to render the operation a continuous one. Likewise such routine must be followed as will ensure the largest possible output and the best quality. With this purpose in view, great care must be exercised to maintain all the parts of the apparatus perfectly clean, and in first-class working order. A regular and systematic plan of drawing the ice must be settled upon and strictly adhered to, and with this object a distinctive number or letter should be stamped or painted upon each can or mould, and so many drawn regularly per hour.

TABLE GIVING SIZES AND CAPACITIES OF ICE-MAKING PLANTS, ETC.

(H.	Η.	Kelley,	" The	Engineer,"	New	York.)	
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Tons *per 24 Hours.	Size of Engine.	Revs.	Size of Com- pressor.	Size of Blocks of Ice.	Gallons of Water per Hour,	Tons of Coal.	No. of Engineers.	No. of Firemen.	No. of Labourers.
I	7× 9	90	\$5 × 10	8 × 8 × 28		1	I	• • •	
3	8×16	80	5 × 15 6 × 18	8 x 15 x 28	15	I	2	2	2
3 5	IO × 20	75	6 x 18	8 x 15 x 28	20	I 1/2	2	2	2
10	12 × 30	70	8×20 {	11 × 22 × 28 11 × 11 × 28	1 20	2	2	2	3
101	14 × 30	65	8 × 25 {	11 × 22 × 28 11 × 11 × 28	} 35	2 <u>1</u>	2	2	3
15	14 × 30	65	10 x 20 {	11 × 22 × 28 11 × 11 × 28		3	2	2	4
20	16 × 30	55	10 × 30 {	11 × 22 × 28 11 × 11 × 28	} 50	4	2	2	5
30	16 × 42	52	11 × 30 {	11 × 22 × 28 11 × 11 × 28		5	2	2	6
40	18 × 36	50	12 × 30	11 × 11 × 28	90	6 <u>1</u>	2	2	7
45 60	20 x 36	50	15 × 30	11 × 11 × 28	94	8	2	2	7 8
	24 x 36	45	16 x 36	11 × 11 × 28	96	IO	2	2	9
8o	26×48	45	20 x 36	11 × 22 × 28	100	13	2	2	10

^{* 2,000} pounds.

[‡] One cylinder.

Table compiled by E. T. Skinkle, giving sizes of some Freezing Tanks, Piping and Moulds, in actual operation. DIMENSIONS OF ICE-MAKING TANKS.

	Remarks.					Special.		•	•		•
	Mumber Hours for Freezing each Mould.	4	2,9	36	48	52.2	48	84	84	57.6	22.6
sp	Number of Mould per ton Ice-mak ing Capacity.		3,0	3 00	50.4 ~	21.36	20.4	20.4	20.4	16	91
3	Net Weight of Ice from each Mould.	al of				 8 8 8				388	300
	Size of Moulda ein inches.	8×15×13	8×15×33	8×15×33	11X22X33	11×22×33	11×22×33	11×22×33	11 X 22 X 33	11 × 22 × 45 11 × 22 × 45 11 × 22 × 45	11×22×45
k.	Number of Ical InsT ni sbluoM	Ş	8	150	192	256	28 20 30 30 30	192	288	284 284 254 254	480
8	reet of Pipe pe ton Ice-making Capacity.	122	8	283	340	329	335	340	335	261	261
No. of Pipes, High. Length of Coils. Total feet of Pipe in Tank.		644	8	1,440	3,400	4.488	5,032	3,400	5,032	7,840 8,820	7,840
		15-4	15-0	15-0	17-0	17—0	17-0	17-0	17-0	28 18 0	0 80 80
		9	9	9	00	00	00	00	00	8 01	00
	Size of Pipe in inches,		н	н	н	н	н	н	H	HH	H H
	No. of Coils.	~	10	91	25	33	37	25	37	35	35
KS.	Thickness of Plates in inches,	3-16	3-16	3-16	4	44	mic.	rie	4.	-dej-dej	-(-(-
TANKS	Depth of Tank in inches.	33	33	33	33	33	33	33	33	48	400
S OF	Width of Tank. Feet & inches.	6—2	0-6	14—6	0-61	0-61	0-61	0-61	0-61	30-0	30-0
SIZE	Length of Tank. Teet & Inches. Width of		17-0	17-0	29-0	37-6	43-0	29-0	43-0	43-0	43-0
•	No. of Tanks	н	н	н	н	н	н	CI	2	Ha	N
	Ice-making Capacity.	н 8	(7)	S	10	123	15	20	30	283	00

Dimensions of one tank only are given in each instance. Average of 14-in. pipe per ton, 272 feet. ::

PURE WATER.

If properly distilled water, or ice made from such water, be evaporated slowly on a piece of platinum foil over a spirit-lamp or a Bunsen gas-burner, there should be no residuum whatever

In the manufacture of ice intended for domestic consumption, the use of pure water is a matter of paramount importance, consequently it is well to define what pure water is, and as very much the same requirements that are made by authorities with respect to potable water, also apply to ice, we will give some of the demands made in the former case. Pure water is soft, is transparent, has a certain amount of sparkle, is sufficiently aërated, has no matter held in suspension that is visible, is completely tasteless, and is either entirely colourless or has a slight bluish tint. The requirements of some authorities in the United States in this direction—great care being there exercised—are given by Prof. Siebel as follows: "I. Such water should be clear, temperature not above 15° C. 2. It should contain some air. 3. It should contain in 1,000,000 parts: Not more than 20 parts of organic matter. Not more than o'r part of albuminoid ammonias. more than 0.5 part of free ammonia. 4. It should contain no nitrates, no sulphuretted hydrogen, and only traces of iron, aluminium, and magnesium. Besides the mentioned substances, it should not contain anything that is precipitable by sulphuretted ammonia. 5. It must not contract any odour in closed vessels. 6. It must contain no saprophites and leptothrix, and no bacteria and infusoria in notable quantities. 7. Addition of sugar must cause no development of fungoid growth. 8. On gelatine it must not generate any liquefying colonies of bacteria."

SIMPLE RULES FOR ASCERTAINING THE QUALITY OF SO-CALLED MINERAL WATER.—(Frick Company.)

Water turning blue litmus paper red before boiling, which after boiling will not do so; and if the blue colour can be restored by warming, then it is carbonated (containing carbonic acid).

If it has a sickening odour, giving a black precipitate

with acetate of lead, it is sulphurous (containing sulphuretted

hydrogen).

If it gives a blue precipitate with yellow or red prussiate of potash by adding a few drops of hydrochloric or muriatic acid, it is chalybeate (carbonate of iron).

If it restores blue colour to litmus paper after boiling, it

is alkaline.

If it has none of the above properties in a marked degree and leaves a large residue after boiling, it is a saline water (containing salts).

TESTING BY REAGENTS.

If water becomes turbid or opaque by using the following reagents, it is not pure:—

With baryta water, indicating carbonic acid. With chloride of barium, indicates sulphate.

With nitrate of silver, indicates chloride.

With oxalate of ammonia, indicates lime salts.

With sulphide of hydrogen, slightly acid, indicates presence of antimony, arsenic, tin, copper, gold, platinum, mercury, silver, lead, bismuth, and cadmium.

With sulphide of ammonia, alkaloid by ammonia, indicates nickel, cobalt, manganese, iron, zinc, alumina, any

chromium.

With chloride of mercury or gold and sulphate of zinc, indicates organic matter.

FREEZING TANK OR BOX.

These are constructed of sheet iron and steel, and also of wood and cement. The amount of pipe required is about 250 feet of 2-inch pipe, or 350 feet of $1\frac{1}{4}$ -inch pipe, or their equivalent per ton of ice per twenty-four hours, in accordance with the temperature of the brine and the capacity of the machine. Less pipe than the above, says Prof. Siebel, is employed in the United States, even as low as 150 feet of 2-inch pipe, and 200 feet of $1\frac{1}{4}$ -inch pipe per ton of ice-making capacity (in twenty-four hours), but in that case the back pressure must be carried excessively low, which duly increases the consumption of coal and the wear and tear of the machinery.

in the freezing tank may be cooled on either

ation or the direct expansion system.

The size and length of pipe in the brine tank, it is recommended by the above-mentioned authority, should be arranged in such a manner that each row of moulds or cans is passed by an ammonia pipe on each side, preferably on the wide side of the mould or can. The series of pipes in the ice tank or box are connected by a manifold, the liquid ammonia entering the manifold at the lower extremity, and the vapour leaving by the suction manifold placed at the higher extremity of the refrigerating coils.

When working with the wet vapour of ammonia, the liquid must be admitted at the upper extremity of the refrigerating coils, and be drawn off to the compressor at their lower extremity.

Brine for Use in Refrigerating and Ice-making Plants.

A brine suitable for the above purpose can be made with from 3 to 5 lbs. of chloride of calcium, or muriate of lime, in accordance with its degree of purity, dissolved in each gallon of water. The density of this solution is about 23° Beaumé, its weight about $13\frac{1}{2}$ lbs. per gallon, and the freezing-point is -9° Fahr. As the above standard of density must be kept up, in order to prevent the brine from becoming congealed in the refrigerator, or the icemaking tanks or boxes, it is desirable to test it periodically with a salinometer.

In the best American practice first quality medium ground salt, preferably in bags for convenience of handling, is employed, the proportions being about 3 lbs. of salt to each gallon of water. The brine is made in a brine mixer, consisting of a water-tight box or tank about 4 ft. × 8 ft. × 2 ft., having a suitably perforated false bottom, and a small compartment, partitioned off at one extremity, communicating with the main compartment through an overflow situated at the upper end of the partition, and fitted with a large strainer, to prevent the passage into the small compartment of salt or foreign bodies. The water is admitted through a perforated pipe situated beneath, and running the full length of the false bottom, and the brine is removed through a pipe from the

upper part of the end compartment, at the lower extremity of which latter pipe is a strainer-box and strainer through which the brine passes before delivery into the brine-tank. A salt gauge, salinometer, or hydrometer is also placed in the small or end compartment.

The salt should be dissolved in the water until it reaches a density of about 90° by the hydrometer. To facilitate dissolution it is desirable to stir the salt in the mixer with some handy implement, the salt being shovelled in as fast as it can be got to dissolve.

By the use of this mixture the settlement of salt on the bottom, and on the coils in the brine tank, which inevitably results when the dissolution is effected directly in the latter, is avoided.

To maintain the strength of the brine it is recommended to suspend bags filled with the salt in the brine tank, or to pass the return brine through the above-described brine maker or mixer.

A cheap and easily constructed apparatus for mixing brine can be made out of an old barrel in which a perforated false bottom is fixed a short distance above the bottom, the water to form the solution being delivered to the space between the two bottoms, and an overflow pipe fitted with a suitable strainer and a well to receive a salinometer being provided near the top to draw off the brine.

SOLUTIONS OF CHLORIDE OF CALCIUM (CaCl2). (Manufacturer of Chloride of Calcium, U.S.)

Specific Gravity at 64° Fahr.	Degree Beaumé at 64° Fahr.	Degree Salino- meter at 64° Fahr.	Per cent. of Chloride of Calcium.	Freezing- point Degrees Fahr.	Ammonia Gauge. Lbs. per square inch at Freezing-point.
1.007	7		0.943	+31.50	46
1.014	2	8	1.886	+30.40	45
1.051	3	12	2.829	+29.60	44
1.028	4	16	3.772	∔ 28⋅80	43
1.032	5	20	4.715	∔ 28∙oo	42
1.043	6	24	5.658	+ 26·89	41
1.050	7	28	6.601	+25.78	40
1.028	8	32	7.544	+24.67	38
1.062	9	34	8.487	+23.26	37
1.073	10	40	9.430	+22.09	35.5

SOLUTIONS OF CHLORIDE OF CALCIUM (CaCl2). (Manufacturer of Chloride of Calcium, U.S.)

Specific Gravity at 64° Fahr.	Degree Beaumé at 64° Fahr.	Degree Salino- meter at 64° Fahr.		Freezing- point Degrees Fahr.	Ammonia Gauge, Lbs. per square inch at Freezing-point.
1.081 1.081	11 12 13	44 48 52	10·373 11·316	+20.62 +19.14 +17.67	34 32·5 30·5
1·105 1·114 1·112	14 15 16	56 60 64	13·202 14·145 15·088	+15.75 +13.82 +11.89	29 27 25
1·131 1·140 1·149	17 18 19	68 72 76	16.031 16.974 17.917	+ 9.96 + 7.68 + 5.40 + 3.12	23.2 21.2 20
1·158 1·167 1·176	20 21 22	80 84 88	18·860 19·803 20·746	- 0·84 - 4·44	18 15 12·5
1·186 1·196 1·205 1·205	23 24 25 26	92 96 100 104	21.689 22.632 23.575	- 8.03 -11.63 -15.23	10·5 8 6
1.546 1.536 1.546	27 28 29	104 108 112 116	24·518 25·461 26·404	-19.56 -24.43 -29.29	4 1.5 166 vacuum
1·257 1·268 1·279	30 31 32	120	27·347 28·290 29·233 30·176	-35·30 -41·32 -47·66 -54·00	5 ⁶⁶ 8·5 ⁶⁶ 12 ⁶⁶ 15 ⁶⁶
1.302 1.303	33 34 35	=	33.000 31.110	-44·32 -34·66 -25·00	10 ⁶⁶ 4 ⁶⁵ 1·5 lbs.

Properties of Solution of Chloride of Calcium. (Prof. Siebel, "Compend. of Mechanical Refrigeration.")

• •	_			•
Percentage by Weight,	Specific Heat.	Specific Gravity at 60° Fahr.	Freezing- point Degrees Fahr.	Freezing- point Degrees Cels.
I	o •996	1.000	31	-0.2
5	0.964	1.043	27.5	-2.5
10	0.896	1.087	22	-5.6
15	o.860	1.134	15	-9.6
20	0.834	1.182	5	-14.8
25	0.790	1.234	-8	-22.1

PROPERTIES OF SOLUTION OF CHLORIDE OF CALCIUM (CaCl2).

	(H. J.	(H. J. West & Co., Ltd.,		"Catalogue of ice-making and Kefrigeraling machinery.	J Ice-Ma	emg ana	Kejrigeran	ing Machin	, (c/)	
Degrees	Degrees on Various Scales	Scales.	Specific	_	Weight	Weight of 1 Gal. of Solution	Solution.	Specific	Freezin	Freezing Temp.
Salinometer.	Beaumé.	Twaddell.	Gravity at 60° Fahr. Water=1.	caCl 2 by Weight.	Water, lbs.	CaCl ₂ lbs.	Total lbs.	Heat of Solution.	Fahr.	Celsius.
24	9	6	1.043	5	806.6	0.521	10.43	0.964	27.5°	-2.5,
47	12	12	1.087	01	6.583	1.087	10.87	968.0	22.0°	-2.0%
.89	17	27	1.134	15	6.636	102.1	11.34	098.0	12.00	9.6-
76	23	36	1.182	20	9.426	5.364	11.82	0.834	2.0%	-14.8°
112	, 2 2 2 3	46	1.234	25	9.255	3.085	12.34	0.26c	-8.0%	-22.1°

PROPERTIES OF SOLUTION OF CHLORIDE OF SODIUM (COMMON SALT).

Degrees	Degrees on Various Scales.	Scales.	Specific	Percentage	Weight o	Veight of 1 Gal. of Solution	Solution.	Specific	Freezin	reezing Temp.
Salinometer.	Beaumé.	Twaddell.	Gravity at 60° Fahr. Water=1.	SALT, by Weight.	Water, lbs.	Salt, lbs.	Total lbs.	Heat of Solution.	Fahr.	Celsius.
02	, , , , , , , , , , , , , , , , , , ,	7	1.037		0.851	0.518	10.37	096.0	25.50	-3.8%
40	٠ <u>٥</u>	15.	1.073	.01	9.657	1.073	10.73	0.892	18.7°	-7.4°
.8	15		1.115	15	9.475	1.672	11.15	0.855	12.50	°0.11-
&	61	0,0	1.150	20.	0.500	2.300	11.50	0.820	6. I°	-14.4
001	24	38	161.1	2.5	8.923	2.611	16.11	0.783	0.20	-17.82

COMPARISON OF VARIOUS HYDROMETER SCALES.—(Yaryan.)

	Specific	Gravities.	C.	Jr.	-sn.		tric	1
Degrees Beaumé.	Standard adopted by U.S. Chem. Mfg. Ass. 15.5°. Sp. gr. = 145°04	Modulus 144'38. Custom in France.	Degrees Densimetric 15'5°	Degrees 'Iwaddell 60 Fahr. $1^{\circ} = 200 \text{ (Sp. gr.} - 1)$.	Degrees Brix. Official Prussian Hydrometer 15'6° C. Sp. gr. = $\frac{400}{400-Bx^{o}}$	Degrees Beck 12°5° C. Sp. gr. = $\frac{170}{170 - \text{Bk}^{\circ}}$	Degrees Brix Saccharimetric (per cent. Sugar).	Gay-Lussac (Centigrade).
0	1.000	1.0000	0.0	0.0	0.0	0.0	0.0	0.0
I	1.002	1.0070	0.7	1.4	2.8	I.5	1.8	0.4
2	1.014	1.0140	1.4	2.8	5.5 8.2	2.3	3.6	1.4
3	1.031	1.0212	2.I	4·2 5·6	8.2	2·3 3·5 4·6	1·8 3·6 5·4 7·1	2·1 2·7
4	1.058	1.0582	2.8	5.6	10.9	4.6	7.1	2.7
5	1.036	1.0380	3.6	7.2	13.9	5.9	6.0	3.5
6	1.043	1.0432	4.3	8.6	16.5	7.0	10.4	4.I
3 4 5 6 7 8	1.021	1.0510	4·3 5·1 5·8 6·6	10.5	19.4	5·9 7·0 8·3	12.6	3.5 4.1 4.8
8	1.028	1.0282	5.8	11.6	21.9	9.3	14.3	5.5
9	1.066	1.0665	0.0	13.2	24.8	10.4	16.1	6.2
10	1.074	I.0745 I.0825	7.4 8.2	14.8	27.5	11.7	18.0	6.9
11	1.000	1.0025		16·4 18·0	30.0 30.3	12.9	19.8	6·9 7·6 8·3
	1.098	1.0902	9.8	19.6	33.0	14.1	21.5	8.9
14	1.107	1.1022	10.7	21.4	30.0	16.4	25.3	9.7
15	1.112	1.1190	11.5	23.0	41.3	17.6	27:0	10.3
13 14 15 16	1.124	1.1242	12.4	24.8	44.3	18.8	23·3 25·2 27·0 28·9	11.0
17	1.133	1.1332	13.3	26.6	46.5	20.0	30.7	11.7
17	1.142	1.1422	14.2	28.4	49.7	21.2	32.6	12.4
19	1.121	1.1515	16.0	30.5	52.5	22.3	34.4	13.1
20	1.190	1.1607	16.0	32.0	55.2	23.5	36.2	12.8
2 I	1.169	1.1702	16.9	33.8	57.8	24.6	38.0	14.5
22	1.179	1.1795	1.7.9	35.8	49.7 52.5 55.2 57.8 60.7	25.8	40.0	15.2
23	1.188	1.1892	18.8	35·8 37·6	63.3	26.9	41.7	14·5 15·2 15·8 16·5
24	1.108	1.1992	19.8	39.6	99.I	28·I	43.6	16.2
25	1.208	1.5002	20.8	41.6	68.9	29.3	45.2	17.5
20	1.518	1.5102	21.8	43.6	71.6	30.4	47.3	17.9
27	1.229	1.2300	22.9	45·8 47·8	74.2	31.7	49.4	18.6
65	1.239	1.2402	23.9	47.8	77.2	32.8	21.5	19.3
29	1.50	1.2625	23.9 25.0 26.1	50.0	79:3 82:8	34°0 35°2	53.2	20.0
30	1.272	1.2735	27.2	52·2 54·4	85.5	35 4	53·2 55·1 57·0 58·9 60·9	20.7
1 2	1.583	1.5820	28.3	56.6	85.2	37.5	57.0	21.4 21.4
33	1.295	1.2960	29.5	20.0	91.1	36°4 37°5 38°8	90.0	22.8
34	1.306	1.3080	30.6	59.0	93.7	39.9	62.7	23.4
5	1:318	1.3200	31.8	63.6	96.5	41.0	64.7	24·I

Comparison of Various Hydrometer Scales. — (Continued.)

	Specific	Gravities.	Degrees Densimetric 15'5 C.	Degrees Twaddell 60 Fahr. 1° = 200 (Sp. grr).	Official Prus- meter 15'6° C. 400 400—Bxº		Degrees Brix Saccharimetric (per cent, Sugar).	e).
	U.S. 15°. B		12.6	Ę.	4 %	Degrees Beck 12.5° C. Sp. gr. = $\frac{170}{170 - Bk^0}$	ığ .	Gay-Lussac (Centigrade). Sp. gr. = roo_Co
Degrees Baumé.	Standard adopted by U.S. Chem. Mfg. Ass. 15 5°. Sp. gr. = 145.04 Sp. gr. = 145.04	Cus- e.	ric	8 .	egrees Brix. Official P sian Hydrometer 15'6° Sp. gr. = \frac{400}{400-Bx^0}	2.2 -B	ses Brix Saccharir (per cent. Sugar).	Centigr 100 100–Cº
3au	d b	ice	ıetı	lell 8 %	6 te 6	13 ck	Sugar	Cen 100 100
S I	opted - Ass. 145'04 145'04	.38 rai	ısin	Sp ad	9 4 4	Bec	S +	
ě	ado [fg. = 1	144 n F)en	#8	ees Brix. Hydrom Sp. gr.=	8 5	.¥ 8	y-Lussac (Sp. gr. =
) eg	M. M	lus m i	, s	8 1	P. B.	egrees Sp. gr.	Ser B	P. B.
	Chem. Mfg. Ass. 15 Chem. Mfg. Ass. 15 Sp. gr. = 145'04 145'04—1	Modulus 144'38. (tom in France.	Ĕ	are To	Degrees Brix. sian Hydrom Sp. gr.=	Deg S	8-2	S S
ł	Ch	™	<u>ق</u>		Siis	,	👸	Ü
	$\frac{1}{N}$				<u> </u>		 -	
36	1.330	1.3320	33.0	66∙0	99.2	42.2	66.7	24.8
37 38	1:342	1.3442	33.0 34.5	68.4	101.9	43.3	68.6	25·5 26·2
38	1.368	1.3570	35.2	71.0	104.7	44.6	70.7	
39	1.308	1.3700	35.2 36.8 38.1	73.6	107.6	45.8	72.7	26.9
40	1.381	1.3830	39.4	73.6 76.2 78.8 81.6	113.2	46·9 48·0	74°7	27.6
41 42	1.408	1.4100	40.8	81.6	112.9	49.3	78.8	28·3 28·9
43	1.421	1.4240	42·I	84.2	118.2	50.4	80.8	29.6
44	1.436	1.4380	43.2	87.0	121.3	51.5	82.0	30.3
45	1.450	1.4525	45.0 46.5 48.0	90.0	124.1	51·5 52·8	85·1 87·2	31.0
46	1.462	1.4675	46.5	93.0	126.7	53.0	87.2	31.7
47	1.479	1.4827	48.0	96.0	129.7	55·í	89.4	32.4
48	1.492	1·4980 1·5135	49.5 51.0	105.0 30.0	132·4 135·1	50.3	93.6	33.8
50	1.210 1.26 1.242	1.2300	52.6		137.9	57.4 58.6	93.0	34.2
51	1.242	1.5460	54.2	108.4	140.6	59.8	::	35.5
52	1.226 1.226	1.2030	55·9 57·6	111.8	143.4	61.0 20.8		35.9
53	1.226	1.2800	57.6	115.5	146.2	62.2	•••	35·9 36·6
54 55 56	1.263	1·5965 1·6150	91.1 29.3	118.0	148.9	63.3	•••	37.2
55	1.611	1.6335	62.9	122.2	151.7	64·5 65•7	•••	37·9 38·6
57	1.648	1.6520	64.8	125.8	157.3	66.9	::	39.3
57 58	1.666	1.6715	66.7	133.4	160.0	68· o		40.1
59 60	1.686	1.6910	68.6	133.4	162.8	69.2		40.7
60	1.406	1.7110	70.6	141.2	165.5	70.4	••	41.4
61	1.726	1.7315	72.6	145.2	168.3	71.5	••	42.1
62 63	1.747 1.768	1·7525 1·7740	74·7 76·8	149.4	171·0 173·8	72.7	••	42.8
64	1.790	1.7950		158.0	176.5	75.0	••	43°4 44°1
65	I·8I2	1.8185	79·0	153.6 158.0 162.4	179.3	73·8 75·0 76·2	•••	44.8
65 66	1.825	1.8420	83.5	167.0	182.0	77.4		45.2
67 68	1.859	1.8660	85·a	171.8	184.8	77.4 78.6	••	46.2
68	1.883	1.8910	88.3	176.6	187.5	79·7 80·9	••	46.9
69	1.907	1.9121	90.7	181.4	190.2	85.1 80.0	••	47.6
70 72·5	1.000	1.9410 2.0085	93.3	200.0	193.0	85.0	**	48·3
1-3] - 550	,		200 0	050		300
				<u></u>	·			

FREEZING TIMES FOR DIFFERENT TEMPERATURES AND THICKNESSES OF CAN ICE.

(Siebert.)

Thickness.		r in.	2 in.	3 in.	4 in.	5 in.	6 in.	7 in.	8 in.	9 in.	ro in.	ıı ii.	12 in.
Temperature		0,35	1.58	2.86	5.10				20*4		31.8	38.2	45.8
••	12°			3.12						28.4			50.4
,,	140			3,20					25 C		39.0		56.0
,,	16°			3.94					28.0		43'7	53.0	63.0
,,	180			4.20						40.2			
,,	20°	0.28	2.35	5.52	9.30	14.6	51,0	28.2	37.3	47.5	58.3	70.2	84.0
,,	22°				11.5	17.2	25.5	34.3	44.8	56.4	20.0		100.0
,,	24°	0.88	3.20	7.86	14.0	21.0	31.2	12.8	560	71.0	87.5	100.0	126.0

TIME REQUIRED FOR WATER TO FREEZE IN ICE CANS. (The Triumph Ice Machine Company, Catalogue.)

Cans, size, 6 in. by 12 in. by 24 in. Weight of cake, 50 lbs. Time to freeze, 20 hours.

Cans, size, 8 in. by 18 in. by 32 in. Weight of cake, 100 lbs. Time to freeze, 36 hours.

Cans, size, 8 in. by 16 in. by 40 in. Weight of cake, 150 lbs. Time to freeze, 36 hours.

Cans, size, 11 in. by 22 in. by 32 in. Weight of cake, 200 lbs. Time to freeze, 55 hours.

Cans, size, 11 in. by 22 in. by 44 in. Weight of cake, 300 lbs. Time to freeze, 60 hours.

Cans, size, 11 in. by 22 in. by 57 in. Weight of cake, 400 lbs. Time to freeze, 60 hours.

Note.—Temperature of bath 14 to 18 degrees Fahrenheit. As a rule, the higher the bath temperature the slower the process of freezing, but the finer and clearer the ice.

STORING ICE.

For storing purposes ice should be clear, solid, and devoid of core. In America some persons insist that ice for storage should not be made at temperatures higher than 10° to 14° in brine tank.

The first requisite for a storage house for artificial ice, as also for natural ice, is of course the best possible insulation; other necessary points to be attended to are drainage and ventilation. The best shape for an ice storage house is square, or as nearly approaching this form

as possible, and the roof should have a good pitch. An ante-room or lobby is also desirable, as by the provision of this latter the necessity for the frequent opening of the main store is done away with.

To preserve the ice, the storage rooms as well as the ante-chambers or lobbies must be refrigerated, and the amount of the latter required may be roughly estimated, according to Prof. Siebel, at from about ten to sixteen British thermal units of refrigeration per cubic feet contents for twenty-four hours. About one foot of 2-inch pipe (or its equivalent in other size pipe) per fourteen to twenty cubic feet of space is frequently allowed, says the same gentleman, in ice storage houses for direct expansion, and about one-half to one-third more for brine circulation. The pipes should be located on the ceiling of the ice storage house.

The ventilation of an ice storage house should be carefully attended to, and ventilators fitted with suitable regulators should be provided both in the highest part of the roof and also in the gable ends. The drainage should be such as to absolutely prevent the accumulation of any moisture beneath the bed of ice. It is recommended to paint an ice store white, preferably with a mineral paint such as barytes, or

patent white.

Respecting the best method to adopt for packing the ice in the store, considerable diversity of opinion seems to exist. It is well to provide a bed of from eighteen inches to two feet of cinders, as this tends to improve the drainage of the house. In one method the blocks are placed on edge and as closely packed together as possible, the blocks in each succeeding layer being placed exactly over those beneath and all breaking of joints being avoided. The ice is covered between the times of storing with dry sawdust or soft wood shavings, and the uppermost layer is invariably covered with dry sawdust or shavings.

Mr. R. Thompson, writing to the Canadian Farming World, says that in filling the house he puts the ice on edge, placing every alternate layer crossways, which plan, he claims, enables ice to keep better and come out easier.

Others recommend that the ice be stored with alternate ends touching, and alternately from one and a half to two inches apart, so as to prevent the ice from freezing together. The cakes or slabs of ice should not be parallel to each other, and storage should only be made when the temperature is at or below freezing. Or, again, $\frac{1}{2}$ -inch strips placed between the layers of ice in the store so as to separate the cakes or blocks top, side, and bottom, from all others in the house.

For packing the ice, sawdust, rice chaff, straw, hay—marsh or prairie hay being said to be preferable—are employed, the latter materials being the best, and rice chaff being capable of being dried and re-used. Six inches of well-packed hay should be placed between the ice and the walls, and no covering until the store is full.

A cubic foot of ice is taken to weigh 57.5 lbs. approximately at 32° Fahr. A cubic foot of water frozen at 32° will make 1.0855 cubic foot of ice, thus showing an expansion of 8.5 per cent. due to freezing. A cubic foot of pure water at 39° Fahr., its point of greatest density, weighs 62.43 lbs. Fifty cubic feet of ice, as usually stored, equals about one American or short ton of ice (2000 lbs.), or 62 cubic feet one English ton. In small ice houses, in which the ice is closely packed, a short ton of ice can be got into from 40 to 45 cubic feet.

When withdrawing ice from a store, breaking out bars for bottom and side breaking are required, and if properly skilled assistance is not available a considerable amount of the ice will in all probability be broken up and wasted.

The wastage of ice in an ice store not artificially cooled from January to July is, in the United States, at the rate of about o'r lb. of ice per twenty-four hours for each square foot of wall surface, or say from 5 to 10 per cent. of the ice stored during the six months.

The amount of heat that will pass through a square foot of ice one inch in thickness is put at 10 British thermal units per hour for each degree Fahrenheit difference between the respective temperatures on each side of the sheet of ice.

In handling and selling ice, the waggons should be clean and sanitary, the men in charge should avoid walking about in them with dirty boots, and blocks of ice should not be deposited and slid about on filthy pavements. These matters are attended to in the United States, but here they

are totally neglected.

In the United States the selling and delivery of ice is generally done by the coupon system, which is thus described by Prof. Siebel: "It is a system of keeping an accurate account with each customer of the delivery of and the payment for ice by means of a small book containing coupons, which in the aggregate equal 500 or 1000 or more pounds of ice taken by the customer every time ice is delivered. These books are used in the delivery of ice in like manner as mileage books or tickets are used on the railroad. A certain number of coupons are printed on each page, each coupon being separated from the others by perforation, so that they are easily detached and taken up by the driver, when ice is delivered. Such books are each supplied with a receipt or due bill, so that if the customer purchases his ice on credit, all that is necessary for the dealer to do is to have the customer sign the receipt or due bill and hand him the book containing coupons equal in the aggregate to the number of pounds of ice set forth in the receipt or due The dealer then has the receipt or due bill, and the customer has the book of coupons. The only entry which the dealer has to enter against such purchaser in his books is to charge him with coupon book number, as per number on book, to the amount of 500, 1000, or more pounds of ice, as the value of the book so delivered may be. The driver then takes up the coupons as he delivers the ice from day to day."

SECTION IV.

INSULATION.

In addition to non-conducting qualities, a good insulating material should be non-odorous, non-hygroscopic, not liable

to silt, and both vermin and fire-proof.

Perfect insulation would be attained when there was absolutely no transmission of heat through the walls of the building, which state of things is practically an impossibility. Every one should, however, endeavour to secure as near an approximation to the above as possible, and it should be remembered that poor insulation is a constant drain upon the machinery and pocket of the owner, as a very large percentage of the actual work of a refrigerating machine is that required to make up for the transfer of heat through the walls, floor, and ceiling of the cold store, resulting from defective insulation.

In the following tables the results of a number of tests as to the values of different insulating materials are given, and from these tables may be deduced sufficient information to enable an intelligent choice to be made. In Australia pumice stone is much used, and is said to give good results. In this country and the United States silicate cotton or slag-wool; cork, in slabs, bricks, and granulated; and charcoal are employed, and there is something to be said in favour of each of these materials.

When charcoal is employed it should be well dried, and packed as nearly as possible to a consistency of 11 lbs. per cubic foot. Silicate cotton or slag-wool is usually packed to a consistency of about 12 lbs. per cubic foot, one ton equalling about 187 cubic feet. Some engineers prefer, however, to use 13 lbs. per cubic foot.

An advantage possessed by granulated cork is its extreme lightness. One cubic foot weighs only $4\frac{1}{3}$ lbs., and one ton occupies about 450 cubic feet.

TRANSMISSION OF HEAT THROUGH VARIOUS INSULATING STRUCTURES.—(Starr, American Warehousemen's Assoc.)

Col. I. gives B.T.U. per square foot per day per degree of difference of temperature. Col. II. gives meltage of ice in pounds per day by heat coming through 100 square feet at a difference of 40°.

One 7 in board at in minoral word names one 7 in	Col. I.	Col. II.
One $\frac{7}{8}$ -in. board, $2\frac{1}{2}$ -in. mineral wool, paper, one $\frac{7}{8}$ -in. board	3.918 3.918	9 3 '4
boards and paper	3.30	92.9
One $\frac{7}{8}$ -in. board, paper, 2-in. calcined pumice, paper, and $\frac{7}{8}$ -in. board	3.38	95.3
One 3-in. board, paper, 3-in. sheet cork, paper, one 3-in. board	2· IO	60.0
Double boards and papers, 4-in. granulated cork, double boards and paper	1.70	48·o

RESULTS OF TESTS TO DETERMINE THE NON-CONDUCTIVE VALUES OF DIFFERENT MATERIALS.

(H. F. Donaldson, M.I.C.E., Proceedings, Inst. C.E.)

EXPERIMENT No. 1.

	Thickness		Weigh	Loss after		
	of Insulating Material.	Original Weight of Ice.	Twenty- four Hours.	Seventy- two Hours.	Seventy- two Hours.	
	Inches.	Ozs.	Ozs.	Ozs.	Per cent.	
Peat (compressed and set in Fossil			_			
Meal)	9	95	81	59 56 40 1	37.89	
Charcoal	II	96]	$79\frac{1}{2}$ $73\frac{1}{2}$	56	41·97 56·21	
Silicate Cotton	41/2	95 96 1 92 1	731/2	40 1	56.51	
Magnesia and As- bestos Fibre	41/2	93	73	40½	56.45	
	<u> </u>	<u> </u>				

NOTE.—The author thought it undesirable to consider further compressed peat set in fossil meal, as he found by experiment its powers of absorption of moisture to be so great as to constitute in his opinion a source of danger.

EXPERIMENT No. 2.

 Thicknes		Original	W	Loss after		
_	of Insulating Material.	Weight	Twenty- four Hours	Forty- eight Hours.	Ninety- six Hours.	Ninety- six Hours.
Silicate Cotton Sawdust Peat Charcoal	Inches. 6 9 9 9	Ozs. 104 103½ 104 104	Ozs. 883 861 771 883	Ozs. 76 3 71 56 78 1	0zs. 58½ 48 26½ 60½	Per cent. 43.75 52.62 74.75 41.82

EXPERIMENT No. 3.

		Thickness	Original	Weigh	Loss after	
		of Insulating Material.	Weight of Ice.	Twenty- four Hours.	Seventy- two Hours.	Seventy- two Hours.
Silicate Cotton Charcoal		Inches. 9 II	Ozs. 92 92	Ozs. 83½ 82¾	Ozs. 72½ 70½	Per cent. 21.19 23.36

EXPERIMENT No. 4.

	Thickness	Original	Weigh	Loss after		
	of Weight Insulating of Material. Ice.		Twenty- four Hours.	Ninety- six Hours.	Ninety- six Hours.	
Silicate Cotton	Inches.	Ozs.	Ozs.	Ozs.	Per cent.	
(loosely packed)	0	110	103	841	23.41	
Silicate Cotton	, ģ	110	1013	8o3	26.20	
Charcoal	11	110	1001	79	28.18	
Vegetable Silica	11	110	1017	763	30.22	
Diatomite	11	110	99	73	32.95	

RESULTS OF TESTS TO DETERMINE THE NON-CONDUCTIVE VALUES OF VARIOUS MATERIALS.

(Dr. Wm. Wallace.)

MATERIALS.			Cubic Centimetres (grammes) of water melted in 12 days.	Average c.c.'s per day.
Silicate Cotton			0.470	780
	• •	• •	9,470	789
Flake Charcoal			11,010	917
Felt			11,760	980
Fossil Meal			12,530	1,044
Twig Charcoal			13,590	1,132
Plain Cork Slabs	• •	• •	14,020	1,168
Tarred Cork Slabs			14,610	1,217
Broken Lump Charcoal	• •		15,916	1,326
Ashes	• •	••	23,316	1,943

Coleman's method was used in making the above tests, with walls 6 in. thick.

RATE OF PASSAGE OF HEAT THROUGH VARIOUS MATERIALS.—(Alex. Marcet.)

British Thermal Uni	its per ho	our per su 6 in. thic		foot thro	ugh mate	erials
	T = 60°		T =	50°	T = 40°	
	Dry.	Wet.	Dry.	Wet.	Dry.	Wet.
Silicate Cotton Cow Hair Charcoal Sawdust Infusorial Earth Cork Bricks	4·11 4·11 4·70 6·75 10·00 5·87	14.05 8.80 12.30 15.60	2·34 2·34 2·93 4·40 6·18 3·20	8·57 5·30 7·50 9·60 —	1·17 1·17 1·76 2·34 3·57 2·90	6·70 3·50 4·40 5·50

T = The Difference of Temperature (Fahr.) on the two sides of the material.

RESULTS OF TESTS ON THE HEAT CONDUCTIVITY OF DIFFERENT SUBSTANCES.

(Various authorities.)

(Silicate Cotton being taken at 100.)

SUBSTANCE.	C. E.	J.J.Cole-	W. H.	Prof.
	Emery,	man,	Collins,	Jamieson
	1881.	1884.	1891.	1894.
Silicate Cotton or Slag Wool Hair-Felt or Fibrous Composition Papier-Maché Kieselguhr Composition Sawdust Charcoal Cotton Wool Sheep's Wool Pine Wood (across the grain) Loam Gasworks Breeze or Coal Ashes Asbestos	100 122 132 150 240 229	100 117 — 136 163 140 122 136 — —	100 114 147 — 142 — — — — — — 299 179	100 112 111 112 ————————————————————————

Table giving the Relative Heat Conductivity of Various Boiler-covering Materials.

(The "American Engineer.")

Silicate Cotton or M	[ineral	Wool	• •			100
Hair Felt				••	••	117
Cotton Wool						122
Sheep's Wool			••	• •	••	136
Infusorial Earth	••		••			136
Charcoal	••			••	••	140
Sawdust			• •		• •	163
Gasworks Breeze	••			••		230
Wood and air space	• •	• •			••	280

RESULTS OF EXPERIMENTS REGARDING NON HEAT-CON-DUCTING PROPERTIES OF VARIOUS SUBSTANCES.— (Prof. J. M. Ordway.)

	Coverings 1 inch thick.		Pounds of Water heated 10° F. per hour by 1 sq. foot.
, 1	"Silicate Cotton" or "Slag Wool"	•••	13.0
2	Paper		140
* 3	Cork Strips, bound on	• •	14.6
1 4	Straw Rope, wound spirally	• •	18.0
5	Loose Rice Chaff	••	18.7
1 6	Blotting Paper, wound tight	• •	21.0
/ 7	Paste of Fossil Meal and Hair	• •	16.7
8		• •	21.0
1) 9	Paste of Fossil Meal with Asbestos	• •	22.0
1) 10		• •	27.0
(11	Paste of Clay and Vegetable Fibre		30.9
12		• •	30.9
13	Asbestos Paper, wound tight		21.7
14			48·o
15	Fine Asbestos		49.0
ığ	Sand	• •	2.16

^{*} These substances are not well suited for covering heated surfaces—owing to their nature they soon become carbonised.

† Hard substances that, with the action of the heat, break, powder,

and fall off.

N.B.—The Asbestos of 15 had smooth fibres, which could not prevent the air from moving about. Later trials with an Asbestos of exceedingly fine fibre have made a somewhat better showing, but Asbestos is really one of the poorest non-conductors. By reason of its fibrous character it may be used advantageously to hold together other incombustible substances, but the less the better.

NON HEAT-CONDUCTING PROPERTIES OF VARIOUS SUB-STANCES.—(From "Engineering.")

Prepared Mixtures, for Covering Boilers, Pipes, &c.	Pounds of Water heated 10° Fahr, per hour, per square foot.
Slag Wool (Silicate Cotton) and Hair Paste	10.0 lbs.
Fossil Meal and Hair Paste	10.4 ,,
Paper Pulp alone	14.7.,
Asbestos Fibre, wrapped tightly	17.9 "
Fossil Meal and Asbestos Powder	26.3 "
Coal Ashes and Clay Paste, wrapped with Straw	29.9 ,,
Clay, Dung, and Vegetable Fibre Paste	39.6 "
Paper Pulp, Clay and Vegetable Fibre	44.6 ,,

RESULTS OF EXPERIMENTS REGARDING NON HEAT-CON-DUCTING PROPERTIES OF VARIOUS SUBSTANCES.

(Walter Jones, "Heating by Hot Water.")

Frame Filled with				Left for	Highest Temp. Registered.
Leroy's Boiler-covering Asbestos Powder Hair Felt	ng Con	npositio	on	3 hours 4 " 9 " 9 "	94° 86° 77° 76°

HEAT IN UNITS TRANSMITTED PER SQUARE FOOT PER HOUR THROUGH VARIOUS SUBSTANCES.

(Peclet.)

Materials.	Units of heat trans- mitted.	Materials.	Units of heat trans- mitted.
Gold	625 600 595 520 230 225 178 113 24 14 6-6 4-8 4-8 3-8 2-1; 1-7	Guttapercha India-rubber Brickdust, sifted Coke, in powder Iron filings Cork Chalk, in powder Charcoal (wood) in powder Straw, chopped Coal, powder sifted Wood ashes Mahogany dust Canvas, hempen new Calico, new Writing-paper, white Cotton and sheep's wool Eiderdown Blotting-paper, grey	1·37 1·36 1·33 1·29 1·26 1·15 0·86 0·53 0·54 0·53 0·52 0·41 0·34 0·32 0·31 0·26

RELATIVE AND ABSOLUTE THERMAL CONDUCTIVITY OF SUBSTANCES USED AS LAGGING FOR STEAM BOILERS.—
(Professor Jamieson.)

RESULTS OF THE TESTS.

Name of Material.	Weight of Sample (including Tin).	Total fall of Tempera- ture in 120 minutes,	Thermal Conductivity in Absolute Measure.	Conductivity as Compared with Dry Still Air.	
Dry air	1bs. oz. 7 2 5 15 7 13 7 6 9 9 8 12	Deg. Cent. 6·0 21·5 30·0 29·0 29·0 35·5 34·5 37·5	0.0000558 0.0002689 0.0003613 0.0004336 0.0004424 0.0004550 0.0005019	1·00 4·82 6·47 6·95 7·77 7·93 7·98 8·99	

* The outside diameter of this sample was about \(\frac{1}{4} \) in. smaller than the inside diameter of the middle tin-case or vessel, and it had consequently a slight advantage over the other samples in having a thin layer of air between its outer surface and the latter.

† The silicate cotton was pressed together tightly, and thus its conductivity appears greater than would have been the case had it been

more loosely packed.

† The Kieselguhr employed consisted on the average of Silica 83.8, Magnesia 0.7, Lime 0.8, Alumina 1.0, Peroxide of Iron 2.1, Organic Matter 4.5, Moisture and Loss, 7.1. It was employed in conjunction with 10 per cent. of binding material, viz., fibre and mucilaginous extract of several vegetable matters.

§ Papier maché composition, consisting of paper pulp mixed with clay

and carbon, together with hair and fragments of hemp rope.

A lighter modification of above.

The quantity of heat in units, transmitted through one square foot of plate per hour, may be found thus: Subtract

the temperature of the cooler side from that of the hotter side of the plate, then multiply the result by the number in the table on p. 121 corresponding to the material used, and divide the product by the thickness of plate in inches. Thus an iron plate 2 in. thick, having a temperature of 60° on one side and 80° on the other, will transmit $80-60 \times \frac{230}{2} = 2300$ units of heat per square foot per hour.

HEAT-CONDUCTING POWER OF VARIOUS SUBSTANCES, SLATE BEING 1000.—(Molesworth.)

Slate .		. 1,000	Chalk				564
Lead .		. 5,210	Asphalt				45 I
Flagstone		. 1,110	Oak .			•	336
Portland stor	ıe	. 750	Lath and	plaste	er		255
Brick .		600 to 730	Cement	•			200
Fire-brick		. 620					

Tests regarding Conductivities of Asbestos and Kieselguhr.—(J. G. Dobbie.)

RESULTS OF TESTS.

	Asbestos.	Kieselguhr Com- position.		
	Water Condensed in Inches.	Water Condensed in Inches.		
After 15 minutes	44 34 355 377	2 1 2 2 2 2 2 2 8		
Totals in one hour	143	91		

RESULTS OF DIFFERENT EXPERIMENTS ON THE HEAT CONDUCTIVITIES OF VARIOUS SUBSTANCES.—(W. H. Collins.)

(Silicate cotton being taken as 100.)

Substance.	C. E. Emery. 1881.	J. J. Coleman.	W. H. Collins. 1891.	Prof. Jamieson. 1894.
Fossil meal composition Cement with hair-felt Silicate cotton or slag wool Hair-felt or fibrous composition Papier-maché Kieselguhr composition Sawdust Charcoal Cotton wool Sheeps' wool Pine wood (across the grain) Loam Gasworks breeze or coal ashes Asbestos	83 100 122 132 150 240 229	 100 117 136 163 140 122 136 	100 114 147 142 299	70 93 100 112 111 112

EXPERIMENTS BY T. B. LIGHTFOOT AND G. A. BECKS.

EXPERIMENT No. 1.

Duration of experiment, 48 hours. Average temperature of room or chamber, 90° F.

A piece of ice 23 lbs. in weight was placed in a zinc box 12 in. cube, and covered with 2 in. silicate cotton, this latter being provided with an outer cover, also of zinc. When the ice was taken out it weighed 10½ lbs., showing a loss of 12½ lbs.

12½ lbs. × 142 (latent heat of ice) = 1775 thermal units passed through in 48 hours. $\frac{1775}{48} = 36.979166$ thermal units passed through in 1 hour.

Difference in temperature between inner box and outer air = 58° F. $\frac{36.9}{68} = 0.63$ thermal unit transmitted per hour per degree difference in temperature. Area of zinc boxes: inner box, 6 sq. ft.; outer, 10.6 sq. ft.; mean, 8.1 sq. ft.

Thermal units transmitted through the three areas—

$$\therefore \frac{0.63}{6} = 0.102, \frac{0.63}{8.1} = 0.04, \frac{0.63}{10.9} = 0.020$$

which being multiplied by 2 for the thickness of cotton, gives thermal units per hour, per degree difference in temperature, per square foot, per inch of thickness, as follows: 0'210 inner tin, 0'118 outer tin, 0'14 mean.

EXPERIMENT No. 2.

Duration, 48 hours. Average temperature of room, 00° F.

A piece of ice 26 lbs. in weight, covered with 6 in. of charcoal. When taken out it weighed $7\frac{1}{2}$ lbs., showing a loss of $18\frac{1}{2}$ lbs. $18.5 \times 142 = 2627$ thermal units in 48 hours. $\frac{24\frac{1}{2}7}{2} = 54.72$ thermal units per hour. $\frac{54\frac{1}{2}7}{2} = 0.94$ thermal units per hour, per degree difference in temperature between inner box and outer air. Area of tins: inner box, 6 sq. ft.; outer, 24 sq. ft.; mean, 13.5 sq. ft.

The number of thermal units transmitted per hour, per degree, per square foot—

$$\frac{0.04}{9} = 0.12, \frac{0.04}{13.2} = 0.060, \frac{0.04}{5} = 0.030$$

which being multiplied by 6 for the thickness of charcoal, gives thermal units transmitted per hour, per degree, per square foot, per inch of thickness; 0.90 inner tin, 0.234 outer tin, 4.14 mean.

FORMULA FOR ASCERTAINING UNITS OF REFRIGERATION (R)
REQUIRED IN 24 HOURS, TO CARRY OFF HEAT
RADIATED THROUGH SQ. FT. (f) OF WALL, FLOOR,
AND CEILING.

$$R = fn(t - t_1)HU$$

HU = heat units of 772 ft. lbs., t = internal temperature, $t_1 =$ external temperature, and n = heat units transmitted per 24 hours per sq. ft. of surface for difference of 1° Fahr. between internal and external temperature.

TRANSMISSION OF HEAT THROUGH VARIOUS INSULATING STRUCTURES.—(Starr, American Warehousemen's Assoc.)

Insulating Structures.	B. T. U. per sq. ft. per day per deg. of difference of tempera- ture.	Meltage of ice in lbs. per day by heat coming through 100 sq. ft. at a difference of 40°.
§-in. oak, paper, I-in. lampblack, 7-in. pine		160'7
(ordinary Stock family refrigerator)	5.7	
3-in. board, 1-in. pitch, 3-in. board	4.90	138.0
Four 3-in. spruce boards, two papers, solid,	0	
no air-space	4.58	120.0
Two double boards and paper (four 7-in.		
boards), and one air-space	3.41	102.0
7-in. board, 2-in. pitch, 7-in. board	4.52	119.7
7-in. board, 21-in. mineral wool, paper,		
7-in. board	3.62	101.9
Two 7-in. double boards, and two papers,		
1-in. hair felt	3.318	93'4
Two 3-boards and paper, 1-in. sheet cork,		
two 7-in. boards and paper	3.30	92.9
7-in. board, paper, 2-in. calcined pumice,		
paper, and 7-in. board	3.38	95.5
Four double 7-in. boards with paper between		1
(eight boards), and three 8-in, air-spaces	2.7	76.0
Hair quilt insulator, four boards, four quilts	•	
hair	2.217	70'9
7-in. board, 6-in. pat. silicated straw-board,	, ,	' '
air-cell finished inside with thin layer of		
patent cement	2.48	69.8
7-in. board, paper, 3-in. sheet cork, paper,	_ 75	'
7-in. board	2.10	60.0
Two 7-in. boards and paper, 8-in. mill		
shavings and paper, two ?-in. boards and	1	,
	1.35	38.3
paper	1.80	50.7
Same, slightly moist	2.10	60.0
Same, damp	2 10	55.5
Double boards and paper, 1-in. air, 4-in.	1.50	33.6
sheet cork, paper, 7-in. board		
Same, with 5-in. sheet cork	0.90	25.3
3-in. board, paper, 1-in. mineral wool, paper,	4.6	120:0
7-in. board.	4.6	130.0
Double boards and papers, 4-in. granulated		48.0
cork, double boards and paper	1.2	48.0
	!	

WALLS FOR COLD STORES.

The following materials and dimensions have been recommended for walls of cold chambers:—

14 in. brick wall, $3\frac{1}{2}$ in. air space, 9 in. brick wall, 1 in. layer of cement, 1 in. layer of pitch, 2 in. by 3 in. studding, layer of tar paper, 1 in. tongued and grooved boarding, 2 in. by 4 in. studding, 1 in. tongued and grooved board, layer of tar paper, and, finally, 1 in. tongued and grooved boarding, the total thickness of these layers or skins being 3 ft. 3 in.

36 in. brick wall, I in. layer of pitch, I in. sheathing, 4 in. air space, 2 in. by 4 in. studding, I in. sheathing, 3 in. layer of mineral or slag-wool, 2 in. by 4 in. studding, and, finally, I in. sheathing; total thickness, 4 ft. 7 in.

14 in. brick wall, 4 in. pitch and ashes, 4 in. brick wall, 4 in. air space, 14 in. brick wall; total thickness, 3 ft. 4 in.

14 in. brick wall, 6 in. air space, double thickness of 1 in. tongued and grooved boards, with a layer of water-proof paper between them, 2 in. layer of the best quality hair felt, second double thickness of 1 in. tongued and grooved boards, with a similar layer of paper between them; total thickness, 2 ft, 2 in.

14 in. brick wall, 8 in. layer of sawdust, double thickness of 1 in. tongued and grooved boards, with a layer of tarred waterproof paper between them, 2 in. layer of hair felt, second double thickness of 1 in. tongued and grooved boards, with a similar layer of paper between them; total thickness, 2 ft. $4\frac{1}{2}$ in.

Brick wall, 3 in. scratched hollow tiles, 4 in. silicate cotton or slag-wool, 3 in. scratched hollow tiles, and layer

of cement plaster.

Brick wall, I in. air spaces between fillets or strips, I in. tongued and grooved boarding, two layers of insulating paper, I in. tongued and grooved boarding, 2 in. by 4 in. studs, 16 in. apart, spaces filled in with silicate cotton, I in. tongued and grooved boarding, two layers of insulating paper, air spaces between fillets, or strips I in. by 2 in. spaced 16 in. apart from centres, I in. tongued and grooved boarding, two layers of insulating paper, and I in. tongued and grooved boarding.

Brick or stone wall, well coated on inside with pitch or asphaltum, 2 in. by 3 in. studding, 24 in. centres spaces between filled in with silicate cotton, $\frac{3}{4}$ in. rough tongued and grooved boarding, two layers waterproof insulating paper, $\frac{3}{4}$ in. rough tongued and grooved boarding, 2 in. by 3 in. studding 24 in. centres in spaces between, $\frac{3}{4}$ in. rough tongued and grooved boarding, two layers of waterproof insulating paper, $\frac{3}{4}$ in. rough tongued and grooved boarding, 2 in. by 3 in. studding, 24 in. centres spaces between filled in with silicate cotton, $\frac{3}{4}$ in. rough tongued and grooved boarding, two layers of waterproof insulating paper, and $\frac{3}{4}$ in. tongued and grooved match-boarding. Paper to be laid one-half lap and cemented at all joints.

Brick wall 2 in. air space, 2 in. thicknesses of tongued and grooved boards with three layers of paper between, 2 in. air space, 2 in. thicknesses of tongued and grooved boards with three layers of paper between, 2 in. air space and 2 in. thicknesses of tongued and grooved boards with

three layers of paper between.

Brick wall well coated with pitch, 2 in. air space, 2 in. thicknesses of tongued and grooved boards with three layers of paper between, 2 in. space filled with slag-wool or cork, 2 in. thicknesses of tongued and grooved boards, with three layers of paper between, 2 in. space filled with slag-wool or cork, 2 in. thicknesses of tongued and grooved boards with three layers of paper between. Shelving should be fixed horizontally in the spaces packed with slag-wool or cork at about 16 in. apart.

Brick wall, I in. air space, $\frac{3}{4}$ in. match-boarding, 9 in. slag-wool or silicate cotton, layer of insulating paper, and

§ in. match-boarding.

Brick wall, I in air space, 6 in slag-wool or silicate cotton, I in silicate of cotton slab, layer of insulating paper, $\frac{1}{2}$ in air space, and $\frac{3}{4}$ in match-boarding.

Brick wall, r in air space, r in silicate of cotton slab, 4 in silicate of cotton, r in silicate of cotton slab, $\frac{1}{2}$ in

air space, and 3 in match-boarding.

Brick wall well coated with pitch, 2 in. air space, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 4 in. slag-wool or silicate cotton, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of

paper, 7/8 in. tongued and grooved boarding, 2 in. air space, 7 in. tongued and grooved boarding, two layers of paper,

and $\frac{7}{8}$ in. tongued and grooved boarding.

Brick wall, 2 in. air space, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. air space, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, and 7 in, tongued and grooved boarding.

Brick wall, 2 in. air space, 7 in. tongued and grooved boarding, one layer of paper, 4 in. slag-wool or silicate cotton, $\frac{7}{8}$ in. tongued and grooved boarding, one layer of paper, 4 in. air space, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, and $\frac{7}{8}$ in. tongued and grooved

boarding.

Brick wall, layer of pitch, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. air space, $\frac{7}{8}$ in. tongued and grooved boarding, one layer of paper, 3 in. cork dust, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, and 3 in. tongued

and grooved boarding.

Brick wall, $2\frac{1}{2}$ in. air space ventilated by air-bricks every 5 feet in all directions, 1 in. tongued and grooved boarding, layer of insulating paper, 1 in. tongued and grooved boarding, 12 in. charcoal supported by horizontal shelving 28 in. centres apart, 1 in. tongued and grooved boarding, two thicknesses of brown paper, and 1 in. tongued and grooved boarding.

Wall of cold storage room when made of wood: 2 in. thicknesses of tongued and grooved boarding with three layers of paper between, 2 in. air space, 2 in. thicknesses of tongued and grooved boarding with three layers of paper between, 2 in. air space, 2 in. thicknesses of tongued and grooved boarding with three layers of paper between, 2 in. air space, 2 in. thicknesses of tongued and grooved boarding with three layers of paper between, 8 in. slag-wool or silicate cotton, and i in tongued and grooved boarding.

2 in. boards, $5\frac{1}{2}$ in. by 3 in. uprights, spaces between filled with carefully dried wood charcoal, $1\frac{1}{4}$ in. boarding,

layer of insulating paper, and 11 in. boarding.

Outside siding, two layers of insulating paper, 1 in. tongued and grooved boarding, 2 in. by 6 in. studdings, 16 in. apart from centres, 1 in. tongued and grooved boarding.

two layers of insulating paper, 1 in. tongued and grooved boarding, 2 in. by 4 in. studding 16 in. apart from centres, spaces filled in with silicate cotton, 1 in. tongued and grooved boarding, two layers of insulating paper, 2 in. by 2 in. fillets or strips 16 in. apart from centres, 1 in. tongued and grooved boarding, two layers of insulating paper, and 1 in. tongued and grooved boarding.

DIVISIONAL PARTITIONS FOR COLD STORES.

Tongued and grooved match-boarding, wire netting, 6 in. silicate of cotton or slag-wool, wire netting, tongued and grooved match-boarding. The object of the netting is to render the partition fire-proof by supporting the silicate of cotton after the match-boarding might have burnt away.

 $\frac{3}{4}$ in. match-boarding, $\frac{1}{2}$ in. air space, I in. silicate cotton slab, 4 in. of silicate of cotton or slag-wool, I in. silicate of cotton slab, $\frac{1}{2}$ in. air space, and I in. silicate of cotton

slab.

2 in. tongued and grooved boarding, with three layers of paper between, 2 in. silicate of cotton or cork, 2 in. tongued and grooved boarding with three layers of paper between, 2 in. silicate of cotton or cork, 2 in. tongued and grooved boarding with three layers of paper between.

 $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 4 in. silicate cotton or slag-wool, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. air space, $\frac{7}{8}$ in, tongued and grooved boarding, two layers of

paper, and 7 in. tongued and grooved boarding.

 $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 6 in. silicate of cotton or slag-wool, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. air space, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, and $\frac{7}{8}$ in. tongued and grooved boarding.

 $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. silicate cotton or slag-wool, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. air space, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of

paper, and 7 in. tongued and grooved boarding.

 $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. air space, $\frac{7}{8}$ in.

tongued and grooved boarding, two layers of paper, and

 $\frac{7}{8}$ in. tongued and grooved boarding.

 $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 8 in. silicate cotton or slag-wool, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, and $\frac{7}{8}$ in. tongued and grooved boarding.

 $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 4 in. silicate cotton or slag-wool, $\frac{7}{8}$ in. tongued and grooved boarding, two layers

of paper, and 7 in. tongued and grooved boarding.

 $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. hair felt, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. silicate cotton or slagwool, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, and $\frac{7}{8}$ in. tongued and grooved boarding.

FLOORING FOR COLD STORES.

2 in. flooring, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. air space between fillets or scantlings, $\frac{7}{8}$ in. tongued and grooved boarding, 12 in. joists, spaces between packed with silicate cotton or slag-wool, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. air space between fillets and scantlings, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, and $\frac{7}{8}$ in. tongued and grooved boarding.

2 in. cement, 3 in. concrete, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, 2 in. flooring, 4 in. silicate cotton between fillets or scantlings, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, and 2 in. flooring

boards on fillets or scantlings set in concrete.

2 in. asphalte, $\frac{7}{8}$ in. tongued and grooved boarding, two layers of paper, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. air space between scantlings, $\frac{7}{8}$ in. tongued and grooved boarding, 3 in. silicate cotton or slag-wool between fillets or scantlings, $\frac{7}{8}$ in. tongued and grooved boarding, 2 in. air space between fillets or scantlings, concrete.

1 in. asphalte, 2 in. concrete, 1 in. pitch, 2 in. concrete,

brick arches.

11/4 in. tongued and grooved flooring, layer of insulating

paper, 2 in. by 9 in. joists, 12 in. centres apart, spaces filled with silicate cotton or slag-wool, wire netting, layer of insulating paper, $\frac{3}{4}$ in. match-boarding on 2 in. by 2 in. fillets or scantlings air spaces between, existing wooden or concrete flooring. The wire netting secured to the under side of the joists serves to retain the silicate cotton in case of fire.

I in. tongued and grooved boarding, three layers of insulating paper, I in. tongued and grooved boarding, 2 in. by 9 in. joists, spaces between filled in with silicate cotton or cork, I in. tongued and grooved boarding, three layers of insulating paper, and I in. tongued and grooved

boarding.

 $1\frac{1}{4}$ in. tongued and grooved flooring, layer of insulating paper, 2 in. by 9 in. joists, 12 in. centres apart, spaces between filled in with silicate cotton or slag-wool, 1 in. silicate cotton slab on $\frac{1}{2}$ in. by 2 in. fillets air spaces between, and $\frac{3}{4}$ in. match-boarding. The 1 in. silicate of cotton slab is nailed on the under side of joists and is claimed to render the floor fire-proof, and to prevent radiation through the joists.

2 in. matched flooring, two layers of insulating paper, 1 in. matched sheathing, 4 in. by 4 in. sleepers 16 in. apart from centres, spaces between filled in with silicate cotton, double 1 in. matched sheathing with twelve layers of paper between, and 4 in. by 4 in. sleepers 16 in. apart

from centres imbedded in 12 in. of dry underfilling.

Ground, concrete, layer of asphalte, r in. tongued and grooved match-boarding well tarred, two layers of stout brown paper, r in. tongued and grooved match-boarding, floor joists 3 in. by 11 in. spaced 21 in. apart, binder joists 11 in. by 4 in., bearing edges of floor joists protected by strips of hair felt $\frac{1}{4}$ in. thick and spaces between joists filled in with flake charcoal, and $r\frac{1}{4}$ in. tongued and grooved flooring boards.

As a further example of methods that have been actually successfully employed for insulation, it will be interesting to know that the cold storage chambers built at the St. Katherine Dock, London, were constructed as follows:—

On the concrete floor of the vault, as it stood originally, a covering of rough boards r_{\perp}^{1} in. in thickness were laid

longitudinally. On this layer of boards were then placed transversely, bearers formed of joists 4½ in. in depth by 3 in. in width, and spaced 21 in. apart. These bearers supported the floor of the storage chamber, which consisted of 2½ in. battens tongued and grooved. The 4½ in. wide space or clearance between this floor and the layer or covering of rough boards upon the lower concrete floor was filled with well-dried wood charcoal.

FLOORING FOR ICE HOUSES.

Floor to incline 3 in. towards central drain, and cross channelled fillets or scantlings on 11 in. flooring, 2 in.

cement, 6 in. concrete, ground.

I in. tongued and grooved match-boarding, three layers of paper, I in. tongued and grooved match-boarding (to incline 3 in. towards central drain) on fillets or scantlings, air spaces between, I in. tongued and grooved match-boarding, three layers of paper, I in. tongued and grooved match-boarding, 2 in. by 9 in. joists spaces between filled with 4 in. silicate of cotton or slag-wool kept in position by $\frac{3}{4}$ in. boards secured by cleats to joists.

CEILINGS FOR COLD STORES AND ICE HOUSES.

I in. tongued and grooved match-boarding, three layers of insulating paper, I in. tongued and grooved match-boarding, 2 in. air spaces between strips or fillets, I in. tongued and grooved boarding, three layers of insulating paper, I in. tongued and grooved boarding, joists spaces between filled with silicate cotton or cork, I in. tongued and grooved match-boarding, three layers of insulating paper, and I in. tongued and grooved match-boarding.

Insulated flooring, joists, $\frac{7}{8}$ in. tongued and grooved match-boarding, two layers of insulating paper, $\frac{7}{8}$ in. tongued and grooved match-boarding, 2 in. spaces between strips or fillets filled in with silicate cotton or cork, $\frac{7}{8}$ in. tongued and grooved match-boarding, three layers of insulating paper, and $\frac{7}{8}$ in. tongued and grooved match-

boarding.

I in tongued and grooved boarding, two thicknesses of

brown paper, I in. tongued and grooved boarding, joists with spaces between packed with silicate cotton, I in. tongued and grooved boarding, Willesden paper, and I in. tongued and grooved boarding.

Concrete floor, 3 in. book tiles, 6 in. dry underfilling, double space hollow tile arches and layer of cement plaster.

Double 1 in. floor with two layers of insulating paper between, 2 in. by 2 in. strips or fillets 16 in. apart from centres, spaces filled in with silicate cotton, two layers of insulating paper, 1 in. tongued and grooved match-boarding, 2 in. by 2 in. strips 16 in. apart, spaces filled in with silicate cotton, two layers of insulating paper, 1 in. tongued and grooved match-boarding, joists and double 1 in. flooring with two layers of insulating paper between.

DOOR INSULATION.

I in. tongued and grooved match-boarding, three layers of insulating paper, I in. tongued and grooved match-boarding, 2 in. by I in. fillets or strips, with spaces between filled in with silicate cotton or cork, I in. tongued and grooved match-boarding, three layers of insulating paper, I in. tongued and grooved match-boarding, 2 in. by I in. fillets or strips, spaces between filled in with silicate cotton or cork, I in. tongued and grooved match-boarding, three layers of insulating paper, and I in. tongued and grooved match-boarding.

1 in. tongued and grooved match-boarding, two layers of insulating paper, 1 in. tongued and grooved match-boarding, 12 in. space filled in with silicate cotton, 1 in. tongued and grooved match-boarding, two layers of insulating paper, and

I in. tongued and grooved match-boarding.

WINDOW INSULATION.

Windows are better dispensed with in cold stores and artificial light resorted to; where present, three sashes spaced a few inches apart and glazed at both sides should be used.

TANK INSULATION.

Tank sides: 4 in. air space between studding, 1 in. tongued and grooved match-boarding, three layers of insulating paper, 1 in tongued and grooved match-boarding, 4 in. space filled with cork, 1 in. tongued and grooved match-boarding, three layers of insulating paper, 1 in. tongued and grooved match-boarding, 2 in. air space, 1 in. tongued and grooved match-boarding, three layers of insulating paper, and I in tongued and grooved matchboarding. Bottom: 1 in. space between strips, fillets or studding, well tarred before tank is placed in position, r in. tongued and grooved match-boarding, three layers of insulating paper, I in. tongued and grooved match-boarding, I in. air space between strips, fillets or studding. I in. tongued and grooved match-boarding, three layers of insulating paper, 1 in. tongued and grooved match-boarding, and 2 in. by 9 in. joists on concrete or ground spaces between filled with cinders.

Tank: 2 in. air space between fillets, $\frac{7}{8}$ in. tongued and grooved match-boarding, two layers of insulating paper, $\frac{7}{8}$ in. tongued and grooved match-boarding, 4 in. silicate cotton or slag-wool, $\frac{7}{8}$ in. tongued and grooved match-boarding, two layers of insulating paper, and $\frac{7}{8}$ in. tongued

and grooved match-boarding.

Tank: 2 in. air space between studding, layer of insulating paper, 2 in. flooring, two layers of insulating paper, $\frac{7}{8}$ in. tongued and grooved boarding, joists, spaces between filled with charcoal for three-quarters depth, $\frac{7}{8}$ in. tongued and grooved match-boarding, two layers of insulating paper, $\frac{7}{8}$ in. tongued and grooved match-boarding, ground or concrete.

SECTION V.

TESTING AND MANAGEMENT OF REFRI-GERATING MACHINERY.

TESTING.

THE testing of a refrigerating plant is carried out for the purpose of ascertaining what it is capable of performing under comparable normal conditions, and as to the amount of refrigeration produced in relation with the expenditure of work, and the coal consumption.

To determine the efficiency of an installation on the compression system, the following instruments and fittings are required, viz.: An indicator, so that diagrams can be taken from the compressor; stroke counters, to enable the number of strokes made by the steam-engine and brine pumps to be ascertained; and mercury wells to admit of the temperature being obtained at various points throughout the system.

In making a test it is desirable that it should last at the very least for fully 12 hours, and it is better to carry it on for 24 hours. The number of readings which it is desirable should be taken from the various instruments will vary in accordance with whether or not the work is steady or otherwise, and the person carrying out the test will have, of course, to use his own judgment on this head. Where artificial ice is made, for example, twice an hour will be sufficient, whilst on the other hand, four or more readings per hour should be taken in cases where the variation in the temperature of the materials to be cooled is wide. Indicator diagrams should be taken from both the steam-engine cylinder and the compressor cylinder every two hours.

A mercury well, for an horizontal pipe, when the latter is of sufficient dimensions, consists usually in a short piece of tubing closed at its lower end, and fitted into the pipe by means of a suitable bushing. It is filled about three parts full of mercury, and the thermometer, which should have an elongated cyclindrical bulb, is held in position therein by means of a perforated cork. For vertical pipes, or pipes of very small dimensions, where this arrangement would be impracticable, the well is generally formed by means of a wooden or other block, one side of which is shaped to the outline of the pipe to which it is to be applied, and has a suitable recess formed therein. This block is firmly secured against the pipe by metal strips in such a manner that a portion of the wall of the well will be formed by the pipe, the latter being scraped perfectly clean at that part. The joint between the block and the pipe must be made perfectly tight, which can easily be effected by means of a little white-lead paint, there being no pressure, and the whole should be surrounded by a thick layer of non-conducting composition, through which the stem of the thermometer is permitted to project.

The points in the system where it is desirable to locate the mercury wells are: The suction pipe just at its connection with the compressor; the discharge pipe, as close as possible to its connection with the compressor; the ammonia discharge pipe from the condenser, as near the latter as practicable. Where a brine circulation is employed: The pipe or manifold supplying the various coils or sets of pipes in the refrigerator; the discharge pipe of the refrigerator; the brine discharge pipe, at the point where it connects to the refrigerator; and the brine return pipe in proximity to where it connects with the refrigerator.

INTERPRETATION OF COMPRESSOR DIAGRAM.

The interpretation of a compressor diagram with respect to the working, valves, defects, etc., of the latter are given as follows by Hans Lorenz, in "Neuere Kuehlmaschinen," Muenchen and Leipzig, 1899.

Assuming all the parts of the machine to be in good order, then the diagram will have the general appearance

shown in Fig. 23. The suction line S is only slightly below the suction pressure line V, and the pressure line D is only slightly above the condenser pressure K. Small projections at the pressure and suction line indicate the work required to open the compressor valves, and the effect of clearance is shown by the curve R, which latter cuts the back pressure line after the piston has commenced to perform its return or back stroke, and consequently reduces the suction volume to that amount. It can also be seen from this diagram that the vapours are taken in by the compressor, not at the back pressure, but at what may be called the suction pressure, which is somewhat lower. This is the reason that the compression curve C does not intersect the back pressure line until after the piston has changed its direction of movement. The theoretical volume of the compressor, as indicated by the line V, is consequently reduced in practical working for vapours possessing a certain tension.

In Fig. 24 is shown a diagram taken from a compressor having an excessive amount of clearance. In this case, it will be seen, the back expansion line R passes through a flat course, and thereby reduces the useful volume of the

compressor.

Fig. 25 is a diagram which indicates the binding of the pressure valve, which may be due to an inclined position of the guide rod of the valve. This deficiency also frequently causes a delay in the opening of the pressure valves, a state of things indicated by a too great projection in the pressure line. As soon as the valve is once opened the pressure line pursues its normal course until the piston commences its return stroke, when the defect is again manifested in the back pressure line, as mentioned.

Fig. 26 shows a diagram indicating too great a resistance in the pressure and suction pipes respectively, when the valves are over-weighted. In this case the pressure and suction line are at a comparatively great distance from the condenser pressure line and the back pressure line. The remedy for this is to replace the valve springs by weaker ones; and should there be then no marked effect, then the pipe-lines and shutting-off valves should be inspected, and,

if found necessary, cleaned.

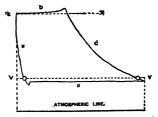


Fig. 23.—Diagram from Compressor with all parts in good order.

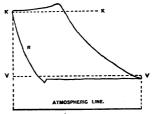
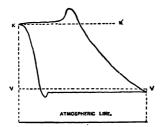


Fig. 24.—Diagram from Compressor with excessive amount of clearance.



Ftg. 25.-Diagram from Compressor indicating the binding of the Pressure Valve.

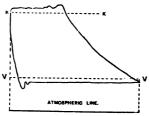


Fig. 26.—Diagram from Compressor indicating too great a resistance in the Pressure and Suction Valves.

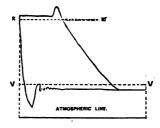


Fig. 27.—Diagram from Compressor indicating the binding of the Suction Valve.

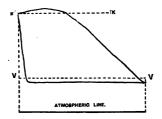


Fig. 28.—Diagram from Compressor indicating leaking of Compressor Valves.

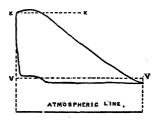


FIG. 29.-Diagram from Compressor indicating Defective Packing of Piston.

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Fig. 27 indicates the binding of the suction valve by which a considerable decline is caused in the pressure at the beginning of the suction, which is consequently shown by an increased projection in the commencement of the suction line. At the beginning of compression this defect makes itself felt by causing a delay in the latter, which effect is also shown on this diagram.

Fig. 28 shows leaking of the compressor valves. In this diagram the projections in the compression and suction line do not appear, but the compression line gradually merges into the pressure line, and the back expansion line passes gradually into the suction line. If the leak in the pressure valve is the predominant one, then the compression curve will be almost in a straight line and very steep; if, on the contrary, the leak in the suction valve is the predominant one, then the compression line will run a rather flat course.

Fig. 29 indicates that the piston is not well packed, and, being leaky, the vapours are permitted to pass from one side of the piston to the other, thus causing a very gradual compression, and as a result a compression line having a flat course. On the other hand, a longer time will be taken before the suction line reaches its normal level on the return or backward stroke, inasmuch as the suction valve is prevented from opening until such time as the velocity of the piston becomes such that the amount of vapours leaking past the piston is insufficient in amount to fill the suction space. The pressure then gradually diminishes and the suction valve then begins to act, as is shown on the diagram.

It is to be understood that several of the defects above mentioned may exist at the same time.

Management of Ammonia Compression Machines.

Every particular type of machine working on this principle has, as a rule, certain distinctive or characteristic features, and will, of course, so far at least as these are concerned, require special care and adjustment, and it would consequently be totally impossible to lay down an arbitrary set of rules for working that would be suitable to

all; nor is this necessary or required, as full particulars relating to the manipulation of each particular machine are invariably supplied by the makers. The following points, however, are more or less applicable to all machines working on the ammonia compression principle, and should therefore be familiar to those in charge of the same.

Before charging an empty machine with anhydrous ammonia, all air must first be carefully expelled. This is effected by working the pumps so as to discharge the air through special valves which are usually provided on the

pump dome for that purpose.

The entire system should have been previously to this thoroughly tested by working the compressor, and permitting air to enter at the suction through the special valves provided for that purpose, and it should be perfectly tight at 300 lbs. air pressure on the square inch, and should be able to hold that pressure without loss. Whilst testing the system under air pressure, it should be also carefully blown through and thoroughly cleansed from all dirt, every trace of moisture being also removed.

It is totally impossible to eject all air from the plant by means of the compressor, therefore it is advisable to insert the requisite charge of ammonia gradually and not all at once, the best practice being to put in from 60 to 70 per cent, of the full charge at first, and cautiously permit the air still remaining to escape through the purging-cocks with as little loss of gas as possible, subsequently inserting an additional quantity of ammonia once or twice a day. until all the air has been got rid of by displacement, and

the complete charge has been introduced.

To charge the machine, the dryer or dehydrator of the apparatus for manufacturing or generating anhydrous ammonia, or where no such apparatus is included in the installation, the drum or iron or steel flask of anhydrous ammonia should be connected, through a suitable pipe, to the charging valve; the expansion valve must be then closed, and the valve communicating with the dryer or dehydrator, or that in the flask or bottle, opened. The machine should be run at a slow speed when sucking ammonia from the drier, or whilst the flask is being emptied, with the discharge and suction valves full open.

In the latter case, when one of the said flasks or bottles has been completely emptied, it must be removed, the charging-valve having been first closed, and another placed in position, until the machine is sufficiently charged to work, when the charging-valve should be finally closed, and the main expansion valve opened and regulated. A glass gauge upon the liquid receiver will show when the latter is partially filled, and the pressure gauges, and the gradual cooling of the brine in the refrigerator (in the case of a brine circulation or ice-making apparatus), and the expansion pipe leading to the refrigerator coils becoming covered with frost, indicate when a sufficient amount to start working has been inserted.

It is sometimes advisable to slightly warm the vessels or bottles containing the anhydrous ammonia by means of a gas jet, or in some other convenient manner, whilst transferring their contents to the machine, as otherwise, if frost forms on the exterior of the said bottles, they will not be completely discharged, and loss of ammonia will ensue.

The flasks, bottles, or other receptacles containing the anhydrous ammonia should be always kept in a tolerably cool and a perfectly safe situation, and they should moreover be moved and handled with the utmost caution and care.

In the event of an accident occurring, and any considerable quantity of the ammonia becoming spilt, it is well to remember that it is so extremely soluble in water that one part of the latter at a temperature of 60° Fahr. will absorb some 800 parts of the ammonia gas, therefore water should be employed to kill or neutralise it, and any person attempting to penetrate an atmosphere saturated with this gas should not fail to place a cloth well saturated with water over his nose and mouth.

The machine having been started, and the regulating valve opened, it is essential to note carefully the temperature of the delivery pipe on the compressor, and if it shows a tendency to heat, then the said regulating valve must be opened wider; whilst, on the contrary, should it become cold, this valve must be slightly closed, the regulation or adjustment thereof being continued until the normal temperature of the delivery pipe is the same as that of the cooling water leaving the condenser. When the charge of ammonia in the machine is insufficient, the delivery pipe will become heated, and that even when the regulating

valve is wide open.

There are many additional signs of the healthy working of the apparatus other than the fact that it is satisfactorily performing its proper refrigerating duty, which soon become easily recognisable to those in charge; for example, every stroke of the piston will be clearly marked by a corresponding vibration of the pointers or indexes of the pressure and vacuum gauges. The frost visible on the exterior of the ammonia pipes leading to and from the refrigerator will be about the same. The liquid ammonia can be distinctly heard passing in a continuous and uninterrupted stream through the regulating valve. The temperature of the condenser will be about 15° higher than that of the cooling water running from the overflow. And finally, the temperature of the refrigerator will be about 15° lower than the actual temperature of the brine or the water being cooled.

Air will find its way into the system through leaky stuffing-boxes, improper regulation of the expansion valve, etc. Its presence in any considerable volume is shown by a kind of whistling noise, the liquid ammonia passing through the expansion valve in an intermittent manner, a rise of pressure in the condenser, and also loss of efficiency thereof, and other obvious signs. In this case the above air must be got rid of through the purging-cocks in a similar manner to that which remains in the system when first charging the machine.

The presence of any considerable amount of oil or water in the system, which may result from careless distillation, will cause a reduction in efficiency, and will be evidenced

by shocks within the compressor cylinder.

The temperature can be regulated either by running the machine at a higher speed or by increasing the back pressure, or by a combination of both. The back pressure can be regulated by means of an expansion valve or valves fitted between the receiver and the refrigerator evaporating coils or pipes in the main liquid pipe.

LEAKS IN AMMONIA APPARATUS.

Leaks are readily detected by the smell of the escaping ammonia gas when the machine is being filled; at a later stage, when working, their detection is not so easy. During the operation of the machine, when the liquor or brine in the tanks commences to smell of ammonia, it indicates a considerable leakage. It is recommended to test the liquor or brine periodically with Nessler's solution or otherwise.

Nessler's reagent, which is the best to use for the discovery of traces of ammonia in water or brine, consists of 17 grms. of mercuric chloride dissolved in about 300 cc. of distilled water, to which are added 35 grms. potassium iodide dissolved in 100 cc. of water, and constantly stirred until a slight permanent red precipitate is produced. To the solution thus formed are added 120 grms. of potassium hydrate dissolved in about 200 cc. of water, allowed to cool before mixing; the amount is then made up to 1 ltr., and mercuric chloride added until a permanent precipitate again forms. After standing for a sufficient time, the clear solution can be placed in glass-stoppered blue bottles and kept in a dark place.

If a few drops of this reagent be added to a sample of the suspected brine or water in a test-tube, or other small vessel, and the slightest trace of ammonia is present, a yellow colouration of the liquid will take place; a large

quantity of ammonia will produce a dark-brown.

When the leaks are comparatively insignificant they can be closed in the usual way, by solder, using as a flux muriatic or hydrochloric acid killed with zinc. In some instances electric welding may be resorted to with advantage, or the leak may be closed by means of a composition of litharge and glycerine mixed into a stiff paste, bound with sheet-rubber, and covered with sheet-iron clamped firmly in position. When, however, the leak is at all serious, it is usually the better plan to at once put in a new coil, or a new length of pipe.

LEAKS IN CARBONIC ACID MACHINES.

To detect these, smear the joints with a solution of soap and water, and any leakage of gas will be evidenced by the formation of bubbles. Carbon dioxide or carbonic acid being a completely inodorous gas, precautions are required

to prevent the unnoticed occurrence of leakage.

Before closing this chapter, a few words upon the excess condensing pressure invariably found in ammonia compression machines will not be out of place. This excess of the actual working condensing pressure over the theoretical is caused by the ammonia gas being imprisoned in the comparatively confined space afforded by the coils or pipes in the refrigerator, and the excess pressure is more marked in a horizontal compressor running at a high speed of, say, 140 revolutions per minute, than it is in vertical ones having only a low speed of from 35 to 60 revolutions per minute; it varies, moreover, in almost every make of compressor. At a low suction pressure of about 15 lbs. it should not be more than 10 lbs., but with a suction pressure of, say, 27 or 28 lbs. it may rise to 50 lbs., or even more.

The condensing pressure affords a means of ascertaining whether or not the apparatus contains the proper full charge of ammonia, or if the losses sustained by leakage are sufficient to render it necessary to insert an additional supply. For this reason it is advisable for the person in charge to keep a record in a proper book, suitably ruled for the purpose, of the temperature of the condensed ammonia when leaving the condenser, and also of the condensing and suction pressures, at regular intervals of, say, three hours. This will enable him to follow the state of the ammonia charge; for example, if the condensing pressure is found to be gradually falling during a three months' period, as compared with the average condensing pressure of the previous three months, whilst at the same time the condensing temperature and the suction pressure remain constant, it will be evident that the charge of ammonia has become reduced by leakage to a sufficient extent to require replenishing. This reduction in the condensing pressure is caused by the diminution in the charge of ammonia giving larger condenser space, the gas having thus a much more extended worm, coil, or tube space wherein to condense and liquefy, and hence the decrease. As a general rule, it may be taken that, whenever the condensing pressure is found to have fallen about

8 lbs., enough ammonia to restore the original condensing pressure should be inserted into the machine.

LUBRICATION OF REFRIGERATING MACHINERY.

This important point is apt to be as much neglected by users of refrigerating machinery as it is by those of other types of machinery. It would be well for these gentlemen to at once dismiss from their minds the idea that low-priced inferior quality oils are really the cheapest, and understand that, on the contrary, not only are high-grade oils necessary to ensure the highest efficiency of the machinery, but that they are also the least expensive in the long run.

In refrigerating machinery the use of three different kinds of oil is demanded, viz. steam cylinder oil; oil for general

use; and compressor pump oil:-

Oil for the steam cylinder. Good cylinder oil is entirely free from grit, does not gum up the valves and cylinder, and does not evaporate rapidly on exposure to the heat of the steam. The quality of a cylinder oil is demonstrated on removal of the cylinder head. If the oil is of good quality, the wearing surfaces should appear well coated with lubricant, which will not show a gummy deposit, or blacken on the application of clean waste.

Oil for general use on all the bearings and wearing surfaces of the machine proper: This may be any oil that will not gum, is not too limpid, possesses a good body, is free from grit and acids, is of good wearing quality, and flows freely from the oil-cups at a fine adjustment without a tendency to clog. For the larger bearings it is well to use a heavier grade of oil.

Oil for use in compressor pumps: This should be what is known as zero oil, or cold test oil, that is to say, it should be capable of withstanding a very low temperature without freezing, and it should be of the best quality. American makers recommend the use of the best paraffin oil, and clear West Virginia crude oil.

SUGGESTED FORM FOR ENGINEER'S DAILY REPORT.

Gallons to Remarks. Brine or salt water column. Wea-Conditions. Temperature. on leaving steam condenser. Final temperature of water Date tering steam condenser. l'emperature of water on en monia condenser. emis or ornigheracine to am-Refrigeration daily in tons. No. 12 Room. No. 11 Room. No. 10 Room. No. 9 Room. Coal receipts. Refrigerator Temperature. Engineer's Daily Report. No.8 Room. Fuel. No. 7 Koom. No. 6 Room. Up to present To-day. Total No. 5 Room. No. 4 Koom. Boilers. Hours run. No. 3 Room. No. 2 Room. No. 1 Room. Vacuum. To-day. Total, Boilr. : : Steam. Brine or salt water column. Engine Room. Revolutions. No. 4 Engine. Department No ... No. 3 Engine. Engines. Hours run. No. 2 Engine. present date. No. 1 Engine. Up to Suction pressure. Engine. Direct pressure. No. 1 Hour.

Engineer's Signalure...

LIGHTING COLD STORES.

It is desirable that daylight should not be allowed to enter a cold store, and therefore artificial light is usually resorted to, electric light being invariably employed, owing to there

being practically an absence of heat therefrom.

Incandescent lamps should be always used inside the cold stores, but arc lamps may be placed, if desired, in the engine-room, and employed for the external lighting of the premises. Lower voltage lamps are the most durable, and serve the purpose quite as well as those of a higher voltage.

The mains should be kept as far as practicable in the corridors, and tinned cables of high conductivity and with

rubber insulation should preferably be employed.

Iron piping, steel conduits, or wood casing, may be used for carrying the main cables, the latter being the cheapest both in cost of material and in fixing, and also lending itself more readily to any subsequent alterations that may become necessary. Steel conduits, however, possess several important advantages. The steel-armoured insulating conduit material now much used is installed in a similar manner to ordinary gas-pipe construction, the principal difference in electric piping being that specially insulated boxes, bends, elbows, etc., are substituted for the ordinary tees or angles of a gas-pipe system. The use of the conduit system ensures a mechanically and electrically protective duct for the installation of the electric conductors.

When wood casing is used, the interior should be painted with asbestos paint, and the cover fixed with brass screws

on each edge, not in the central fillet.

Iron piping has an internal lining of suitable insulating material, and is, as a rule, coated with a bituminous compound of some description intended to act as a preservative.

There are two systems of carrying out wiring now in use, viz. the tree system, and the distributing-board system.

In the first of these, or the tree system, two main cables are carried through the building, the branch circuits being all taken from these cables or mains. In the second, or distributing-board system, a main switchboard is placed close to the dynamo, from which main switchboard cables are carried to supplementary distributing boards located at convenient points, from which the lamps are wired.

An obvious advantage of this latter plan is that all the joints are readily get-at-able, being at the distributing boards and fittings. The insulation of the cable is left completely intact.

In fixing wood casing all joints should be united, and no sharp edges or corners left for the cable to pass over. The casing is ordinarily secured by screws to the walls, floors, and ceilings, and either on the surface, partially sunk, or sunk flush therewith. In very damp situations, however, the casing should be supported, so as to be clear of the surfaces, by means of small porcelain insulators.

The circuits may be arranged either on the series system or on the parallel arrangement, the latter being the most common, and the former being, as a rule, only employed where a number of arc lamps are used. The series circuit and parallel circuit are shown in the diagrams (Figs. 30 and 31), the dynamos, main cables, lamps, and switches being indicated thereon.

In the series circuit the current is maintained constant in value, the difference in pressure varying with the work on the circuit.

In the parallel circuit all the lamps are connected as separate paths between the two main leads, each path being quite independent of the other paths. The difference of electrical pressure is maintained constant, the current varying with the work that is on the circuit. The switching off of a lamp causes a break in the wires connecting the lamp to the circuit.

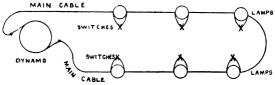


Fig. 30.—Diagram illustrating Arrangement of Electric Lighting on the Series Circuit System.

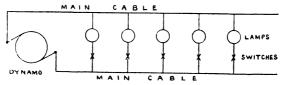


Fig. 31.—Diagram illustrating Arrangement of Electric Lighting on the Parallel Circuit System.

SECTION VI.

GENERAL TABLES AND MEMORANDA.

EXPERIMENTS IN WORT COOLING.

The following tabulated experiments of the performance of a tubular refrigerator for wort cooling are gleaned from *Engineering*. The water and wort are moved in opposite directions, the former through thin metallic tubes, which are surrounded by the wort to be cooled:—

bo		W	ORT.				WAT	ER.	
Area of Cooling Surface of Refrigerator.	Speoific Gravity.	Quantity passed through per Hour.	Initial Temperature.	Final Temperature.	Cooled down.	Quantity passed through per Hour.	Initial Temperature.	Final Temperature.	Warmed up.
Square Feet. No. 1. 881 No. 2. 514 No. 3. 514 No. 4. 514 No. 5. 514	 1·104 1·188 1·035 1·018	Bbls. 33.9 36.1 36.6 47.3 48.0	Fahr. 212° 155 191 193 178	Fahr. 72° 59 59 59 59	Fahr. 140° 96 132 134 119	Bbls. 61·1 75·5 99·5 90·7 102·0	Fahr. 65° 54 54 54 54	Fahr. 169° 100 100 100	Fahr 1046 46 46 46 46

NOTE 1.—A barrel contains thirty-six gallons, or 360 lbs. of water. NOTE 2.—The temperature of the air in Nos. 2 and 4 was 44° F., and in Nos. 3 and 5, 40° F.

TABLE SHOWING THE TENSION OF AQUEOUS VAPOUR IN MILLIMETRES OF MERCURY, FROM -30° C. TO 230° C. -(Siebert.)

Temp.	Tension.	Temp.	Tension.	Temp.	Tension.	Temp.	Tension.
-30°	0.39	210	18.2	94.0°	610.4	104°	876
-25	0.91	22	19.7	94.5	622.2	105	907
-10	0.0	23	20'9	95.0	633.8	107	972
-15	1'4	24	22.7	95.2	645.7	110	1,077
-10	2.1	25	23.6	96.0	657.5	115	1,273
-5	3.1	26	25.0	96.2	669.7	120	1,491
-2	4.0	27	26.6	97.0	682.0	125	I,744
- I	4.3	28	28.1	97.5	694.6	130	2,030
0	4.6	29	29.8	98.0	707:3	135	2,354
I	4'95	30	31.6	98.5	721.2	140	2,717
2	5.3	35	41.9	99.0	732.2	145	3,125
3	5·7 6·1	40	55.0	99.1	735'9	150	3,581
3 4 5 6		45	71.2	99'2	738.5	155	4,088
5	6.2	50	92.0	99'3	741.5	160	4,551
	7.0	55	117.5	99'4	743.8	165	5,274
7 8	7.5	60	148.0	99.2	746.5	170	5,961
8	8.0	65	186.0	. 99.6	749°2	175	6,717
9	8.6	70	232.0	99'7	751.9	180	7,547
10	9.1	75	287.0	99.8	754.6	185	8,453
II	9.7	8o	354.0	99.9	757.3	190	9,443
12	10.4	85	432.0	100.0	760.0	195	10,520
13	II.I	90	525.4	100.1	762.7	200	11,689
14	11.9	90.2	535.2	100.5	765.5	205	12,956
15	12.7	91.0	545.8	100.4	772.0	210	14,325
16	13.2	91.2	556.2	100.6	776.2	215	15,801
17	14'4	92.0	566.3	101.0	787.0	220	17,390
18	15.3	92.2	577.8	102.0	816.0	225	19,097
19	16.3	93.0	588.4	103.0	845.0	230	20,926
20	17.4	93.2	599'5			į.	
		t!		!	1	1	

Degrees C..... 120 134 144 152 159 171 180 190 213 235 Atmospheres.. 2 3 4 5 6 8 10 15 20 25

TABLE OF PHYSICAL CONSTANT OF GASES.—(Peckham.)

			Critical Temp. Centigrade.	Critical Pressure Atmo- spheres.	Boiling- point at Ordinary Pressure.	Freezing- point Centigrade.	Freezing Pressure Mm.	Density of Gas.	Density of Liquid at Boiling- point.	Colour of Liquid.
Carbon Dioxide, CO		:	3101	0.11	-78.503	-79%	8/	22	0.8300	Colourless
Ethylene, C,H,		:	0.56	~~ •••••	-110	:	:	14	;	. :
Hydrogen, H ₂		:	{-234'5"} {(Theor.)}	0.08	~~	;	i		i	Colourless
Nitrogen, N2	:	:	-146	35.0	~	-203 to -214 Mean -280.	8	14	0.885	Colourless
Carbonic Oxide, CO .	:	:	-139.5	35.2		-207.0	100	14	:	Colourless
	:	:	0.121-	9.0		9.681-	:	6.61	apont 1.2	Colourless
:	:	:	-140.0	36.0		-207	:	:	0.633	Bluish
:	:	:	8.811-	20.8		:		91	1.124	Bluish
:	:	:	-03.2	71.3	_	- 167.0	138	15	:	Colourless
Marsh Gas, CH,	:	:	8.18	54.6		-185.8		œ	0.415	Colourless
:	:		:	:	Below - 2647	:	:	2.02	:	:
Fluorine	:	:	:	:	- 187	:	:	:	:	:
		-	_	_		_	_	_	_	

Andrews, Deschanel Nat. Phil., II., 352.

2 Villard & Jarry, Comptes Rendus, 1895, 120, 1413.

³ Regnault, Muspratt's Chemic, IV., 1626.
⁴ Thilorier, Muspratt's Chemic, IV., 1626.

Fownes, Elem. Chem., 12th ed., p. 534.

" Olzewski, Phil. Mag., 1885 (5), 40; 202.

7 Olzewski, Ann. Phys. Chem., 1896 (2), 59, 184. * Cleve, Comptes Rendus, 1895, 120, 1212.

" Dewar.

TABLE SHOWING PROPERTIES OF SATURATED STEAM .- Yaryan.

	te Pressure Vacuum.	Above A	Atmosphere.	Tempera-	Total Heat	Heat of Vaporiza-
lbs.per Square In.	Inches of Mercury.	lbs. per Square In.	Inches of Mercury.	ture. Deg. Fahr.	in British Units.	tion or Latent Heat.
1 2 3 4 5 6 7 8 9 10 11 12 13 14 7 15 16 17 18 20 21 22 23 24 25 6 27 28 29 30 31 32	2·0355 4·0710 6·1065 8·142 10·178 12·213 14·249 16·284 18·320 20·355 22·319 24·426 26·462 28·497 29·922 30·535 40·710 42·746 44·781 46·787 48·787 48·787 48·787 48·787 48·787 49·72 50·888 52·923 54·972 57·008 59·044 61·080 63·116 65·152	- 13·7 - 12·7 - 10·7 - 10·7 - 10·7 - 8·7 - 7·7 - 6·7 - 4·7 - 3·7 - 2·7 - 0·0 - 0·3 - 1·3 - 2·3 - 3·3 - 4·3 - 5·3 - 6·3 - 7·3 - 8·3 - 9·3 - 10·3 - 11·3 - 12·3 - 13·3 - 14·3 - 15·3 - 15·3 - 17·3	-27-886 -25-851 -23-815 -21-780 -19-744 -17-709 -15-673 -13-638 -11-602 -9-567 -7-531 -5-496 -1-425 -0-000 -1-425 -0-001 2-646 4-682 6-717 8-753 10-788 12-824 14-859 15-895 18-930 20-966 23-007 25-043 27-079 29-115 31-143 33-187	101·99 126·27 141·62 153·09 162·34 170·14 176·90 182·92 188·33 193·25 197·78 201·98 205·57 212·00 213·03 216·32 229·44 222·40 225·24 222·40 225·24 223·55 233·06 235·47 237·79 240·04 242·21 244·32 246·36 248·34 250·27 252·15 253·98	1113·1 1120·5 1125·1 1128·6 1131·5 1133·8 1135·9 1137·7 1139·9 1142·3 1143·6 1144·7 1145·8 1146·6 1144·9 1149·8 1150·7 1151·5 1152·3 1153·7 1154·4 1155·1 1155·8 1156·5 1157·7 1158·3 1158·8 1159·4	1043.0 1026.1 1015.3 1007.2 1000.8 995.2 986.2 986.2 986.2 987.2 987.3 967.5 965.8 962.8 962.8 962.8 962.8 962.8 963.6 954.6 958.5 954.6 954.6 954.6 954.7 947.6 944.6 944.6 944.7 946.3 948.7 946.3
33 34 35 36 37 38 39	67·188 69·224 71·260 73·296 75·331 77·367 79·403	18·3 19·3 20·3 21·3 22·3 23·3 24·3	37·239 39·295 41·321 43·367 45·319 47·397 50·463	255.76 257.50 259.19 260.85 262.47 264.06 265.61	1159.9 1160.4 1161.0 1162.0 1162.5 1163.0	935.0 933.7 932.6 931.5 930.3 929.2 928.2

TABLE SHOWING PROPERTIES OF SATURATED STEAM. - Yaryan. Continued.

	te Pressure Vacuum.	Above A	Atmosphere.	Tempera-	Total Heat	Heat of Vaporiza-
lbs. per Square In.	Inches of Mercury.	lbs. per Square In.	Inches of Mercury.	ture. Deg. Fahr.	in British Units.	tion or Latent Heat.
40	81.439	25.3	51.499	267.13	1163.4	927.0
41	83.475	26.3	53.234	268.62	1163.9	926.0
42	85.211	27.3	55.283	270.08	1164.3	925.0
43	87.547	28.3	57.619	271.21	1164.8	924.0
44	89.583	29.3	59.655	272.01	1165.5	923.0
45	01.010	30.3	61.601	274.29	1165.6	922.0
46	93.655	31.3	63.727	275.65	1166.0	921.0
47	92.691	32.3	65.763	276.99	1166.4	920.1
48	97.727	33.3	67.799	278.30	1166.8	919.5
49	99.763	34.3	69.835	279.58	1167.2	918.3
50	101.299	35.3	71.871	280.85	1167.6	917.4
55	111.08	40.3	82.050	286.89	1169.4	913.1
60	122.16	45.3	92.530	292.21	1171.2	909.3
65	132.34	50.3	102.410	297.77	1172.7	905.2
70	142.25	55.3	112.20	302.71	1174.3	902.1
75	152.70	60.3	122.77	307.38	1175.7	898∙8
75 80	162.88	65.3	132.95	311.80	1177.0	895.6
85	173.06	70.3	143.13	316.03	1178.3	892.5
9ŏ	185.24	75.3	153.31	320.04	1179.6	889.6
95	193.42	80.3	163.49	323.89	1180.7	886.7
100	203.06	85.3	173.67	327.58	1181.9	884.0
105	213.78	90.3	185.85	331.13	1182.9	881.3
110	223.96	95.3	194.03	334.26	1184.0	878.8
115	234.14	100.3	203.67	337.86	1185.0	876.3
I 2O	244.32	105.3	214.39	341.05	1186.0	874 o
125	254.20	110.3	224.57	344.13	1186.9	871.7
130	264.68	115.3	234.75	347.12	1187.8	869.4
135	274.86	120.3	244.93	350.03	1188.7	867.3
140	285.04	125.3	255.11	352.85	1189.5	865.1
145	295.22	130.3	265.29	355.25	1190.4	863.2
150	305.40	135.3	275.47	358.26	1191.5	861.2
160	325.76	145.3	295.83	363.40	1192.8	857.4
170	345.82	155.3	316.19	368.29	1194.3	853.8
180	366.48	165.3	336.22	372.97	1195.7	850.3
190	386.84	175.3	356.91	377.44	1197.1	847.0
200	407:20	185.3	377:27	381.73	1198.4	843.8

PROPERTIES OF SATURATED STEAM AT PRESSURE FROM ONE POUND TO 200 POUNDS ON THE SQUARE INCH.

("Compend. of Mechanical Refrigeration.")

Specific Gravity.	the atmosphere at 32° being 1.	0.037 0.167 0.318 0.463 0.604 0.742 0.877 1.012 1.142 1.422 1.529		
Weight	cubic foot in Decimals of a pound.	0.0029 0.0135 0.0257 0.0257 0.0373 0.0487 0.0598 0.0598 0.0598 0.025 0.1025 0.1123		
Volume, that of an	weight of Water at its greatest density being r.	20,890 4,627 4,627 1,569 1,280 1,042 881 764 608 506 506		
	at.	Dif. 2.82 1.50 1.50 0.7 0.6 0.7 0.6 0.7 0.6 0.7 0.7 0.6 0.7 0.7 0.7 0.7 0.7 0.7 0.7 0.7 0.7 0.7		
F анк.	Total He	Total He	Total Heat	1,145°05 1,163'46 1,172'89 1,178'92 1,183'5 1,190'3 1,193'0 1,193'0 1,199'6 1,199'6
HEAT IN DEGREES FAHR	Latent Heat.	1,043 ° 05 1,043 ° 05 979 ° 6 979 ° 6 979 ° 6 979 ° 6 979 ° 7 979 ° 7 979 ° 7 979 ° 7 970 °		
HEA	ıture.	Dif. per lb. 1 1 2 2 2 2 2 2 2 2		
	Temperature.	102.0° 162.37 193.29 213.07 228.0 250.4 250.4 250.4 250.4 250.4 250.4 250.4 250.4 250.4 250.4 250.4 250.4 250.4 250.7		
Pressure Absolute.	In inches of Mercury at 32°.	2.0375 10.1875 20.375 30.525 40.75 50.9375 61.125 71.3125 81.5 91.6875 112.0625 112.025		
A.P.	In lbs. on the sq. in.	1 20 20 20 20 20 20 20 20 20 20 20 20 20		

PROPERTIES OF SATURATED STEAM AT PRESSURE FROM ONE POUND TO 200 POUNDS ON THE SQUARE INCH.—(Continued.)

(" Compend. of Mechanical Refrigeration.")

Specific	the atmosphere at 32° being 1.	2.029 2.029 2.151 2.271 2.391 2.511 2.511	2.871 2.990 3.105 3.327 3.347
Weight of one	cubic foot in Decimals of a pound.	0.1535 0.1636 0.1736 0.1833 0.1930 0.2030	0.2319 0.2319 0.2503 0.2598 0.2693
Volume, that of an	weight of Water at its greatest density being r.	381 381 383 383 383 383 383 383 383	259 259 239 231 231
	ea .	Der lb.	7 7 7 7 7 7 7 0
F Анк.	Total Heat	1,206.3 1,207.8 1,209.1 1,210.4 1,211.6 1,212.8	1,215.0 1,216.0 1,218.0 1,218.9 1,219.8
HEAT IN DEGREES FAHR.	Latent Heat.	903.4 900.3 897.1 891.4 888.7 888.7	881.4 875.0 876.9 872.6 872.6
HEA	ature.	Dif. Per lb. 1 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	, 9, 9, 9, 9, 9, 9, 9, 9, 9, 9, 9, 9, 9,
	Temperature.	302'9° 307'5 312'0 316'1 320'2 324'1	334.5 338.0 341.1 347.2 350.0
Pressure Absolute.	In inches of Mercury at 32°.	142.625 152.8125 163.0 173.1675 183.375 193.5625 203.75	213 9375 224.135 234.3125 244.5 254.6875 264.875 275.0625
₽¥	In lbs. on the sq. in.	5288828	110 110 120 130 135

Properties of Saturated Steam at Pressure from one pound to 200 founds on the square inch.—(Continued.)

("Compend, of Mechanical Refrigeration,")

P	Pressure Absolute.		HEA	HEAT IN DEGREES FAHR.	Улик,		Volume, that of an equal	Weight of one	Specific Gravity,
In lbs. on the sq. in.	In inches of Mercury at 32°.	Temperature.	ture.	Latent Heat.	Total Heat	sat,	Water at its greatest density being to	Decimals of a pound.	the atmo- sphere at 32° being r.
			Dif.			Dif.			
	9	0,,616	per lb.	9.898	3.1.6	per lb.	216	0.2881	3.582
04:	205.25	352.9	9 0	8.998	1,222.4	0.5	209	0.2978	3.697
£1.	205.43/3	258.2		864.0	1,223.2	0.5	203	0.3073	3.809
ו ני	215.8125	300.0	3.0	863.1	1,224.0	0.5	961	0.3168	3.927
3.5	226.0	362.4	0.0	861.4	1,224.8	0.5	161	0.3263	4.042
192	336.1875	365.0	0.5	859.7	1,225.6	0.5	981	0.3353	4.157
170	346-375	368.2	0.4	858.1	1,226.3	0.5	181	0.3443	4.270
175	356.5625	3.00.8	0.0	856.4	1,227.0	0.1	176	0.3533	4.383
2	266.75	272.0	7.0	854.8	1,227.7	0.1	172	0.3623	4.495
2 2	276-0275	275.2) C	853.1	1,228.4	0.1	168	0.3713	4.607
9	387.135	27.7.6	6	9.138	1.220.1	1.0	164	0.3800	4.720
3 :	20,123	277.0	7 6	2.0	1 220.8	0.5	091	0.3888	4.032
202	290 3023	281.7	5 C	848.6	1,230.3	i.o	157	0.3973	4.645
}	C / .	, , , ,	<u> </u>	}					

HEAT OF COMBUSTION OF VARIOUS FUELS.

Fuel.	Air Cher Consu per lb. o	med	Total Heat of Combustion of 1 lb. of Fuel.	Equivalent Evaporative Power, from and at 212° F., Water per lb. of Fuel.
	lbs.	Cub Ft. at 62° F.	Units.	lbs.
Asphalt	11.85	156	17,040	17.64
Coal of average composition	10.7	140	14,700	15.55
Coke	10.81	142	13,548	14.02
Lignite	8.85	146	13,108	13.57
Peat, desiccated	7.52	99	, 12,279	12.71
Peat, 30 per cent. moisture	5.24	69	8,260	9.53
Peat charcoal, desiccated	9.9	13ó	12,325	12.76
Petroleum	14.33	188	20,411	21.13
Petroleum oils	17.93	235	27,531	28.50
Straw	4.26	56	8,144	8.43
Wood charcoal, desiccated	9.21	125	13,006	13.46
Wood, desiccated	6.09	80	10,974	11.36
Wood, 25 per cent. moisture	4.22	60	7,951	8.20
Coal gas, per cubic foot at 62° F		_	630	0.20

PERCENTAGES, HANDY RULE.

Regard percentages as a decimal fraction, and with it multiply the whole number wanted. For example, 16 per cent. of 80 is $80 \times 0.16 = 12.8$.

SPECIFIC HEAT OF WATER AT VARIOUS TEMPERATURES.

Tempera- ture. Deg. Fahr.	Specific Heat.	Units of Heat required to raise 1 lb. of Water from 32° F. to given Temperature.	Tempera- ture. Deg. Fahr.	Specific Heat.	Units of Heat required to raise 1 lb. of Water from 32° F. to given Temperature.
32°	1,0000	0,000	248°	1.01 77	217:449
50	1.0002	18.004	266	1'0204	235.791
50 68	1'0012	36.018	284	1.0235	254.187
86	I '0020	54.047	302	1.0565	272.628
104	1.003 0	72.090	320	1.0294	291.132
122	1'0042	90.127	338	1.0328	309.690
140	1.0026	108.247	356	1.0364	328.320
158	1.0072	126.378	374	1.0401	347.004
176	1.0089	144.208	392	1.0440	365.760
194	1.0109	162.686	410	1.0481	384.588
212	1.0130	180.000	428	1.0524	403.488
230	1.0123	199.152	446	1.0568	422.478

SPECIFIC HEAT OF METALS, ETC.

METALS.			STONES (contd.)	
Antimony		0.0202	Chalk	0'2148
Bismuth	!	0.0308	Quicklime	0.5169
Brass	••]	0.0039	Magnesian limestone	0.2174
Copper		0.0021	1	
Cymbal metal		o.086	l.	
Gold	• •	0.0324	CARBONACEOUS.	
Iridium		0.1882	Coal	0.2411
lron, cast		0.1508	Charcoal	
,, wrought		0.1138	Cannel coke	
Lead	• .	0'0314	Coke of pit coal	
Manganese		0'1441	Anthracite	
Mercury solid		0.0319	Graphite, natural	
,, liquid Nickel		0.0333		
Nickel		0.1086	,, of blast furnaces	0.197
Platinum, sheet		0'0324		
,, spongy		0.0320		
Silver		0.0220	SUNDRY.	
Steel		0.1162	Glass	0'1977
Tin		0.0269	Ice	0.204
Zinc		0.0020	Phosphorus	0.2503
			Soda	0.5311
STONES.			Sulphate of lead	0.0872
Brickwork & maso	nrv	0'20	,, of lime	0.1966
Marble		0.5150	Sulphur	0.3036

SPECIFIC HEAT OF LIQUIDS.

Alcohol Benzine Mercury Olive oil Sulphuric acid Density, 1.87 ,, 1.30	0'6588 0'3932 0'9333 0'3096 0'3346 0'6614	Turpentine Vinegar Water at 32° F ,, 212° F ,, 32° to 212° F. Wood spirit Proof spirit	0'4160 0'9200 1'0050 0'6009 0'973
--	--	--	---

SPECIFIC HEAT OF GASES.

For Equal Weigh	ts. (Wa	ter = 1.)	At Constant Pressure.	At Constant Volume.
Air				0.2377	0.1688
Carbonic acid (CO,)		••	0.5164	0'1714
" oxide (CC	Ö)			0.2479	0.1768
Hydrogen	• •		'	3'4046	2.4096
Light carburetted h	ydroge	n	!	0'5929	0.4683
Nitrogen	•••		• •	0'2440	0.1740
Oxygen	• •	• •		0'2182	0.1229
Steam, saturated	• •			- !	0.3020
Steam gas		• •	• •	0.4750	0.3700
Sulphurous acid				0.1223	0.1246

BRITISH THERMAL UNIT, OR HEAT UNIT.

Amount of heat necessary to raise the temperature of 1 lb. of water 1° by the Fahr. scale when at 39.4° (temp. of max. density). Mech. eq. 778 ft.-lbs.

FRENCH CALORIE, ENGLISH EQUIVALENT.

Unit of heat used on the Continent with the metrical system. Amount of heat required to raise 1 kilo. of water through 1° Cent. B.T.U. × 0'252 = calorie. Calories $\times 3.968 = B.T.U.$

Loss of Pressure by Friction of Compressed Air in Pipes. F. A. Halsey.

Pipe.	Cul				pressed assing th					per
ter of	50	75	100	125	150	200	250	300	400	600
Diameter of Pipe.	Lo	ss of Pr	essure i	n Poun	ds per S Straigh	quare I it Pipe.	nch for	each 1,0	oo Feet	of
ins. 1 11 12 2 22 3 31 4 5	lbs. 10·40 2·63 1·22 ·35 ·14	1bs. 5.90 2.75 .79 .32 .11	1bs. 4.89 1.41 .57	7.65 2.20 .90 .31	lbs. 11.00 3.17 1.29 .44 .21	5.64 2.30 .78 .38	8.78 3.58 1.23 .59	5°18 1°77 85 45	9°20 3°14 1°51 °80	7.05 3.40 1.81 .59

FRICTION OF AIR IN TUBES.—Unwin, "Min. Proceedings Inst. C.E."

 $k = \text{coefficient of friction} = \frac{a}{v} + b$, a and b being constants, and v = velocity of air feet per second.

Diameter of tube, ft. Value of a	10064 100704	100941	.00959	
------------------------------------	--------------	--------	--------	--

COEFFICIENTS FOR EFFLUX OF AIR FROM ORIFICES. (Molesworth).

Vena contracta				0.08
Conical converging.				0.0
Cylindrical rounded at ends		•		0.0
Cylindrical throughout .				0.8
Thin plates	•	•	•	0.6

CENTRIFUGAL FANS.—Molesworth.

D = Diameter of fan.

V = Velocity of tips of fan in feet per second.

P = Pressure in lbs. per square inch.

 $V = \sqrt{P \times 97300.}$ $P = \frac{V^2}{97300}$

Power Required for Fans.—Molesworth.

P = Pressure of blast in lbs. per square inch.

A = Area of the sum of the tuyeres in square inches.

V = Velocity of tips of fan in feet per second.

HP = Indicated horse-power required.

 $HP = 0.000016 \text{ V}^2 \text{ A } \hat{P}$.

Proportions of Fans.—Molesworth.

Length of vanes = $\frac{D}{4}$ Width of vanes = $\frac{D}{4}$ Diameter of inlet $=\frac{D}{2}$. Eccentricity of fan $=\frac{D}{2}$. Length of spindle journal = 4 diameters of spindle.

164 REFRIGERATION AND ICE-MAKING.

HYDRAULIC RAM PROPORTIONS OF THE SUPPLY PIPES AND DELIVERY PIPES TO THE NUMBER OF GALLONS.—(Hutton.)

Number of gallons to be raised in 24 hours Diameter of fall or supply	500	1,000	2,500	4,000	6,000
pipe, in inches	I ½	2	$2\frac{1}{2}$	3	4
Diameter of rising main or delivery pipe, in inches .	8	1	I ½	2	2

Efficiency of Hydraulic Rams.—(Hutton.)

Number of times the height to which the water to be raised is contained in the fall.		5	6	7	8	9	10	11	12	13	14	15	16	18	19	20	25
Efficiency per cent	7.5	72	68	62	57	53	48	43	38	35	32	28	23	17	15	12	٥

POWER REQUIRED TO DRIVE CENTRIFUGAL PUMPS.

Diameter of suction and delivery pipes in inches.	Quantity of water delivered per minute, in gallons.	Horse-power required for every foot in height the water is raised.
ı	16	0.01
2	50	0.03
3	100	0.02
3 4 5 6	200	o.o <u>§</u>
5	300 i	0.16
Ď.	500	0.5
7	700	0.32
7 8	800	0.40
9	1,000	0.20
IÓ	1,500	0.75
11	1,800	1.0
12	2,000	1.01
13	2,300	1.08
14	2,500	I.50
	3,000	1.31
15 16	3,500	1.60
17	3,800	1.72
18	4,200	2.0

Table of Power required to raise Water from Deep Wells.—(Appleby.)

Gallons of water raised per hour.	200	350	500	650	800	1,000
Height of lift for one man working on crank, in feet	90	52	36	28	22	18
Height of lift for one donkey working on gin, in feet Height of lift for one horse work-	180	102	72	56	45	36
ing on gin, in feet Height of lift for one horse-power	630	357	252	196	154	126
steam-engine, in feet	990	561	396	308	242	198

Table giving Quantity of Water discharged per Minute by Barrel Pumps,—(Hutton.)

Diam.	Length	Single	barrel.	Double	barrel.	Treble	
of pump.	of stroke.	30 strokes per min.	40 strokes per min.	30 strok e s per min.	40 strokes per min.	30 strokes per min.	40 strokes per min.
Inches.	Inches.	Galls.	Galls.	Galls.	Galls.	Galls.	Galls.
11/2	9	12	21	3 1	41/2	4 1	6 3
2	9	3	4	6	8	9	12
2]	9	48	61	91/2	12	14	19
3	9	6	9	13 2 18 2	18	20	27
31/2	9	91	121	18\$	25	28	37
4	9	12	16	24½	32	36	48
44	9	15 ½	20 2	32	42	46	62
5	9	19	$25\frac{1}{2}$	38	50	57	76
5 5 1 6	9	231	32	46 1	62	69	9 2
6	9	271	37	55 6	73	82	110
2	10	32	41	6	9	10	13
2 ½	IO	5#	7	10	14	15	22
3 3½	10	71/2	10	15	20	22	30
31/2	10	102	138	20	27	32	42
4	10	131/2	18	27	36	40	54 68
4 1	10	17	23	34	45	52	
5	10	22	28	42	56 68	63	84
5 5 2 6	10	251	34	51	68	77	102
6	10	302	40	62	82	92	122
2	12	4.	5	8	10	12	16
21/2	12	4 61	5 *	12	17	19	25
3	12	9 12½	12	18	24	27	36
3 31/2	12	122	16	24	33	37	50
4	12	164	22	32	43	49 62	65
4 4 1	12	201	27	42	55 68		82
5	12	254	33	50 62	68	76	100
5 2	12	302	42	62	82	92	123
5 5 2 6	12	36½	49		97	IÍO	146
61	12	43		73 86	114	129	172
7	12	50	57 66	100	134	149	199
7 1	12	57	76	114	152	171	229
8	12	65	87	130	174	195	262
9	12	82	110	165	220	246	330
10	12	102	134	202	268	303	404
12	12	146	195	294	390	440	588

DIAMETERS, AREAS, AND DISPLACEMENTS.

Worthington Pumping Engine Company.

Diameter.	Area.	Displacement in Imperial Gallons per foot of Travel.	Diameter.	Area.	Displacement in Imperial Gallons per foot of Travel.	Diameter.	Area.	Displacement in Impediate of T
1 1 1 1 1 1 1 1 1 2 2 2 2 2 2 3 3 3 3 3	0122 0490 1104 1963 3068 4417 6013 7854 0940 1·227 1·484 1·767 2·073 2·405 2·761 3·141 3·546 3·976 4·430 4·908 5·911 7·068 8·295 8·946 9·621 10·32 11·04 11·79 12·56 14·18 15·90 17·72 19·63 21·54 23·75 25·96 28·27 30·67 33·18 35·78 38·48	.0005 .0021 .0047 .0084 .0132 .0190 .0259 .0339 .0429 .0530 .0641 .0763 .1038 .1192 .1356 .1531 .1717 .1913 .2120 .23565 .2804 .3053 .3313 .3583 .31583 .34156 .4156 .4156 .4769 .5193 .5426 .6868 .7655 .8480 .9348 .7655 .8480 .9348 .93	77778888899990100111111121213133444445556666677778811155666667777788888999901001111111111111111111111	41.28 44.17 47.17 50.26 53.45 56.74 60.13 63.61 67.20 70.88 74.66 78.54 82.51 86.59 90.76 95.03 99.40 117.8 113.0 117.8 113.7 112.7 1127.6 132.7 1137.8 1148.4 153.9 159.4 1153.9 159.4 1170.8 176.7 182.6 194.8 201.0 207.3 226.9 233.7 2240.5 247.4 254.4	1.783 1.908 2.037 2.171 2.309 2.451 2.597 2.747 2.903 3.362 3.393 3.564 4.484 4.682 4.105 4.294 4.4881 5.088 5.502 5.732 6.482 6.649 6.886 7.132 7.388 7.633 7.888 8.147 8.415 8.683 8.925 6.950 10.095 10.095 10.095 10.095	182 182 192 193 194 195 195 195 195 195 195 195 195 195 195	261·5 268·8 276·1 283·5 291·0 298·6 306·3 314·1 330·0 340·3 347·4 433·7 452·3 471·4 490·8 510·7 530·9 551·5 570·5 630·9 64	11·297 11·612 11·927 12·247 12·247 12·2900 13·232 13·568 14·960 15·681 16·420 17·176 18·735 19·539 20·364 21·202 22·962 22·935 23·824 24·732 25·556 26·558 27·567 28·533 32·607 39·221 41·562 43·949 39·221 41·569 43·949 39·221 41·569 55·656 68·688 71·794
In (<i>i.e.</i> ,	estimating the deliver	the capa y in gallo	city of	Worthir r minute	ngton (an or per h	d other	er duplex) at a given	Pumps rate of

In estimating the capacity of Worthington (and other duplex) Pumps (i.e., the delivery in gallons per minute or per hour) at a given rate of piston speed, it should be noted that they have two double-acting water plungers: the capacity, therefore, is double that of any ordinary double-acting pump of same size, or four times as large as a single-acting pump.

PRESSURE OF WATER.

Worthington Pumping Engine Company.

The pressure of water in pounds per square inch for every foot in height to 270 ft. By this Table, from the pounds pressure per square inch the feet head is readily obtained, and vice verså.

fee	t head i	s rea	dily obt	ained	, and vi	ce ver	så.				
Feet Head.	Pressure per sq. in.	Feet Head.	Pressure per sq. in.	Feet Head.	Pressure per sq. in.	Feet Head.	Pressure per sq. in.	Feet Head.	Pressure per sq. in.	Feet Head.	Pressure per sq. in.
1 2 3 4 5 5 6 7 8 9 10 11 1 12 13 14 15 16 17 18 19 20 21 22 23 30 31 32 33 34 35 5 36 37 38 39 40	0.43 0.86 1.30 2.16 2.59 3.34 3.46 5.63 4.33 4.76 5.63 6.66 9.09 9.53 9.93 10.82 11.26 11.26 11.26 11.21 12.55 12.12 13.86 14.72 15.16 15.59 16.02 16.45 16.45 16.45 16.45 16.45 16.45 16.45 16.45 16.45 16.45 16.45 17.32	46748 4955 555 555 555 566 666 666 667 7 7 7 7 7	19.92 20.35 20.72 21.65 22.09 22.95 23.82 24.69 25.55 22.95 26.85 27.72 28.58 29.02 29.88 30.75 31.62 29.88 30.75 31.62 32.48 32.92 33.78 33.78 33.78 34.21 34.68 35.59 36.88 36.88	91 92 93 94 95 96 97 98 99 100 101 105 107 108 109 110 111 112 113 114 115 116 117 118 119 121 122 123 124 125 126 127 128 129 129 120 121 121 122 123 124 125 126 127 128 129 120 121 121 122 123 124 125 126 127 128 129 120 120 121 121 122 123 124 125 126 127 128 129 120 120 120 120 120 120 120 120	39.42 39.85 40.28 40.72 41.58 42.45 42.45 43.31 43.75 44.61 45.08 45.08 45.08 45.08 45.08 45.08 47.26 49.38 49.38 49.38 49.38 49.38 49.38 49.38 49.38 49.38 49.38 49.38 49.38 49.38 49.38 49.38 50.61 51.54	136 137 138 140 141 142 143 144 145 146 147 150 153 154 155 156 166 167 168 169 170 171 171 172 173 174	58·91 59·34 59·77 60·64 61·07 61·51 63·67 62·37 62·37 62·37 63·67 63·67 64·10 64·54 66·74 66·74 66·74 66·74 67·57 68·83 68·87 69·31 69·74 70·17 70·61 71·04 71·94 72·34 72·77 73·20 73·64 74·77 73·20 73·58 74·94 75·37 75·80	181 182 183 184 185 186 187 190 191 192 193 194 195 197 198 199 200 201 202 203 204 205 207 202 203 204 212 212 213 214 217 218 219 219 219 219 219 219 219 219 219 219	78-40 78-84 79-77 780-14 80-57 81-03 81-87 82-33 83-60 84-03 84-03 84-03 84-03 88-36 88-36 88-36 88-36 88-36 88-36 88-36 89-23 89-60 90-53 90-96 91-83 90-96 93-13 92-26 92-69 93-13 92-26 92-69 93-13 92-26 92-69 93-13 92-26 92-69 93-30 93-55	226 227 228 230 231 232 233 234 235 237 238 239 240 241 242 243 244 2245 245 255 255 256 257 258 259 260 261 262 263 263 263 263 263 263 263 263 263	97.90 98.33 98.76 99.20 99.63 100.06 100.93 101.36 101.79 102.66 103.09 103.53 103.53 104.83 105.26 104.83 105.26 106.13 106.56 106.93 107.86 108.29 108.73 109.59 110.36 110.95 110
41 42 43 44 45	17.75 18.19 18.62 19.05	86 87 88 89 90	37.25 37.68 38.12 38.55 39.98	131 132 133 134 135	56·74 57·18 57·61 58·04 58 ·4 8	176 177 178 179 180	76·23 76·67 77·10 77·53 77·97	221 222 223 224 225	95.73 96.16 96.59 97.03 97.46	266 267 268 269 270	115.22 115.66 116.09 116.52 116.96

DIMENSIONS, ETC., OF STANDARD WROUGHT-IRON PIPES.

Nominal site in inches.	Inside diam. in Inches.	Inside cliam, extra acrong in inches.	Inside diam, extra double strong in ins.	External diam. in inches.	Internal diam. in Inches.	External circumference in inches.	J.cngth in fact per aquare foot outside surface.	Weight per foot in lbs.	Number of threads per inch.
ļ	0.22	0.50	_	0.40	0.022	1.272	9.44	0.54	27
111424	0.36	0.50		o·54 o·67	0.1041	1.696	7.075	0.42	18
3	0.49	0.43	_	0.67	0.1916	2.I3I	5.657	0.26	18
1/2	0.62	0.24	0.54	0.84	0°3048	2.652	4.202 3.637	o.26 o.82	14
4	0.85	o ⁻ 73	0.45	1.02	o·5333 o·8627	3.599	3.637	1.15	14
I	1'04	0.62	o.88	1.99	0.8622	4.134	2.303	1.67	111
, 1 1	1.91	1.52	0.88	1.66	1.496	5.369 2.312	5.301	2.25 2.69 3.66 5.77 7.54	ΙΙŻ
ΙŽ	1.61	1.49	1.08	1.30	2.038	5.969	2.0I	2.69	113
2	2.06	1.93	1.49	2.32	3.352	7.401	1.911	3.66	112
21/2	2.46	2.89 5.89	1.42	2.87	4·783 7·388 9·887	9.032 10.996 12.566	1.358	5.77	8
3 3 2	3.06	2.89	2.58	3.20	7:388	10.996	1.001	7.24	8
31/2	3.24	3.32	2.21	4.00	9 887	12.266	0.955	9.05	8
5 6	4.03	3.81	3.13	4.50 5.56 6.62	12.430	14.137	0.849	10.45	8
5	5.04 6.00	i —	_	2.26	10,000	17.475	0.629	14 [.] 56 18 [.] 77	8
6 ,		-		6.62	28.889	20.813	0.222	18.44	8
7 8	7.02	. —	_	7·62 8·62	38.737	23.954	0.202	23.41 28.35	8
8	7.98	<u> </u>	_	8.62	50.039	27.096	0.444	28.35	8 8 8 8 8 8 8 8
9	9.00	-	! =	9.68	63.633	30.433	0.394	34.07	8
10	10.01	-	· —	10.72	78.838	33.772	0.322	40.64	8

STRENGTH OF ICE.

Ice of a thickness of $1\frac{1}{2}$ inch will support a man; 4 inches in thickness will support cavalry; 5 inches in thickness will support an 84-pound cannon; 10 inches in thickness will support a multitude; 18 inches in thickness will support a railroad train.

FRICTION IN PIPES.

Friction loss in pounds pressure for each 100 feet in length of cast-iron pipe discharging the stated quantities per minute.—(G. A. Ellis, C.E.)

U.S.		1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1
Sizes of pipes, inside diameters.	18,,	0.005 0.005 0.020 0.030 0.031 0.031 0.263
	16,	0000 0010 0010 0010 0010 0010 0010 001
	14"	0017 0036 0036 0031 0031 0031 0031 0031 0031
	12"	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
	"oī	0.000 000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.000 0.
	.,8	0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0
	,,9	0.00 0.00 0.00 0.00 0.00 0.00 0.00 0.0
	,4	0000 00000 00000 00000 00000 00000 00000
	3,6	0.10 0.14 0.17 0.17 0.17 0.17 0.17 0.17 0.17 0.17
	5 1 ,,	200000011120002114 12000011100001114 120000000000
	2,1	7. 7. 7. 7. 7. 7. 7. 7. 7. 7. 7. 7. 7. 7
	,, ‡ 1	48 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9
	r\$''	0 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2
	"1	0.84 3.16.33 3.37.00 4.80 0.00 1.00 1.00 1.00 1.00 1.00 1.00 1
	÷.	78.0 % 70.0 % 70.4 %
Imperial gallons.		4 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1

The frictional loss is increased by bends or irregularities in the pipes.

COMPARISON BETWEEN THE SCALES OF CENTIGRADE AND FAHRENHEIT THERMOMETERS.

Centigrade.	Fahrenheit.	Centigrade.	Fahrenheit.
-73	- 1000	-24	-11.3
-72	−97·6	-23	- 9.3
-7 I	−95·8	-22	- 7.6
<u> </u>	-94·o	-21	- 5.8
-69	-92.2	-20	- 4.0
–6 8	-90.4	-19	- 2.2
-6 7	−88.6	-18	- 0.4
-66	-86.8	-17	+ 1.4
-65	-85·o	-16	+ 3.2
-64	-83.3	-15	+ 5·0 + 6·8
-63	-81.4	-14	
-62	-79.6	-13	+ 8.6
-61	-77.8	-12	+ 10.4
–60	− 76 ·o	-11	+ 12.2
-59	-74.2	-10	+ 14.0
- 58	-72.4	- 9 - 8	+15.8
-57	-70.7		+ 17.6
-56	−68·8	- 7 - 6	+ 19.4
-55	-67.0		+21.2
-54	-65·3	- 5 - 4	+ 23.0
-53	-63·4 -61·6	- 4	+ 24·8 + 26·6
- 52 - 51	-59·8	- 3 - 2	+ 28.4
-50	_58·o	- i	+ 30.5
-49	-56·2	- 6	+32.0
-49 -48	-54·4	+ 1	+33.8
-47	-52·6	+ 2	+35.6
– 46	-50·8	+ 3	+37.4
-45	-49 ·0	+ 4	+ 39.2
-44	-47.2		+41.0
-43	-45.4	+ 5 + 6	+42.8
-42	-43.6	+ 7	+446
-41	- 41.8	+ 7 + 8	+ 46.4
-40	- to.o	+ 9	+48.2
- 39	- 38.2	+ 10	+ 50.0
-38	 36·4	+11	+51.8
-37	- 34·6	+ 12	+ 53.6
-36	-32.8	+ 13	+ 55.4
-35	-31.0	+ 14	+ 57.2
-34	- 29.2	+15	+ 590
-33	-27.4	+16	+60.8
-32	-25·6	+ 17	+62.6
-31	-23·8	+ 18	+64·4 +66·2
-30 -30	-22·0 -20·2	+ 19 + 20	+68.0
-29 -28	-18·4	+ 20 + 21	+69.8
-27	-16·6	+22	+71.6
-26	-14·8	+23	+73.4
-25	-13.0	+24	175.2
-3	•3 •	,	. 13 -

TO CONVERT DEGREES CENTIGRADE OR REAUMUR INTO DEGREES FAHRENHEIT, ETC.

Let F = degrees Fahrenheit; C = degrees Centigrade; and R = degrees Reaumur.

$$F = \frac{9C}{5} + 32$$
 $F = \frac{9R}{4} + 32$ $C = \frac{5(F - 32)}{9}$ $R = \frac{4(F - 32)}{9}$

USEFUL INFORMATION.

A gallon of water contains 231 cubic in., and weighs 8½ lbs. (U.S. standard).

A cubic foot of water contains $6\frac{1}{4}$ gallons, and weighs $62\frac{1}{9}$ lbs.

The friction of liquids and vapours through pipes increases as the square of the velocity.

Sensible heat of a liquid is the amount indicated by the thermometer when immersed in it.

Specific heat is the amount of heat absorbed to produce sensible heat.

Latent heat is the amount of heat required for the conversion into vapour after a liquid has reached its boilingpoint.

The latent heat of vapour is given off whilst condensing to a liquid; the sensible heat is retained.

One U.S. gallon = 0'133 cubic ft.; 0'83 imperial gallon; 3.8 litres.

An imperial gallon contains 277.274 cubic in.; 0.16 cubic ft.; 10'00 lbs.; 1'2 U.S. gallons; 4'537 litres.

A cubic inch of water = 0.03607 lb.; 0.003607 imperial

gallon; 0.004329 U.S. gallon.

A cubic foot of water = 6.25 imperial gallons; 7.48 U.S. gallons; 28.375 litres; 0.0283 cubic metre; 62.35 lbs.; 0'557 cwt; 0'028 ton.

A lb. of water = 27.72 cubic in.; 0.10 imperial gallon;

0.83 U.S. gallon; 0.4537 kilo.

One cwt. of water = 11.2 imperial gallons; 13.44 U.S. gallons; 1.8 cubic ft.

A ton of water = 35.84 cubic ft.; 224 imperial gallons; 298.8 U.S. gallons; 1,000 litres (about); 1 cubic metre (about).

A litre of water = 0.22 imperial gallon; 0.264 U.S. gallon;

61 cubic in.; 0.0353 cubic ft.

A cubic metre of water = 220 imperial gallons; 264 U.S. gallons; 1'308 cubic yard; 61'028 cubic in.; 35'31 cubic ft.; 1,000 kilos; 1 ton (nearly); 1,000 litres.

A kilo of water = 2.204 lbs.

A vedros of water = 2.7 imperial gallons.

An eimer of water = 2.7 imperial gallons.

A pood of water = 3.6 imperial gallons.

A Russian fathom = 7 ft.

One atmosphere = 1.054 kilos per square in.

One ton of petroleum = 275 imperial gallons (nearly); 360 U.S. gallons (nearly).

A column of water 1 ft. in height = 0.434 lb. pressure per

square in.

A column of water I metre in height = 1.43 lb. pressure per square in.

One lb. pressure per square in. = 2.31 ft. of water in height.

One U.S. gallon of crude petroleum = 6.5 lbs. (about).

According to Prof. Siebel, about ten B.T.U. of heat will pass through a square foot of ice I inch thick in one hour for every degree Fahrenheit difference between the temperatures on either side of the ice sheet.

A cubic foot of ice weighs approximately 57.5 lbs.

A cubic foot of water frozen at 32° makes 1.0855 cubic ft. of ice.

One French horse-power = 75 kilogrammetres (542.533 foot-pounds) per second.

One force de cheval = 0.986337 horse-power. One horse-power = 1.01385 force de cheval.

Indicated French horse-power = 3'49 D²PRS.

D = dia. of cy. in metres, S = length of stroke in metres, R = number of revs. per minute, and P = average pressure on piston in kilogs. per square centimetre.



FRACTIONS OF AN INCH AND DECIMAL EQUIVALENTS.

Fractions.	Inch.	Fractions.	Inch.	Fractions.	Inch.
1-32 1-16	0'03125	3-8 13-32	o:375 o:40625	23-32	o [.] 71875
3-32 1-8	0.09322	7-16 15-32	o'4375 o'46875	25-32 13-16	0.78125
5-32 3-16	0.12622 0.1822	1-2 17-32	0.2 0.23122	27-32 7-8	o·84375 o·875
7-32 I-4	0.21872	9-16	o·5625 o·59375	29-32 15-16	0.90625 0.9375
9-32 5-16	0.3152	5-8 21-32	0.625	31-32	0.96875
11-32	0.34375	11-16	o [.] 6875		

Comparison of British Measures with U.S.

United States Standard.		British Standard.				
				0.833565		gill.
				0.833565	,,	pint.
				0.833565	,,	quart.
4 quarts	=	1 gallon	=	0.833262	"	gallon.

An imperial gallon = 4.5435 litres = 1.19968 U.S. standard gallons.

An imperial gallon contains (Act of Parliament, 1878) 10 lbs. of water at a temperature of 62° Fahr. Its accepted volume is 277'274 cubic in.

SPECIFIC GRAVITIES OF GASES.

Gas at 32° and below one atmosphere.	Specific gravity.	Cubic feet in	
Air	1.000	12.38	
Ammonia	o·589	21'01	
Carbonic acid	1'529	8.10	
Chlorine	2'440	5.02	
Nitrogen	0.978	12.72	
Oxygen	1.102	11.50	

Information required by Manufacturers to enable them to estimate for the Cost of a Refrigerating Plant.

1. The length, breadth, and height of the cellars, rooms, or stores to be refrigerated. If the ceiling or roof is vaulted, the height to the centre and spring of the arch will be required. Full particulars of the means of insulation adopted, or, if none exist, of the materials from which the chambers are built.

2. Whether it is desired to refrigerate on the direct expansion, on the brine circulation, or on the cold-air

system.

3. The temperature desired to be maintained in each chamber or store.

4. The nature of the substance which it is desired to refrigerate.

5. In the case of a packing-house, or an abattoir, the largest number of carcases to be cooled daily, and their average weight.

6. In the case of a freezing chamber for beef, mutton, or other produce, the number of carcases, etc., to be frozen in each 24 hours, and their average weight.

7. When a liquid is to be cooled, the number of gallons, or barrels, to be dealt with per hour, and from what tem-

perature down.

8. The nature, quantity, and temperature of the water

supply available for use.

9. Rough dimensioned plan of the establishment, showing the most convenient spot to locate the refrigerating machine.

Information required by Manufacturers to enable them to estimate for the Cost of an Ice-making Plant.

1. Number of tons of ice that it is desired to produce per 24 hours.

2. If clear, crystal, transparent ice is required, or whether opaque ice will do for the purpose.

3. The nature, quantity, and temperature of the supply of water procurable for use.

4. Whether there is an available source of steam supply on the premises; and if spare steam-power, then how many horse-powers could be utilised.

5. When the installation is to be erected in existing

buildings, a rough dimensioned plan of same.

6. Where an estimate of cost of making ice is required, price and quality of fuel; wages of engine-drivers, stokers, and common labourers, for 12 hours day work, and for 12 hours night work; if water has to be bought, cost of same.

VARIOUS HORSE-POWERS IN USE.

		Kilogrammetres per second.	Foot-pounds per minute.	Ratio to British H.P.
Austria	••	76.119	33,034	1,001
Baden	• •	75.000	32,552	0.986
France	• •	75.000	32,552	o·986
Great Britain		76.041	33,000	1,000
Hanover		75.361	32,705	0.990
Prussia		75'325	32,689	0.990
Saxony		75'045	32,568	o·986
Wurtemburg		75.240	32,637	o•988

EXPANSION IN STEAM PIPES.

The expansion and contraction of steam pipes is about 1 inch in 50 feet by reason of temperature variations. This expansion and contraction may be provided for in the case of long lengths of pipe between fixed abutments, by spring bends or lengths, or by expansion sockets. In the latter case, guard bolts should be fitted to prevent the pipes from being drawn out of the sockets.

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